

## Article

# Study on the Catalytic Activity and Selectivity of Manganese Dioxide-Modified Nickel–Iron-Based Hydroxide Electrodes for Initiating the Oxygen Evolution Reaction in Natural Seawater

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**Abstract:** Transition metal oxides, particularly NiFe(OH)<sub>2</sub>, are recognized for their high oxygen evolution reaction (OER) activity and structural stability. However, their performance in natural seawater electrolysis remains insufficiently studied. Manganese dioxide (MnO<sub>2</sub>), which is known for its multiple crystal phases and high OER selectivity, can be incorporated to enhance the catalytic properties. In this study, the OER catalytic performance of carbon cloth-supported manganese dioxide-modified nickel–iron bimetallic hydroxide (MnO<sub>2</sub>-NiFe-LDH/CC) electrodes was explored in both alkaline and natural seawater. Electrochemical tests demonstrated that the MnO<sub>2</sub>-NiFe-LDH/CC electrode achieved overpotentials of 284 mV and 363 mV at current densities of 10 mA·cm<sup>-2</sup> and 100 mA·cm<sup>-2</sup>, respectively, with a Tafel slope of 68.6 mV·dec<sup>-1</sup> in alkaline seawater. Most importantly, the prepared MnO<sub>2</sub>-NiFe-LDH/CC electrode maintained stable OER performance over 120 h of testing. In natural seawater, the MnO<sub>2</sub>-NiFe-LDH/CC electrode outperformed the NiFe-LDH/CC electrode by exhibiting an oxygen evolution selectivity of 61.1%. This study highlights the potential of MnO<sub>2</sub>-modified nickel–iron-based materials for efficient and stable OER in seawater electrolysis, which offers a promising approach for sustainable hydrogen production in coastal desert regions.

**Keywords:** catalytic activity and selectivity; manganese dioxide; nickel–iron-based hydroxide electrodes; oxygen evolution reaction; natural seawater



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## 1. Introduction

Hydrogen is not only a carbon-free energy carrier with extremely high energy density but also a crucial raw material for hydrogenation, petroleum refining, and fertilizer production [1]. Hydrogen production through seawater electrolysis is a viable option, especially in coastal desert regions like the Middle East, where freshwater resources are scarce [2]. By effectively substituting seawater for freshwater in various applications, the freshwater scarcity crisis can be alleviated to some extent. Seawater electrolysis technology is also environmentally friendly and easy to operate [3]. However, the generation of oxygen is often inhibited because seawater contains chloride ions, which lead to the production of chlorine gas at the anode during electrolysis. The release of chlorine gas poses serious health risks, corrodes equipment, and causes environmental pollution [4]. Therefore, developing anode materials that promote oxygen evolution while suppressing chlorine evolution is crucial for clean hydrogen production from seawater electrolysis technology [5]. In the literature, noble metal oxides are reported as the benchmark anode catalysts for the oxygen evolution reaction (OER), due to their rapid reaction kinetics [6,7]. However, the high costs of these noble metal catalysts remain major obstacles to their practical application [8,9]. Although some non-noble metal electrocatalysts, including metal oxides, metal nitrides

and oxynitrides [10], metal carbides and carbonitrides [11], metal sulfides [12], and hydroxides [13], have also been reported with good catalytic performance in catalyzing the OER in seawater electrolysis, it should be noted that the seawater used in these studies was usually simulated seawater or alkaline seawater. Typically, simulated seawater contains only a strong alkali and NaCl, while alkaline seawater is natural seawater with a certain amount of KOH or NaOH present. Compared to natural seawater, simulated seawater has a simpler composition, and the performance of electrodes in simulated seawater significantly differs from that in natural seawater. More specifically, the concentration of  $\text{OH}^-$  in alkaline seawater is much higher than that in natural seawater, which greatly accelerates the OER kinetics in alkaline seawater and suppresses the chlorine evolution process. Therefore, using simulated seawater or alkaline seawater to draw analogies about the performance of anodes in natural seawater is incomplete for effective seawater electrolysis research.

In this study, the performance of carbon cloth-supported manganese dioxide-modified nickel–iron bimetallic hydroxide electrodes was investigated for catalyzing the OER in natural seawater. The focus was on both the catalytic activity of the electrodes in promoting OER and their selectivity toward oxygen evolution under natural seawater conditions. As is well-known, transition metal oxides are a class of positively charged oxides valued for their rich catalytic sites, structural stability, environmental friendliness, and ease of synthesis. Through methods such as controlling the metal atom ratio [14], adjusting defects in the crystal structure [15], modifying the crystalline phase of  $\text{NiFe}(\text{OH})_2$  [16,17], and changing the substrate material [18],  $\text{NiFe}(\text{OH})_2$ , as one of the best and most recognized OER catalysts, has achieved an alkaline OER potential of 1.45 V vs. RHE and a current density of  $100 \text{ mA}/\text{cm}^2$  [19]. In a previous study by Dionigi et al. [20],  $\text{NiFe}(\text{OH})_2$  exhibited good OER catalytic activity and 100% selectivity in artificial seawater or alkaline solutions with NaCl, even with the presence of chloride ions. However, it is still necessary to verify whether  $\text{NiFe}(\text{OH})_2$  can be effectively applied as an anode catalyst in natural seawater electrolysis. Meanwhile, manganese dioxide ( $\text{MnO}_2$ ) has been reported as having high catalytic activity and selectivity for the OER in seawater electrolysis. This is attributed to its multiple crystal phases and morphologies, which are generated by various tunnel structures from  $[\text{MnO}_6]$  structural units with different stacking and connecting styles [21–23]. For instance, Sang et al. [24] studied the activity and oxygen evolution selectivity of  $\gamma\text{-MnO}_2$  and its electrodes when doped with different elements. They achieved 100% oxygen evolution selectivity after optimization. However, their electrode consisted of a titanium plate +  $\text{IrO}_2$  substrate, which indicated a collective catalytic performance of  $\text{IrO}_2$  and  $\gamma\text{-MnO}_2$ . Similar structures were also reported by Vos et al. [25], which further emphasized the positive effect of  $\text{MnO}_2$  as an additive component in seawater electrolysis anode catalysts.

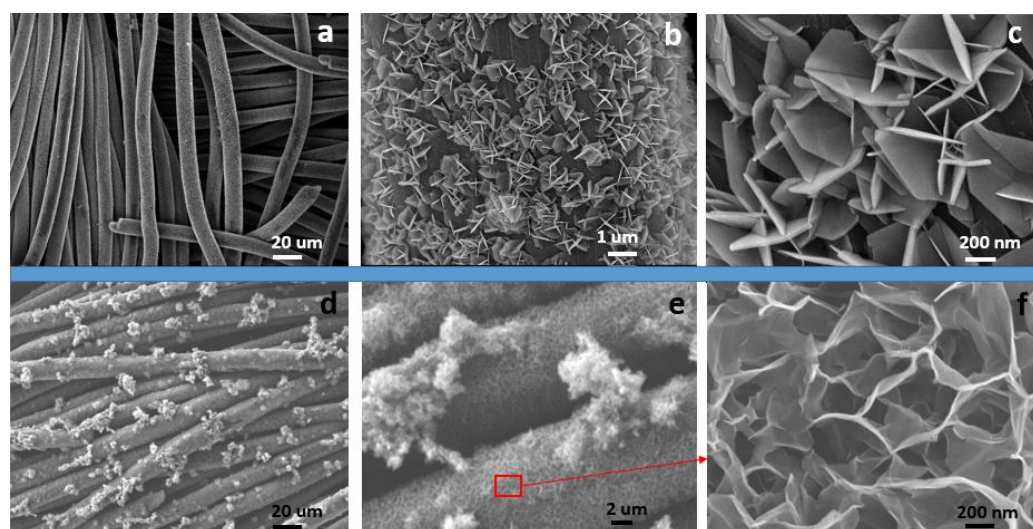
In this work, considering the inertness of carbon cloth (CC) substrate toward  $\text{Cl}_2$  and  $\text{ClO}^-$ , a manganese dioxide-modified nickel–iron hydroxide electrode catalyst ( $\text{MnO}_2\text{-NiFe-LDH}$ ) was constructed into a three-dimensional (3D) self-supporting electrode, using CC as the substrate ( $\text{MnO}_2\text{-NiFe-LDH}/\text{CC}$ ). Their catalytic activity and selectivity for oxygen evolution in natural seawater electrolysis were investigated. The results showed that the optimal  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC}$  electrode sample exhibited an excellent OER catalytic performance in seawater electrolysis, with an oxygen evolution selectivity of 61.1%.

## 2. Results and Discussion

Figure S1 in the Supplementary Materials illustrates the preparation procedure of the 3D  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC}$  electrode sample. First,  $\text{NiFe-LDH}$  nanosheet arrays were grown on the surface of pure CC, followed by the hydrothermal growth of  $\text{MnO}_2$  on the  $\text{NiFe-LDH}$  surface. For optimization, the amount of the precursor  $\text{KMnO}_4$  was adjusted to produce electrode samples with different  $\text{MnO}_2$  loadings, which were then electrochemically tested in 1.0 M KOH for screening. As shown in Figure S2a, the  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC-0.01}$  mmol electrode sample exhibited the lowest voltage and the lowest onset potential at the same current density ( $100 \text{ mA}\cdot\text{cm}^{-2}$ ), which indicates that the electrocatalyst with this  $\text{MnO}_2$  loading achieved the highest OER catalytic activity. The bar chart in Figure S2b presents the

exact overpotential values of four electrode samples with different  $\text{MnO}_2$  loadings at current densities of  $50 \text{ mA} \cdot \text{cm}^{-2}$  and  $100 \text{ mA} \cdot \text{cm}^{-2}$ , respectively. As illustrated, the  $\text{MnO}_2$ -NiFe-LDH/CC-0.01 mmol electrode sample presents the lowest oxygen evolution overpotential. As shown in Figure S2c, the kinetic performance of the  $\text{MnO}_2$ -NiFe-LDH/CC electrode sample was investigated using the Tafel slope, and the  $\text{MnO}_2$ -NiFe-LDH/CC-0.01 mmol sample exhibited a lower Tafel slope of  $68.6 \text{ mV} \cdot \text{dec}^{-1}$ . This result aligns with the analysis of the LSV curves in confirming that the  $\text{MnO}_2$ -NiFe-LDH/CC-0.01 mmol electrode sample exhibited the best OER catalytic activity among the six catalytic samples. The mass change of the samples before and after  $\text{MnO}_2$  loading was recorded to calculate the  $\text{MnO}_2$  loading value. The  $\text{MnO}_2$  loading in the  $\text{MnO}_2$ -NiFe-LDH/CC-0.01 mmol electrode with the best OER performance was  $0.54 \text{ mg} \cdot \text{cm}^{-2}$ . Therefore, subsequent discussions will refer exclusively to the optimal  $\text{MnO}_2$ -NiFe-LDH/CC sample. For convenience, this optimal sample will be referred to simply as  $\text{MnO}_2$ -NiFe-LDH/CC.

Figure 1a–c depicts the scanning electron microscope (SEM) images of the NiFe-LDH/CC sample, wherein NiFe-LDH was hydrothermally deposited on the surface of the CC substrate. In Figure 1a, the NiFe-LDH/CC sample shows intertwined fluffy carbon fibers with diameters of around  $6 \mu\text{m}$ . By comparison with the SEM images of CC carbon fibers in Figure S3 in the Supplementary Materials, it is evident that the fluffy material on the NiFe-LDH/CC fibers' surface is a NiFe-LDH species, and the carbon fiber surfaces are uniform and well-structured. This uniformity indicates an even distribution of NiFe-LDH on the CC surface. The magnified images in Figure 1b,c reveal that NiFe-LDH consists of interwoven sheets with relatively smooth surfaces. This interconnected nanosheet structure is beneficial as it exposes a larger specific surface area. Figure 1d–f shows SEM images of the  $\text{MnO}_2$ -NiFe-LDH/CC sample. Compared to Figure 1a, Figure 1d displays aggregated clusters of heterogeneous  $\text{MnO}_2$  clusters on the fiber surface. Upon magnification, these  $\text{MnO}_2$  clusters resemble willow catkins, as seen in Figure 1e. Zooming into the uniformly covered parts of the fibers (indicated by the red box) still reveals interwoven sheets on the carbon fiber surface. However, comparing Figure 1c,f shows that the sheets in Figure 1f appear bent. Based on previous research [26], these bent sheets in Figure 1f can be identified as interlinked  $\text{MnO}_2$  sheet layers that are deposited on top of the NiFe-LDH layer.



**Figure 1.** SEM images at different magnifications of samples: (a–c) NiFe-LDH/CC and (d–f)  $\text{MnO}_2$ -NiFe-LDH/CC.

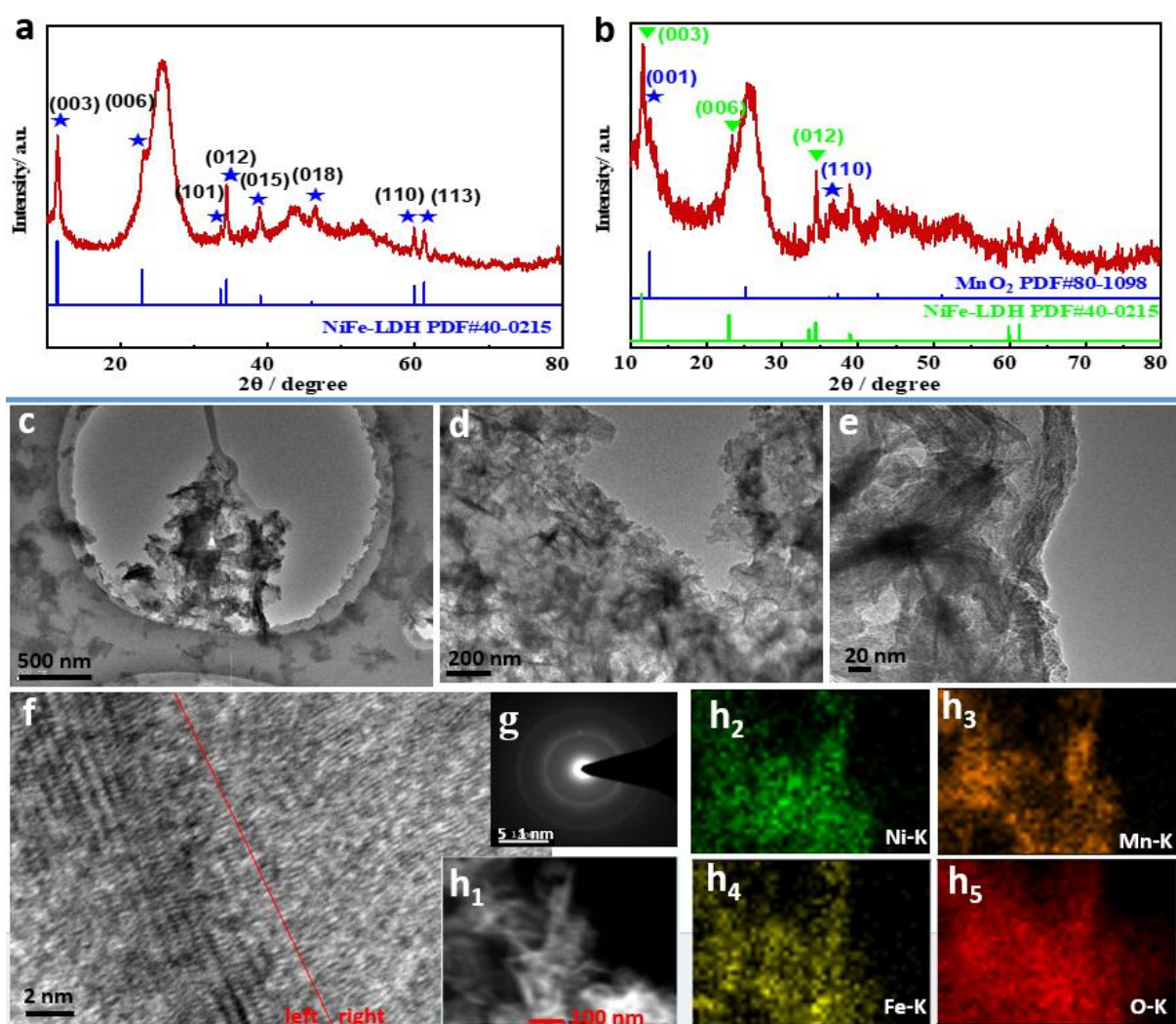
Figure 2a,b presents the X-ray diffraction (XRD) spectra of the prepared samples. In the NiFe-LDH/CC spectrum (Figure 2a), the diffraction peaks observed at  $2\theta$  values of  $11.4^\circ$ ,  $22.9^\circ$ ,  $33.5^\circ$ ,  $34.4^\circ$ ,  $59.9^\circ$ , and  $61.3^\circ$  correspond to the (003), (006), (101), (012), (110), and (113) crystal planes, respectively. These peaks match the standard XRD pattern (PDF#40-

0215) for NiFe-LDH. In the XRD spectrum of the MnO<sub>2</sub>-NiFe-LDH/CC sample (Figure 2b), in addition to the standard NiFe-LDH/CC diffraction peaks, three additional peaks are observed at 2θ values of 12.54°, 25.24°, and 36.22°. These peaks can be attributed to the characteristic peaks of the δ-phase MnO<sub>2</sub> (PDF#80-1098), which indicates that the MnO<sub>2</sub> grown on the CC substrate is in the δ-phase [27–29]. The fine structure of the obtained samples was further characterized using transmission electron microscopy (TEM). The samples were prepared by ultrasonic separation from the nickel foam substrate. The TEM image in Figure S4 in the Supplementary Materials reveals the relatively thin sheets of the NiFe-LDH sample. The high-resolution TEM image displays lattice fringes with a spacing of 0.25 nm, which corresponds to the (012) plane of NiFe-LDH. The TEM image in Figure 2c shows sheet-like structures in the MnO<sub>2</sub>-NiFe-LDH/CC sample over a large area. Enlarged images of the different areas (Figure 2d,e) reveal a lighter color contrast; this indicates relatively thin sheets, which is consistent with the SEM observations. At higher magnification (Figure 2f), some regions of these sheets exhibit high crystallinity, with long lattice fringes observed in the left region that likely originate from the NiFe-LDH. Other areas lacking clear lattice fringes suggest lower crystallinity, which corresponds to MnO<sub>2</sub> sheet structures, based on XRD analysis. This mixed crystalline structure is further supported by the multiple concentric rings observed in the selected area electron diffraction (SAED) pattern (Figure 2g). With the selected area shown in Figure 2h<sub>1</sub>, the elemental mapping of the MnO<sub>2</sub>-NiFe-LDH/CC sample in Figure 2h<sub>2</sub>–h<sub>5</sub> confirms the uniform distribution of Ni, Fe, Mn, and O elements. This demonstrates the homogeneous distribution of all four elements within the MnO<sub>2</sub>-NiFe-LDH/CC sample and affirms the uniform structure of the sheets observed in Figure 2c.

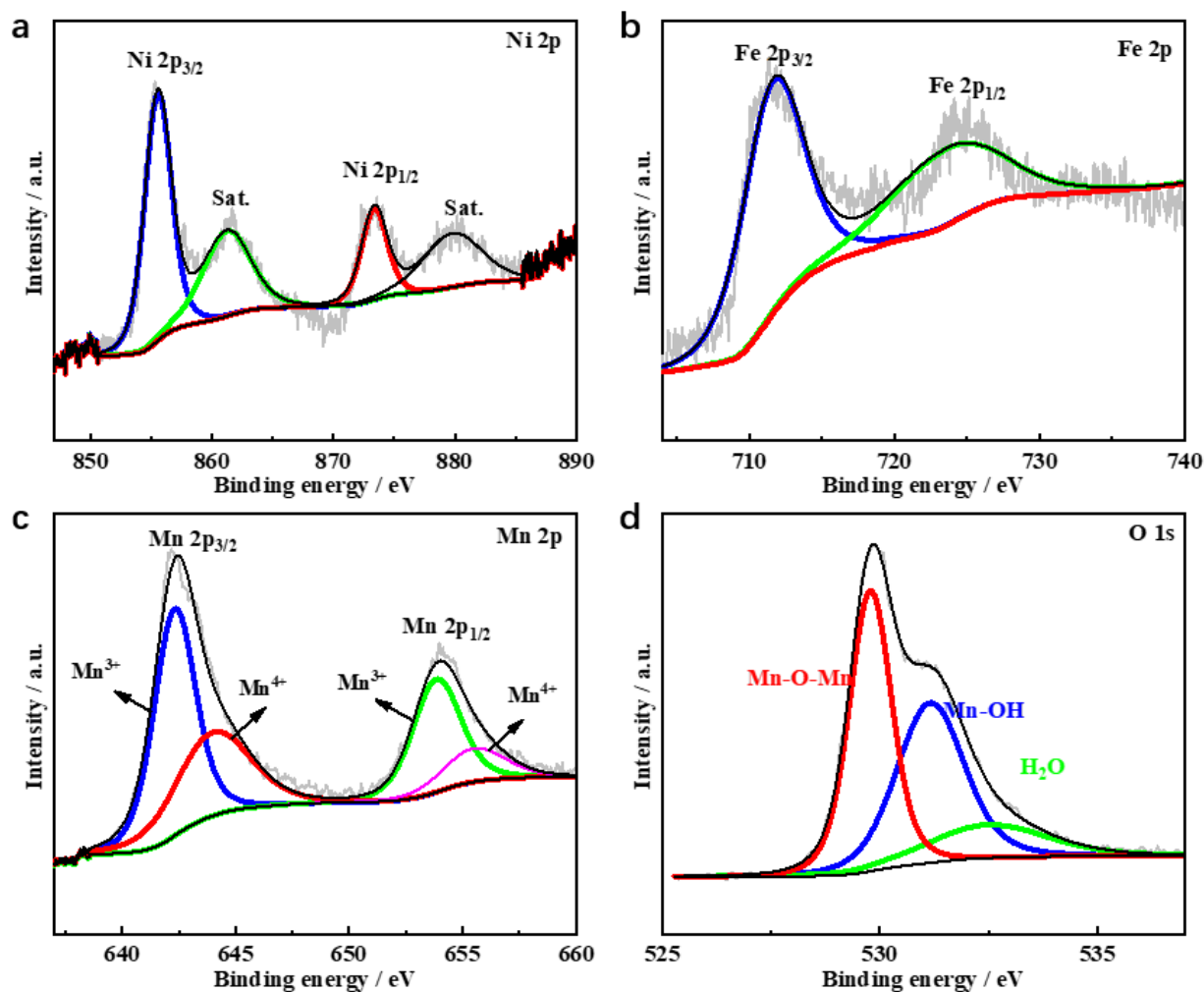
X-ray photoelectron spectroscopy (XPS) was employed to analyze the elemental composition and surface chemical states of the MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol sample (Figure 3). The high-resolution XPS spectrum of Ni 2p (Figure 3a) exhibits characteristic peaks at binding energies of 855.5 eV and 873.4 eV. These correspond to Ni 2p<sub>3/2</sub> and Ni 2p<sub>1/2</sub>, respectively, and imply the presence of the Ni<sup>2+</sup> oxidation state. Two peaks are observed in the Fe 2p XPS spectrum (Figure 3b) at binding energies of 711.6 eV and 723.6 eV, which typify Fe 2p<sub>3/2</sub> and Fe 2p<sub>1/2</sub>, respectively, and indicate the presence of trivalent iron (Fe<sup>3+</sup>) [30–32]. In the Mn 2p XPS spectrum (Figure 3c), the two peaks at 642 eV and 654 eV are attributable to Mn 2p<sub>3/2</sub> and Mn 2p<sub>1/2</sub>, respectively. After convolution fitting of the spin-orbit peaks, four peaks corresponding to the Mn<sup>3+</sup> and Mn<sup>4+</sup> oxidation states are obtained. The peaks at 642.3 eV and 653.8 eV are associated with Mn<sup>3+</sup>, while the peaks at 644.0 eV and 655.5 eV are associated with Mn<sup>4+</sup>. By comparing the peak areas, it is evident that the area for Mn<sup>3+</sup> is larger than that for Mn<sup>4+</sup>, which implies that the Mn is predominantly in the +3-oxidation state. The O 1s spectrum in Figure 3d can be deconvoluted into three peaks corresponding to interlayer oxygen (Mn-O-Mn), adsorbed hydroxyl groups (Mn-OH), and possibly bound water (–H<sub>2</sub>O) [33].

The OER performance of the prepared MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol electrode and the comparative samples was evaluated in a 1.0 M KOH solution. Figure S7a in the Supplementary Materials displays the linear sweep voltammetry (LSV) curves at a scan rate of 5 mV/s, which were measured after multiple cyclic voltammetry (CV) scans to ensure reproducibility. It was observed that the NiFe-LDH/CC sample exhibited the lowest onset potential, and, thus, the highest OER activity among the tested samples. The catalytic performance of the MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol sample for OER was slightly lower than that of the NiFe-LDH/CC sample, which is due to the poor conductivity of the MnO<sub>2</sub> loaded on the surface of NiFe-LDH/CC. Figure S7b presents the overpotential of different catalysts at various current densities. The overpotentials for the MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol composite electrode at current densities of 10 mA·cm<sup>−2</sup> and 100 mA·cm<sup>−2</sup> were 284 mV and 363 mV, respectively. The Tafel slope in Figure S7c was obtained by fitting the corresponding LSV curves in Figure S7a and was used to evaluate the reaction kinetics of the catalytic samples [34–36]. The Tafel slope for the MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol electrode sample (68.6 mV·dec<sup>−1</sup>) was slightly lower than that of the NiFe-LDH/CC

sample, which is consistent with the previously observed trend. Due to poor current response signals from the MnO<sub>2</sub> and the pure CC substrate, their data were not included in the overpotential bar chart and Tafel slope plot. The charge transfer resistance ( $R_{ct}$ ) reflects the kinetics of the OER for the catalyst. Impedance tests were performed at a voltage of 1.48 V (vs. RHE). Figure S7d reveals that the semicircle for the NiFe-LDH/CC sample is the smallest, followed by that of the MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol sample. This indicates that NiFe-LDH/CC has the lowest impedance value; therefore, it correlates with the best OER catalytic performance. This is consistent with the results from the LSV curve analysis. Figure S7e demonstrates the constant current stability of the MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol sample in alkaline seawater. The potential remained stable during 100 h of continuous electrolysis. Figure S7f compares the LSV curves of the electrode material before and after 6000 cycles of CV testing. The slight potential shift of 8 mV to the right suggests that the catalyst maintained long-term stability in alkaline seawater, further demonstrating its durability and effectiveness.



**Figure 2.** XRD patterns of the samples: (a) NiFe-LDH/CC and (b) MnO<sub>2</sub>-NiFe-LDH/CC. (c–f) TEM images at different magnifications, (g) SAED, (h<sub>1</sub>) STEM, and (h<sub>2</sub>–h<sub>5</sub>) elemental mapping of the MnO<sub>2</sub>-NiFe-LDH/CC sample.

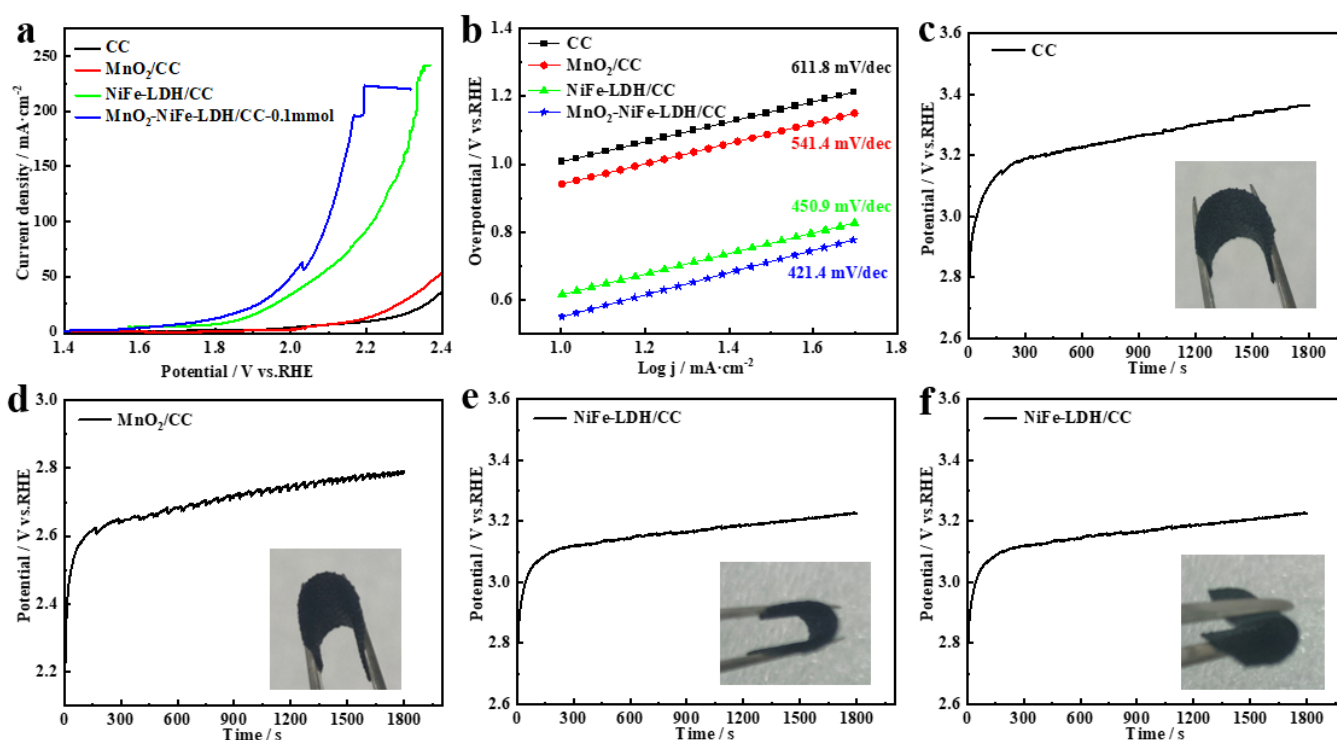


**Figure 3.** The high-resolution XPS spectra of MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol sample: (a) Ni 2p, (b) Fe 2p, (c) Mn 2p, and (d) O 1s.

The electrochemical active surface area (ECSA) of the different catalyst samples was evaluated through double-layer capacitance ( $C_{dl}$ ) measurements. CV tests were conducted at various scan rates (20 mV/s, 40 mV/s, 60 mV/s, 80 mV/s, 100 mV/s, and 120 mV/s) in the non-Faradaic region (0.924–1.024 V vs. RHE). Figure S8a–c shows the CV curves of the CC, MnO<sub>2</sub>/CC, NiFe-LDH/CC, and MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol samples at different scan rates. Figure S8d was obtained after plotting the difference in current density against the scan rate and fitting the data. As can be seen, the  $C_{dl}$  value for MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol is 1.74 mF·cm<sup>-2</sup>, which is lower than the  $C_{dl}$  value of the NiFe-LDH/CC sample (2.38 mF·cm<sup>-2</sup>). The ECSA is proportional to the  $C_{dl}$  and a higher  $C_{dl}$  value indicates a larger electrochemical active area, with more active sites exposed on the catalyst sample [37]. The surface loading of MnO<sub>2</sub> on NiFe-LDH/CC results in the coverage of its active sites and leads to a decrease in the catalytic performance of the OER.

Using natural seawater as the electrolyte, the OER catalytic performance of the prepared electrode samples was studied. Initially, CV scans were performed at a scan rate of 50 mV/s within a potential window from −1 V to 0.2 V to activate the electrode samples. After ensuring the complete overlap of the CV curves, LSV tests were conducted to assess the OER performance under natural seawater conditions (Figure 4). At this point, the sample had been activated in an equilibrium state and was capable of truly reflecting the OER's catalytic performance in the LSV test. As shown in Figure 4a, the LSV tests were conducted at a scan rate of 5 mV/s, using MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol and comparative samples in natural seawater electrolytes. It can be observed that the pure CC

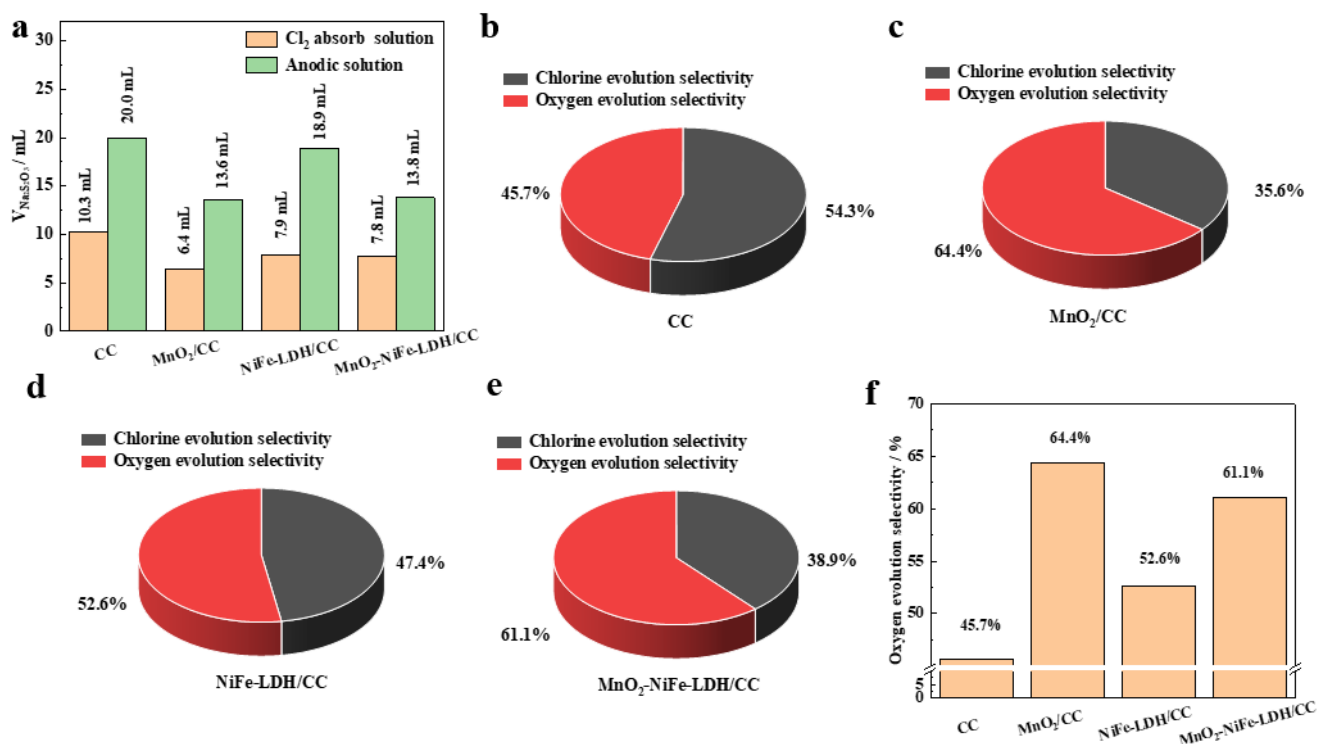
substrate and  $\text{MnO}_2/\text{CC}$  sample exhibited significantly weaker current response signals compared to those from the  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC-0.01}$  mmol and  $\text{NiFe-LDH}/\text{CC}$  samples. More specifically, the  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC-0.01}$  mmol sample showed the lowest onset potential and overpotential out of the four samples, which indicates the superior activity of the OER in seawater electrolytes. The OER performance of the  $\text{NiFe-LDH}/\text{CC}$  sample in seawater was weaker than that of the  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC-0.01}$  mmol sample. This performance contrasts with that observed in alkaline seawater. The reason for this may lie in the fact that during the electrolysis of seawater, the amount of charge available for  $\text{Cl}^-$  oxidation by the  $\text{NiFe-LDH}/\text{CC}$  sample is higher than that for  $\text{Cl}^-$  oxidation by the  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC-0.01}$  mmol sample. The Tafel slopes in Figure 4b were obtained by fitting the LSV curve data. They reveal that the  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC-0.01}$  mmol sample has the smallest Tafel slope value of 421.4 mV/dec, which is significantly higher than the Tafel slope obtained in alkaline seawater. This difference is primarily due to the enhanced kinetics of the OER reaction in strong alkaline electrolytes, where the pH is approximately 14, whereas natural seawater has a pH of around 8. Additionally, in mildly alkaline natural seawater, the presence of abundant  $\text{Cl}^-$  ions leads to chlorine evolution reactions at the anode, and the chlorine gas thus produced may corrode the electrode materials, thereby reducing their OER performance. Figure 4c–f shows the chronoamperometry plots recorded for the CC,  $\text{MnO}_2/\text{CC}$ ,  $\text{NiFe-LDH}/\text{CC}$ , and  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC-0.01}$  mmol samples during constant current electrolysis experiments. The inset images demonstrate that the tested samples can recover their original shape after any deformation caused by external forces.



**Figure 4.** (a) OER LSV of CC,  $\text{MnO}_2/\text{CC}$ ,  $\text{NiFe-LDH}/\text{CC}$ , and  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC-0.01}$  mmol electrode samples in seawater at a scan rate of 5 mV/s. (b) Tafel plots. Constant current curve of samples: (c) CC, (d)  $\text{MnO}_2/\text{CC}$ , (e)  $\text{NiFe-LDH}/\text{CC}$ , and (f)  $\text{MnO}_2\text{-NiFe-LDH}/\text{CC-0.01}$  mmol electrode at a current of 0.1 A.

After constant current electrolysis, titration was conducted on both the anodic and absorptive solutions; the color changes during titration are illustrated in Figure S9a–e in the Supplementary Materials. Upon adding KI solution, the solution turned yellow-brown, and with the addition of  $\text{Na}_2\text{S}_2\text{O}_3$ , the solution gradually lightened. The solution in Figure S9d turned blue because a starch solution was added. The purpose of this addition is to make the color change more noticeable as it approaches the titration endpoint. Figure S9f shows images of the cathodic and anodic regions during constant current electrolysis under seawater electrolyte conditions. In the cathodic region, there was a noticeable formation of white flocculent and precipitate due to the hydrogen evolution reaction ( $2\text{H}_2\text{O} + 2\text{e}^- \rightarrow 2\text{OH}^- + \text{H}_2$ ), wherein  $\text{OH}^-$  ions reacted with the  $\text{Ca}^{2+}$  and  $\text{Mg}^{2+}$  ions present in seawater to form precipitates. Before conducting the experiment, it is crucial to ensure that the setup is well-sealed. A tube connected the anodic region to the  $\text{Cl}_2$  absorption device, as shown in Figure S9g.  $\text{Cl}_2$  gas produced at the anode reacts with  $\text{NaOH}$  in the absorption device ( $2\text{NaOH} + \text{Cl}_2 = \text{NaCl} + \text{NaClO} + \text{H}_2\text{O}$ ) and results in the formation of  $\text{ClO}^-$ . By recording the volume of  $\text{Na}_2\text{S}_2\text{O}_3$  solution consumed during the titration, the amount of charge required for the oxidation of  $\text{Cl}^-$  to  $\text{Cl}_2$  in the anode solution can be calculated. Similarly, titration of the anodic solution is necessary to determine the amount of charge required for the oxidation of  $\text{Cl}^-$  to  $\text{ClO}^-$  in the anode solution. By combining the titration results of the  $\text{Cl}_2$  absorption solution and the anodic solution, the total charge consumed during electrolysis and the charge used for  $\text{Cl}$  oxidation can be determined. The ratio of the charge consumed for oxygen evolution to the total charge during constant current electrolysis gives the oxygen evolution selectivity.

During the titration process, the volumes of  $\text{Na}_2\text{S}_2\text{O}_3$  solution consumed in the anodic region and the  $\text{Cl}_2$  absorption region were recorded, as depicted in Figure 5a. The  $\text{MnO}_2$ -modified  $\text{NiFe-LDH/CC}$  sample consumed less  $\text{Na}_2\text{S}_2\text{O}_3$  solution volume compared to its precursor. Figure 5b–e shows the proportions of OER and chlorine evolution reaction (CIER) for the four electrode samples in natural seawater, while Figure 5f presents the oxygen evolution selectivity of these samples. Experimental data indicated that the composite  $\text{MnO}_2\text{-NiFe-LDH/CC-0.01}$  mmol electrode sample exhibited an oxygen evolution selectivity of 61.1% in natural seawater, which was approximately 10% higher than the  $\text{NiFe-LDH/CC}$  sample. As shown in Figure S10, the presence of  $\text{MnO}_2$  in the  $\text{MnO}_2\text{-NiFe-LDH/CC}$  sample enhanced the  $\text{OH}^-$  adsorption capacity and reduced the  $\text{Cl}^-$  adsorption capacity compared to the  $\text{NiFe-LDH/CC}$  sample. This led to increased oxygen generation and improved oxygen evolution selectivity. This suggests that in natural seawater, the actual OER efficiency of the  $\text{MnO}_2\text{-NiFe-LDH/CC-0.01}$  mmol sample was greater than that of the  $\text{NiFe-LDH/CC}$  sample. The variation in OER performance between alkaline seawater and natural seawater electrolytes can be attributed to the different oxygen evolution selectivity of these two samples. Moreover, the higher oxygen evolution selectivity of the  $\text{MnO}_2/\text{CC}$  sample compared to pure  $\text{CC}$  substrate indicates that loading  $\delta\text{-MnO}_2$  is beneficial for catalytic materials that are used in natural seawater electrolysis conditions.



**Figure 5.** (a) The electrode material consumes a volume of  $\text{Na}_2\text{S}_2\text{O}_3$  during titration. The ratios of oxygen and chlorine evolution in electric natural seawater samples: (b) CC, (c)  $\text{MnO}_2/\text{CC}$ , (d) NiFe-LDH/CC, and (e)  $\text{MnO}_2\text{-NiFe-LDH/CC}$  electrode samples. (f) Oxygen evolution selectivity of the electrode materials in natural seawater.

### 3. Experiments

#### 3.1. Preparation of the NiFe-LDH/CC Sample

Typically, 0.66 mmol of  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ , 0.33 mmol of  $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$ , 2 mmol of  $\text{NH}_4\text{F}$ , and 5 mmol of  $\text{CO}(\text{NH}_2)_2$  were dissolved in 25 mL of deionized water. The mixture was stirred for 10 min before being transferred to a reactor. Then, a piece of pre-treated CC with dimensions of  $2 \times 3 \text{ cm}^2$  was added. Subsequently, the reactor was heated up to  $120^\circ\text{C}$  and maintained at that temperature for 6 h. Afterward, the sample was collected and washed ultrasonically to remove any yellow-green precipitate on the surface. Lastly, the sample was dried in a vacuum oven at  $60^\circ\text{C}$  and labeled as NiFe-LDH/CC.

#### 3.2. Preparation of the $\text{MnO}_2\text{-NiFe-LDH/CC}$ Sample

First, 0.1 mmol of  $\text{KMnO}_4$  was dissolved in 50 mL of deionized water under stirring at room temperature. The solution turned a clear purple-red after approximately 10 min. Then, the solution was transferred to a reactor and a piece of pre-treated NiFe-LDH/CC sample ( $2 \times 3 \text{ cm}^2$ ) was added. The reactor was heated up to  $120^\circ\text{C}$  and the temperature was maintained for 3 h. After the reaction, a brown precipitate was observed on the surface of the prepared catalytic sample. Subsequently, the sample was washed thoroughly with deionized water to remove any residual precipitate. Finally, the electrode sample was dried in a vacuum oven at  $60^\circ\text{C}$  and labeled as  $\text{MnO}_2\text{-NiFe-LDH/CC}$ -0.1 mmol.

For comparative purposes, the amounts of  $\text{KMnO}_4$  varied, at 0.05 mmol, 0.03 mmol, 0.01 mmol, 0.005 mmol, and 0.001 mmol under the same conditions. The obtained samples were labeled as  $\text{MnO}_2\text{-NiFe-LDH/CC}$ -0.05 mmol,  $\text{MnO}_2\text{-NiFe-LDH/CC}$ -0.03 mmol,  $\text{MnO}_2\text{-NiFe-LDH/CC}$ -0.01 mmol,  $\text{MnO}_2\text{-NiFe-LDH/CC}$ -0.005 mmol, and  $\text{MnO}_2\text{-NiFe-LDH/CC}$ -0.001 mmol, respectively.

#### 4. Conclusions

In this work, a MnO<sub>2</sub>-NiFe-LDH/CC electrode sample was prepared to investigate its oxygen evolution reaction (OER) catalytic performance and oxygen evolution selectivity in natural seawater. In the alkaline seawater electrolyte, the optimized MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol electrode sample exhibited overpotentials of 284 mV and 363 mV at current densities of 10 mA·cm<sup>-2</sup> and 100 mA·cm<sup>-2</sup>, respectively, with a Tafel slope of 68.6 mV·dec<sup>-1</sup>. Additionally, the OER catalytic performance of this sample showed no significant degradation after 120 h of electrochemical testing. In natural seawater, the MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol sample demonstrated an oxygen evolution selectivity of 61.1%, which is superior to that of the NiFe-LDH/CC sample. This indicates that MnO<sub>2</sub> modification enhances the oxygen evolution competitiveness of the electrode material in seawater electrolysis. The study reveals MnO<sub>2</sub>'s potential to improve the oxygen evolution efficiency of catalysts under natural seawater conditions.

**Supplementary Materials:** The following supporting information can be downloaded at: <https://www.mdpi.com/article/10.3390/catal14080502/s1>, Figure S1. Schematic illustration of the preparation of the MnO<sub>2</sub>-NiFe-LDH/CC sample; Figure S2. (a) OER LSV of the different loads of the MnO<sub>2</sub>-NiFe-LDH/CC electrodes in alkaline seawater at a scan rate of 5 mV/s, (b) OER overpotential values at of 10 and 100 mA·cm<sup>-2</sup>, and (c) Tafel plots; Figure S3. SEM image of the CC substrate; Figure S4. (a–c) TEM images and (i) element mapping of the NiFe-LDH/CC sample; Figure S5. (a) Survey XPS spectrum of the NiFe-LDH/CC sample, with the deconvoluted high-resolution XPS spectra of (b) Ni 2p and (c) Fe 2p; Figure S6. (a) Survey of the XPS spectrum and (b) atomic percentage in the MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol sample; Figure S7. (a) OER LSV images for the CC, MnO<sub>2</sub>/CC, NiFe-LDH/CC, and MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol electrode samples in alkaline seawater at a scan rate of 5 mV/s. (b) OER overpotential values of 50 and 100 mA·cm<sup>-2</sup>. (c) Tafel plots. (d) EIS spectra of CC, MnO<sub>2</sub>/CC, NiFe-LDH/CC, and MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol samples. (e) Long-term chronopotentiometry of MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol samples under 10 mA·cm<sup>-2</sup> for 100 h. (f) OER LSVs of the 1st and 6000th cycle on the MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol sample in alkaline seawater at a scan rate of 5. mV/s; Figure S8. CV curves at different scan rates in the alkaline seawater solution of the samples: (a) CC, (b) MnO<sub>2</sub>/CC, (c) MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol, and (d) MnO<sub>2</sub>-NiFe-LDH/CC-0.01 mmol and other catalysts; Figure S9. (a–e) Corresponding color changes during the titration. (f) State changes of the anode and cathode during constant current electrolysis. (g) The device that absorbs the chlorine gas; Figure S10. The schematic diagram illustrates the underlying synergetic effects and catalytic mechanisms of the NiFe-LDH/CC and MnO<sub>2</sub>-NiFe-LDH/CC samples.

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