

## Article

# Machine Learning-Based Approach for Modeling the Nanofluid Flow in a Solar Thermal Panel in the Presence of Phase Change Materials

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**Abstract:** Considering the importance of environmental protection and renewable energy resources, particularly solar energy, the present study investigates the temperature control of a solar panel using a nanofluid (NFD) flow with eco-friendly nanoparticles (NPs) and a phase change material (PCM). The PCM was used under the solar panel, and the NFD flowed through pipes within the PCM. A number of straight fins (three fins) were exploited on the pipes, and the output flow temperature, heat transfer (HTR) coefficient, and melted PCM volume fraction were measured for different pipe diameters (D<sub>Pipe</sub>) from 4 mm to 8 mm at various time points (from 0 to 100 min). Additionally, with the use of artificial intelligence and machine learning, the best conditions for obtaining the lowest panel temperature and the highest output NFD temperature at the lowest pressure drop have been determined. While the porosity approach was used to model the PCM melt front, a two-phase mixture was used to simulate NFD flow. It was discovered that the solar panel temperature and output temperature both increased considerably between t = 0 and t = 10 min before beginning to rise at varying rates, depending on the D<sub>Pipe</sub>. The HTR coefficient increased over time, showing similar behavior to the panel temperature. The entire PCM melted within a short time for D<sub>Pipes</sub> of 4 and 6 mm, while a large fraction of the PCM remained un-melted for a long time for a D<sub>Pipe</sub> of 8 mm. An increase in D<sub>Pipe</sub>, particularly from 4 to 6 mm, reduced the maximum and average panel temperatures, leading to a lower output flow temperature. Furthermore, the increased D<sub>Pipe</sub> reduced the HTR coefficient, with the PCM remaining un-melted for a longer time under the panel.

**Keywords:** solar energy; machine learning; collector; eco-friendly nanoparticles; PCM

## 1. Introduction

Today, many countries are struggling with climate change and its consequent environmental impacts. Precipitation reduction and widespread droughts, floods, and hurricanes result from climate change. Global warming is a major explanation for such changes, and massive efforts are required to avoid further temperature increases across the world [1–4]. The excessive emission of CO<sub>2</sub> after the Industrial Revolution has led to climate change and global warming. Industrial and residential energy accounts for a significant portion

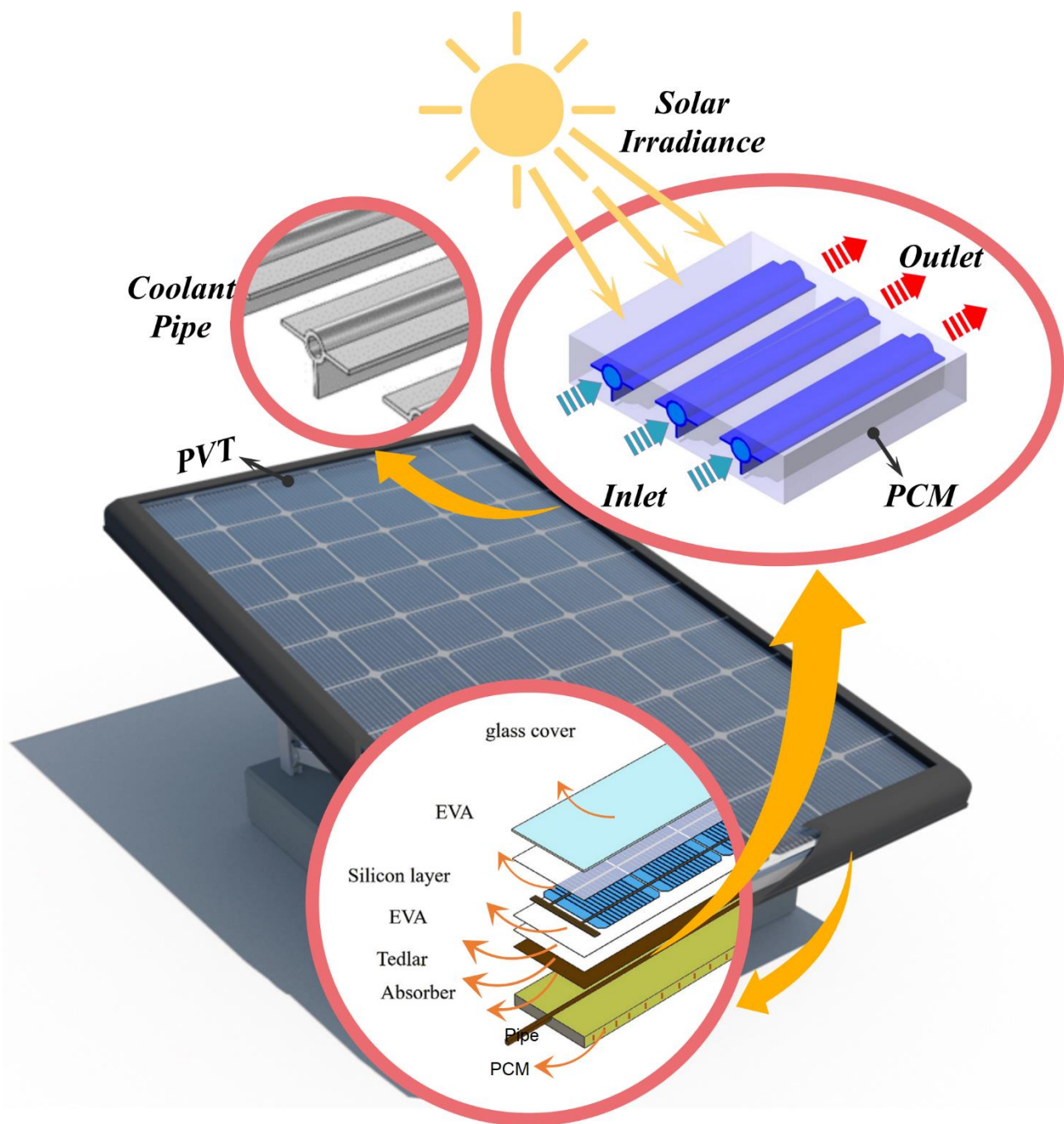
of CO<sub>2</sub> emissions [5–9]. The replacement of traditional energy resources with renewable, clean energy could substantially help reduce CO<sub>2</sub> emissions [10–13]. Today, attention has been paid to the topic of HTR [14,15]. Specifically, solar energy has been of great interest to researchers, and many researchers assume solar energy to be an effective substitute for traditional energy resources [16–19]. Solar panels can be employed to harvest solar energy [20–24]. Solar thermal panels can be more effective for solar energy harvesting since they can generate hot water and can maximize panel efficiency [25–29]. Several researchers studied solar thermal panels [30–34]. By using a thermosyphon–heat pipe combination with water-cooling jackets beneath the PV modules to absorb extra heat from the solar cells, Moradgholi et al. [35] devised a photovoltaic thermal (PVT) system. They reported a 26% reduction in the PV cell temperature. Nizatik et al. [36] employed water spraying to cool PV modules (in the front, in the back, and both in the front and back) in outdoor settings in Croatia. It was found that water spraying in the front, back, and both front and back reduced the solar module temperature by 42.8%, 58.9%, and 60.7%, respectively.

NFDs have been widely employed in thermal devices [37–41]. A NFD is made up of base fluid with NPs. Research has shown that NFDs significantly enhance HTR [42–46]. Jingio et al. [47] theoretically studied the performance of Fe<sub>2</sub>O<sub>3</sub> NFDs as an optical filter on a silicon PV panel. The optimal volume fraction of Fe<sub>2</sub>O<sub>3</sub> NPs for the NFD with a base fluid mixture of 50% water and 50% ethylene glycol was found to be  $5 \times 10^{-4}\%$ . A passive cooling method was suggested by Chandereskar et al. [48] to cool PV modules. On the back of the PV modules, a cotton wick and several NFDs made up the system. The tests were carried out in the climate of an Indian city in April. It was found that the use of a cotton wick and water, a cotton wick and a CuO/water NFD, and a cotton wick and an Al<sub>2</sub>O<sub>3</sub>/water NFD led to 30%, 11%, and 17% temperature reductions, respectively.

Today, it is necessary to protect the environment for future generations. Environmental deterioration in the past decades has led to significant climate change and the extinction of some species [49–52]. The destruction of the environment would destroy human life [53–55]. Hence, environmental revival is important for countries and the United Nations (UN). Substantial CO<sub>2</sub> emissions pose a serious threat to human life. The use of clean and renewable energy in place of fossil fuels to reduce CO<sub>2</sub> emissions is an effective approach to environmental protection. Solar energy could be a promising alternative for future energy generation as it is simple, renewable, and non-polluting. The use of phase change material can also help with the efficiency of heating devices [56–60]. In this work, a NFD containing eco-friendly NPs and a phase change material (PCM) at the same time is used to adjust the temperature of a solar panel. It was presumed that the NFD was a two-phase system. The PCM and a number of pipes with fins were employed under the solar panel to control its temperature. This study assumed a transient system and analyzed the effects of D\_Pipe on the panel temperature, output NFD temperature, and melted PCM volume fraction. It should be noted that eco-friendly NPs were fabricated through tea leaf extracts to implement an even more eco-friendly solar system. In summary, the use of eco-friendly NFD in the PV-thermal panel, the use of PCM in the system, and the examination of the impact of changing the tube diameter on the outputs can be considered innovations of the present work.

## 2. Problem Statement

The system consisted of a solar panel with a size of 54 × 67 cm, under which a PCM of the same size was employed. Three pipes with a laminar NFD flow at a velocity of 1 mm/s were used within the PCM. Three straight rectangular copper fins were used on the pipes. As mentioned, the eco-friendly NPs were fabricated using tea leaf extracts. The D\_Pipe varied from 4 to 8 mm. The solar panel received a constant 850 W/m<sup>2</sup> solar heat flow for 100 min. The system's schematic is shown in Figure 1.



**Figure 1.** Schematic of the system with PCM and NFD flow pipe.

### 3. Governing Equations

#### 3.1. NFD

The governing equations of an incompressible NFD for a two-phase mixture are written as follows [61]:

Conservation of mass

$$\nabla \cdot (\rho_m \vec{v}_m) = 0 \quad (1)$$

Conservation of momentum

$$\nabla \cdot (\rho_m \vec{v}_m \cdot \nabla \vec{v}_m) = -\nabla P_m + \nabla \cdot (\mu_m \nabla \vec{v}_m) + \nabla \cdot \left( \sum_{k=1}^n \varphi_k \rho_k \vec{v}_{dr,k} \vec{v}_{dr,k} \right) \quad (2)$$

Conservation of energy

$$\nabla \cdot \left( \sum_{k=1}^n \varphi_k \rho_k c_{p,k} \vec{v}_k T \right) = \nabla \cdot (k_m \nabla T) \quad (3)$$

where  $\vec{v}$  and  $P$  denote the velocity and pressure, respectively. Furthermore,  $\rho$  is the density,  $\mu$  is the viscosity,  $T$  is the temperature,  $k$  is the conductivity,  $c_p$  is the specific heat capacity, and subscription  $m$  represents the mixture. The average mixture velocity, density, viscosity, and volume fraction are given by the following:

$$\vec{v}_m = \frac{\sum_{k=1}^n \varphi_k \rho_k \vec{v}_k}{\rho_m} \quad (4)$$

$$\rho_m = \sum_{k=1}^n \varphi_k \rho_k \quad (5)$$

$$\mu_m = \sum_{k=1}^n \varphi_k \mu_k \quad (6)$$

$$\nabla \cdot (\varphi_p \rho_p \vec{v}_m) = -\nabla \cdot (\varphi_p \rho_p \vec{v}_{dr,p}) \quad (7)$$

The drift velocity of eco-friendly NPs is written as follows:

$$\vec{v}_{dr,k} = \vec{v}_{pf} - \sum_{i=1}^n \frac{\varphi_i \rho_i}{\rho_m} \vec{v}_{fi} \quad (8)$$

The slip velocity is defined as follows:

$$\vec{v}_{pf} = \vec{v}_p - \vec{v}_f \quad (9)$$

$$\vec{v}_{pf} = \frac{\rho_p d_p^2 (\rho_p - \rho_m)}{18 \mu_f f_{drag} \rho_p} a \quad (10)$$

$$f_{drag} = \begin{cases} 1 + 0.15 Re_p^{0.687}, & Re_p \leq 1000 \\ 0.0183 Re_p^{0.687}, & Re_p > 1000 \end{cases} \quad (11)$$

where  $p$  and  $f$  refer to eco-friendly NPs and the base fluid, respectively. The gravitational acceleration is defined as follows:

$$a = g - (\vec{v}_m \cdot \nabla) \vec{v}_m \quad (12)$$

Table 1 reports the basic properties of the base fluid and eco-friendly NPs.

**Table 1.** The basic properties of the base fluid and eco-friendly NPs [62].

	$c_p$ (J/kg·K)	$k$ (W/m·K)	$\mu$ (kg/m·s)	$\rho$ (kg/m <sup>3</sup> )
EG	2430.8	0.2532	0.0141	1088
Ag	235	429	-	10,500
Water	4179	0.613	0.001	997.1

### 3.2. PCM

The governing equations of the PCM are written as follows:

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{U}) = 0 \quad (13)$$



$$\frac{\partial}{\partial t}(\rho \vec{U}) + \nabla \cdot (\rho \vec{U} \vec{U}) = -\vec{\nabla} p + \rho \vec{g} + \nabla \cdot \vec{\tau} + \vec{F} \quad (14)$$

$$\frac{\partial(\rho H)}{\partial t} + \nabla \cdot (\rho \vec{U} H) = \nabla \cdot (K \nabla H) + S \quad (15)$$

The function  $\beta$  is defined as follows [62]:

$$\beta_k = \begin{cases} \beta = 0 & \text{if } T < T_{solidus} \\ \beta = 1 & \text{if } T > T_{Liquidus} \\ \beta = \frac{T - T_{solidus}}{T_{Liquidus} - T_{solidus}} & \text{if } T_{Liquidus} < T < T_{solidus} \end{cases} \quad (16)$$

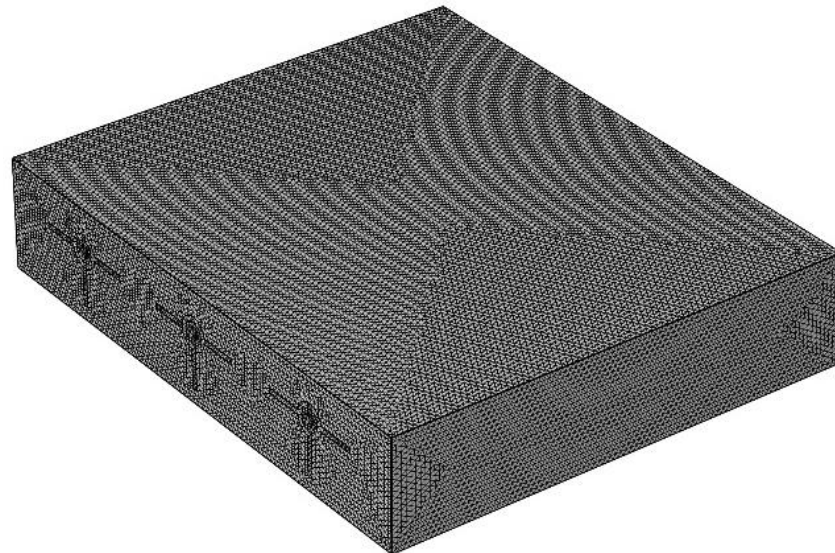
The  $\beta$ -function represents the phase change of the PCM [62]. The specific heat capacity of the system is obtained as follows:

$$\Delta C_{P(System)} = C_{P(np\text{cm})} + L \times D(T) \quad (17)$$

Paraffin wax was used as the PCM with a conductivity of 0.365 W/m.K, a latent heat of 202.1 J/g, and a melting point of 27.7 °C [63].

#### 4. Numerical Method, Grid Study, and Validation

By discretizing the equations, the finite element approach was used to address the PCM melting and NFD flow problems [64]. The two-phase mixing technique was utilized to simulate the flow. The enthalpy method was used to resolve the PCM melt front. The optimal conditions for having a panel with the lowest temperature and having a NFD at the output with the highest temperature and the lowest pressure drop in the solar system were investigated using machine learning in order to more thoroughly examine the effect of parameters on the outputs. Design Expert software was used for this purpose. The domain was meshed using hexagonal pieces, as shown in Figure 2.



**Figure 2.** Meshed domain with hexagonal elements.

Finer meshes were used in areas with larger temperature gradients. The sensitivity of the output to the number of meshes was analyzed. Table 2 shows the output flow temperature at different numbers of meshes and for a D\_Pipe of 6 mm. The ideal grid for the simulations was chosen, which has a total of 1,145,000 components.

**Table 2.** Output flow temperature for a D\_Pipe of 6 mm.

Element Number	911,000	1,027,000	1,145,000	1,283,000
T-out	300.41	300.68	300.80	300.81

The proposed model was validated by simulating the NFD flow through a helical pipe [65]. Two-phase NFD mixture maximization was employed. Table 3 compares the enhancement of the HTR coefficient by the proposed method and that by the method of Bizhaem and Abbasi (65) for a D\_Pipe of 50 and three volume fractions at Reynolds numbers of 200 and 500.

**Table 3.** Proposed model versus the method of Bizhaem and Abbasi [65].

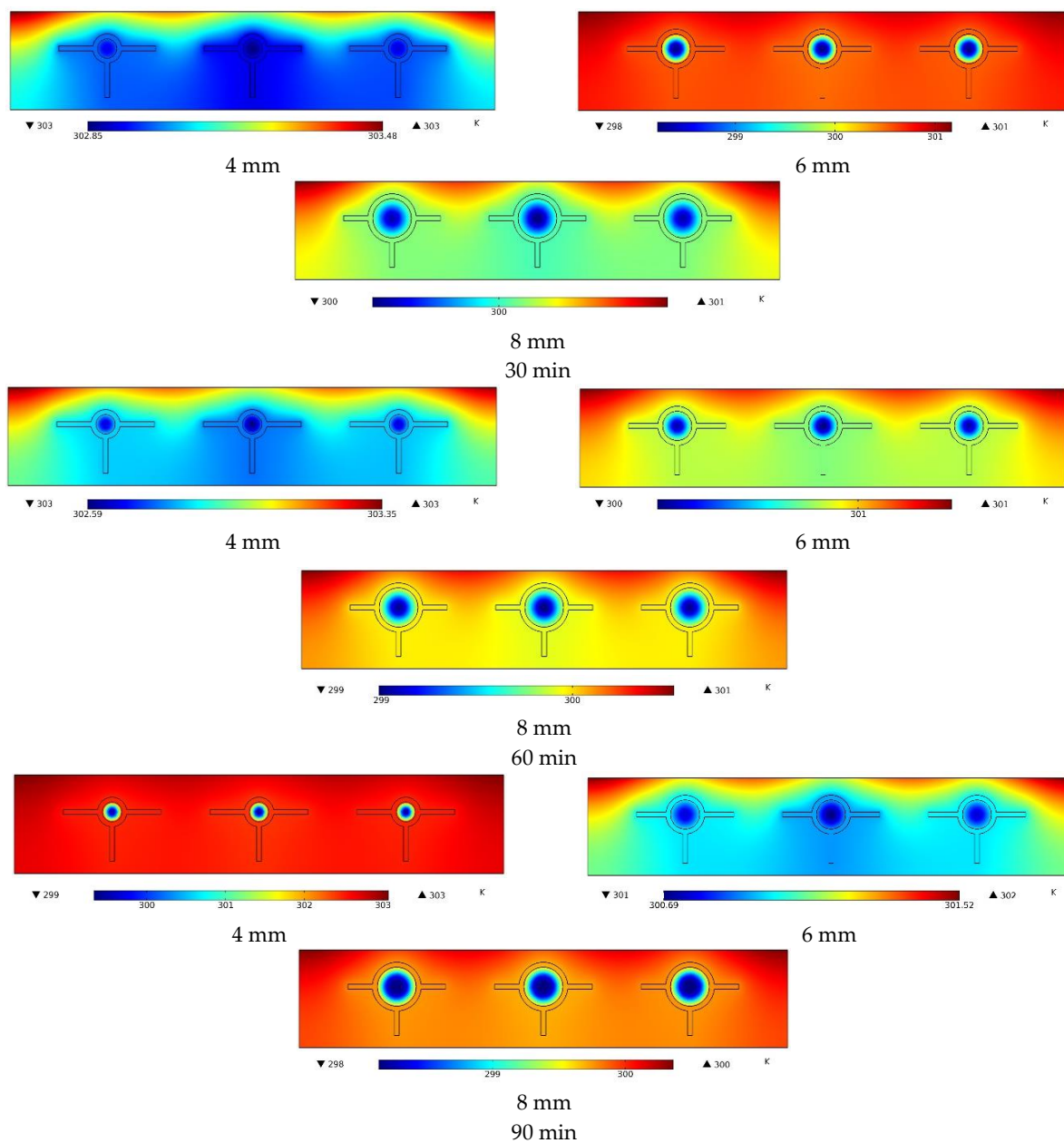
$\varphi$	1%	2%	3%
	Re = 200		
Bizhaem and Abbasi (65)	22.86	29.17	33.48
Present study	22.19	28.78	32.89
	Re = 500		
Bizhaem and Abbasi (65)	7.93	13.92	18.53
Present study	7.59	13.12	18.09

## 5. Results and Discussion

The effect of a change in the diameter of the tube, ranging from 4 to 8 mm, on the temperature of the panel and changes in the volume fraction of a PCM within 100 min are examined in this section. In all cases, the value of the NFD flow rate at the inlet is constant and the number of fins is three. Additionally, the temperature of the NFD at the inlet is considered to be constant. It is noteworthy that the NFD flow in the tubes improves HTR due to the higher thermal conductivity of NFDs compared to normal fluids. Since it has been proven by many researchers, changes in the volume percentage of NPs are not considered in the present work and the volume percentage of NPs is assumed to be 1%.

Figure 3 shows the temperature contour in a vertical cross section of the middle portion of the panel at  $t = 30, 60,$  and  $90$  min for D\_Pipes of 4, 6, and 8 mm. In general, the temperature of the panel somewhat increased over time, particularly for a diameter of 4 mm. Due to the poor NFD flow in pipes with a diameter of 4 mm, the PCM melted within a short time, with the temperatures of both the PCM and panel rising at the same time. An increase in the D\_Pipe to 8 mm better controlled the temperature of the panel and reduced the temperature increase; the colder part of the pipe covered a larger area of the PCM, and the top of the pipe and the solar panel had higher temperatures. The PCM temperature was controlled thanks to the higher flow rate via the 8 mm pipe, with a greater percentage of the PCM staying un-melted.

For widths of 4, 6, and 8 mm throughout the course of 100 min, Figure 4 shows the average panel temperature. The panel temperature with a fixed solar heat flux (irradiance) increased from  $t = 0$  to  $t = 100$  s, particularly during the first ten minutes. The temperature of the panel rose as a result of sun radiation. The panel temperature was lowered using the PCM and NFD flow. The highest and lowest panel temperatures occurred for pipe sizes of 4 and 8 mm, respectively. A smaller D\_Pipe led to a higher panel temperature. Furthermore, the PCM was effective in panel temperature control, and it could control the temperature of the panel as long as it remained un-melted. The PCM also allows for providing hot water during periods when irradiance is poor.



**Figure 3.** The temperature profile for pipes with diameters of 4, 6, and 8 mm at time intervals of 30, 60, and 90 min.

The highest panel temperature for D Pipes of 4, 6, and 8 mm is shown in Figure 5 as a function of time. The D Pipe influenced the maximum panel temperature, and as the D Pipe increased, the maximum temperature fell. In particular, an increase in the diameter from 4 to 6 mm dramatically decreased the maximum temperature of the panel. The maximum panel temperature increased over time due to solar radiation exposure. The heat was stored in the form of latent heat in the PCM or discharged by the NFD so that the panel temperature would not increase. The maximum panel temperature was very high for a D\_Pipe of 4 mm due to the poor NFD flow and faster PCM melting. For a diameter of 8 mm, however, the stronger flow and un-melted PCM kept the maximum panel flow low for a longer time. The fluid flow under the solar panel was used to reduce its temperature and the temperature of the fluid to increase. The HTR between the fluid flow and the panel caused the temperature of the panel to decrease and the temperature of the fluid to increase. A fluid with a greater thermal conductivity might increase the amount of heat it transfers to the panel. Therefore, a NFD was utilized instead of normal fluids to improve HTR and to ultimately reduce the panel temperature.

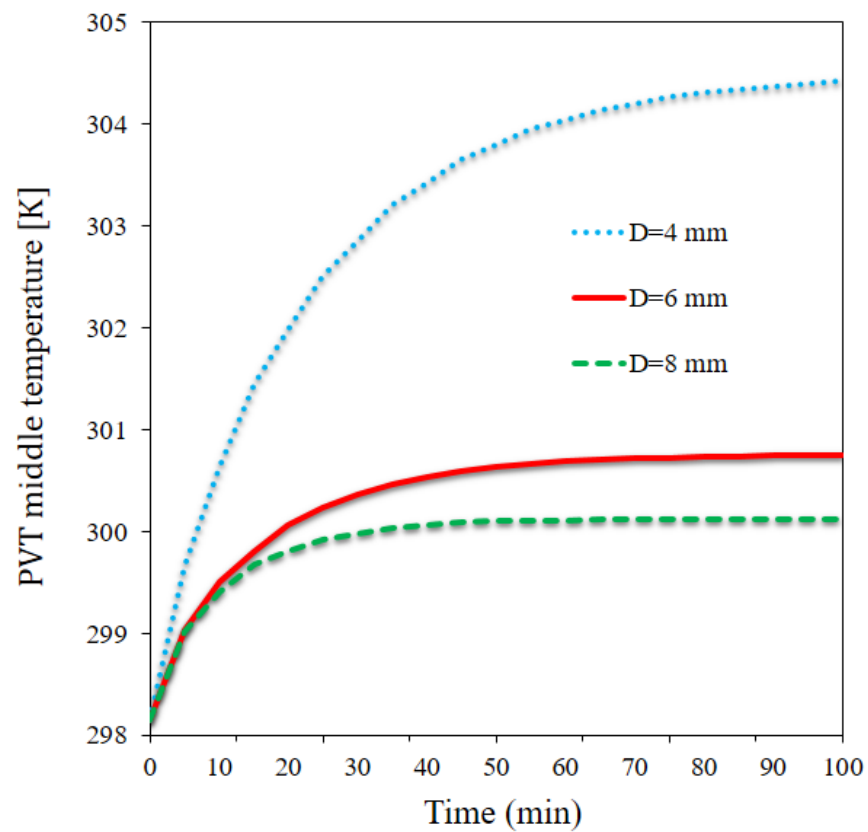


Figure 4. The average panel temperature for diameters of 4, 6, and 8 mm for 100 min.

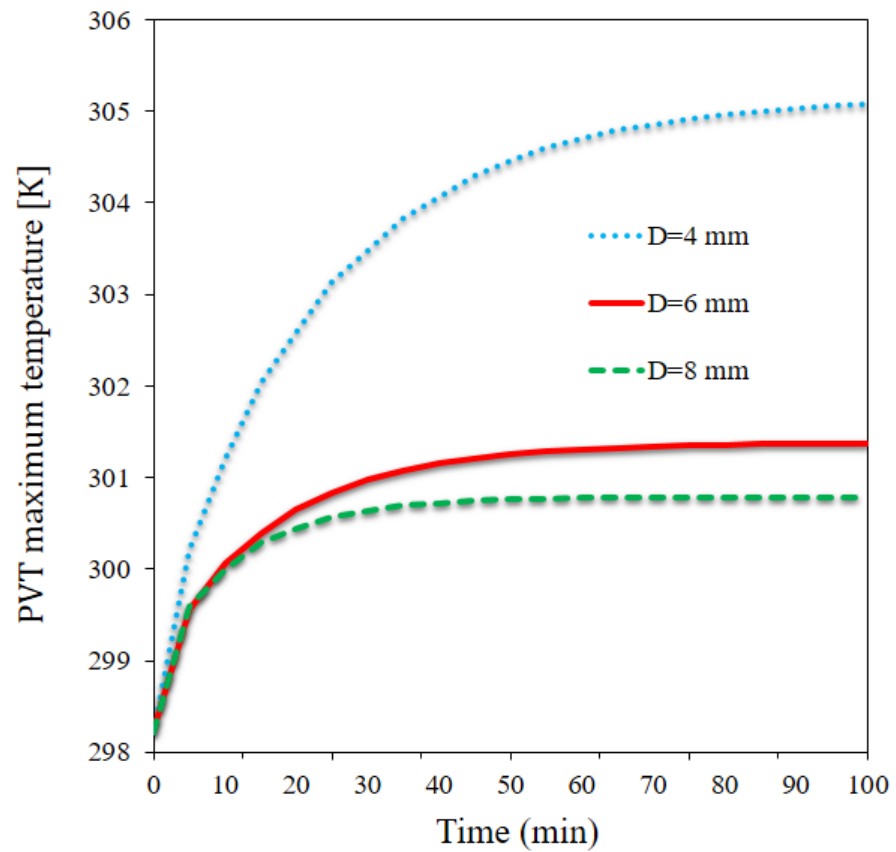
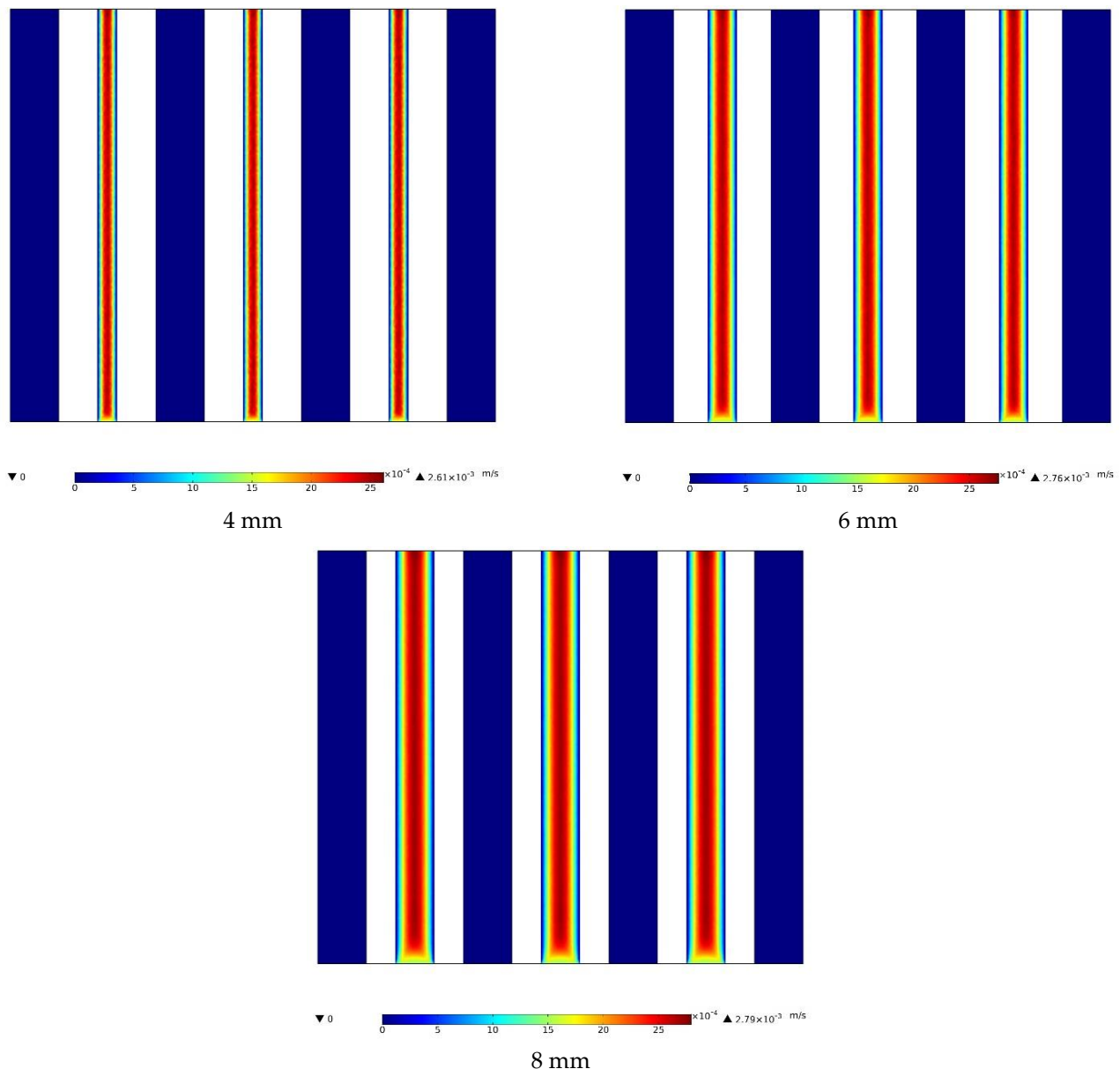


Figure 5. The maximum panel temperature for D\_Pipes of 4, 6, and 8 mm over time.



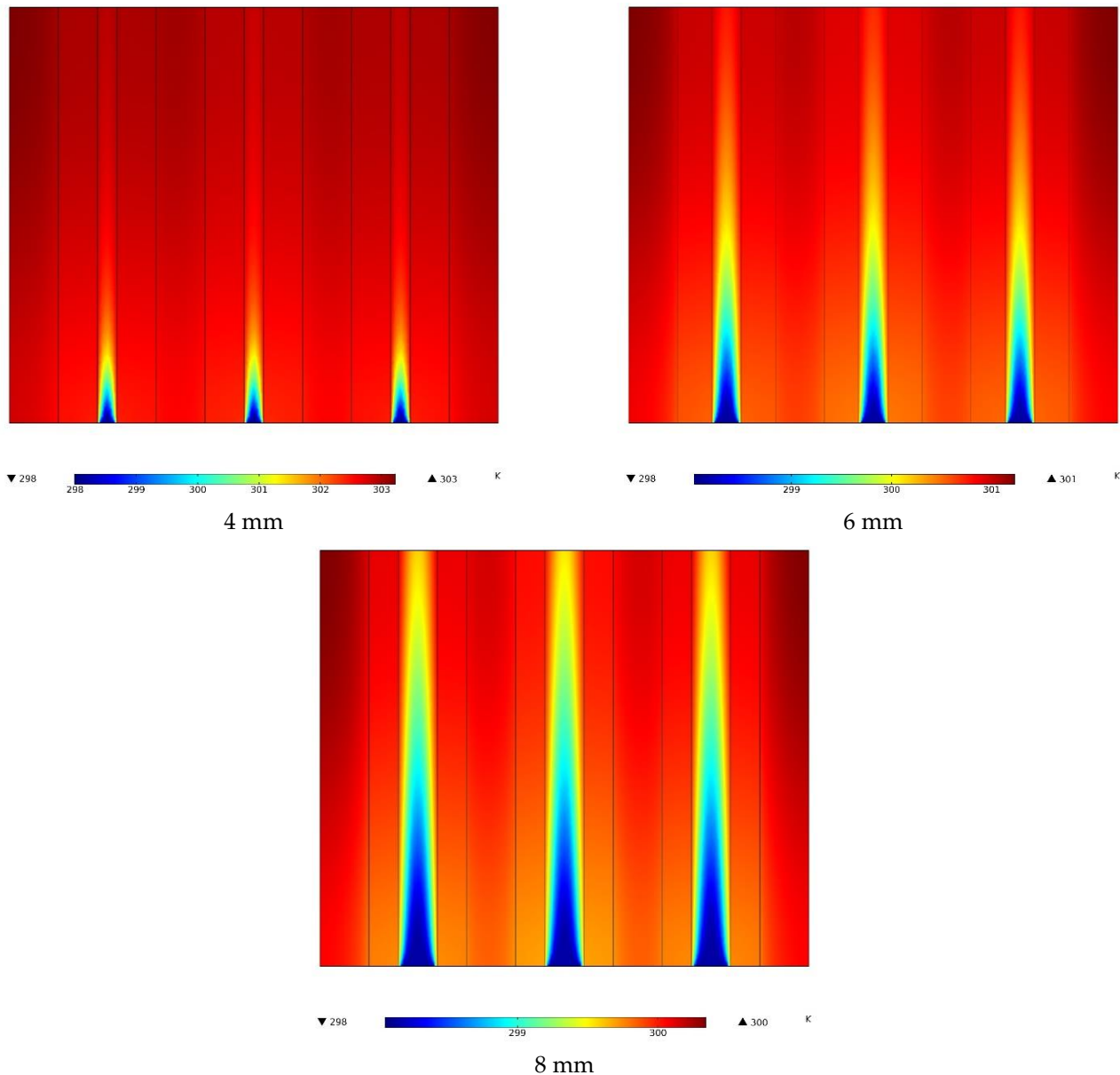
Figure 6 shows the velocity profile for pipes with diameters of 4, 6, and 8 mm in a horizontal cross section of the center of a panel. An underdeveloped flow regime was present at the pipe wall when the NFD entered the channel at a constant speed. However, the flow profile developed within a short distance. For a larger diameter, due to the larger pipe cross-sectional area and fixed input velocity, the NFD flowed through the pipe at a greater rate and absorbed and discharged more heat. However, for smaller D\_Pipes, the fluid had fewer collisions with the wall in the middle of the pipe, leading to a lower output temperature.



**Figure 6.** The velocity contour of the horizontal cross section of the middle portion of the panel for D\_Pipes of 4, 6, and 8 mm.

Figure 7 displays the temperature contours for D Pipes of 4, 6, and 8 mm for the horizontal cross section of the middle area of the panel. The cold NFD flowed into the pipe at a constant temperature and experienced an increase in temperature through the pipe due to collisions with the pipe wall. The pipe absorbed heat from the surrounding PCM. The PCM underwent a temperature increase upon contact with the solar panel under solar irradiation. The PCM temperature was low until it began melting, increasing the

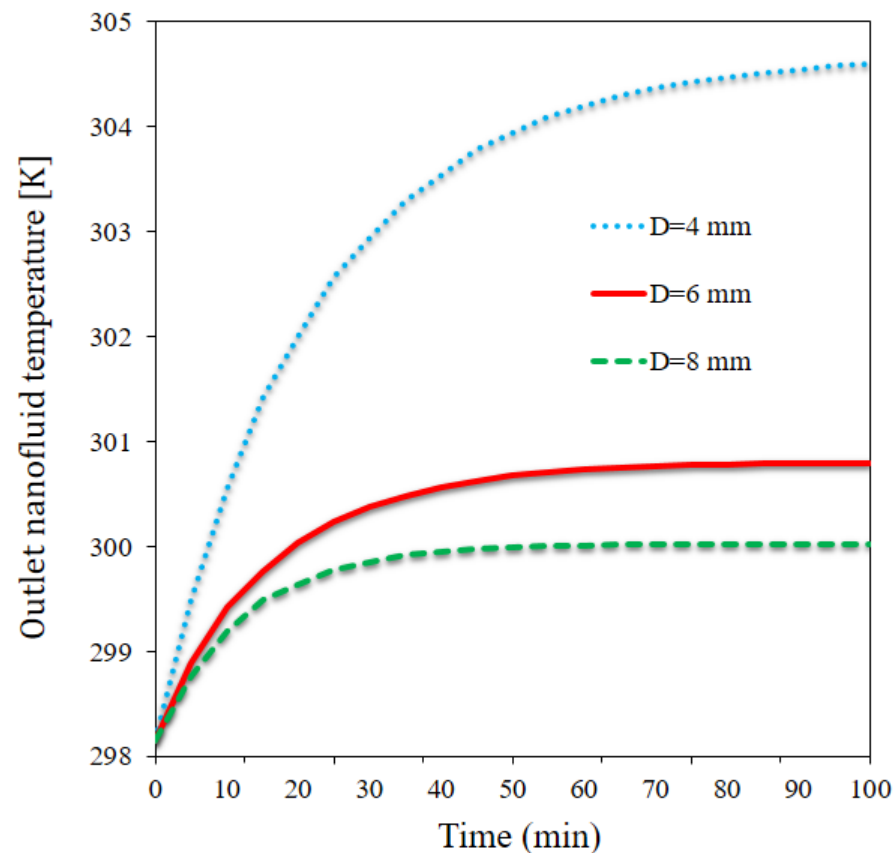
pipe temperature. Hence, the output temperature was higher for a diameter of 4 mm than for 6 and 8 mm. Furthermore, for a diameter of 8 mm, the flow had a high velocity and fewer collisions with the pipe wall in the middle of the pipe. Thus, the flow temperature remained low in more of the pipe since the heat would take longer to reach the middle of the pipe.



**Figure 7.** The temperature contours of the horizontal cross section of the middle portion of the panel for D\_Pipes of 4, 6, and 8 mm.

Figure 8 depicts the output flow temperature for D\_Pipes of 4, 6, and 8 over time. The output temperature is a critical parameter for electrical efficiency improvement. It is dependent on the panel temperature, and a higher panel temperature leads to a higher output temperature. Given the constant solar heat flux on the solar panel, the output temperature was higher for lower D\_Pipes. At larger flow rates, the flow had fewer collisions with the pipe wall in the middle of the pipe, resulting in less HTR to the NFD. Furthermore, for smaller D\_Pipes, the PCM melted within a shorter time and the flow collided with the PCM at a higher temperature, increasing the flow temperature. As a

result, the output temperature was higher for lower  $D_{\text{Pipes}}$ , and the temperature of the NFD continued to increase for a longer time.



**Figure 8.** The output flow temperature for  $D_{\text{Pipes}}$  of 4, 6, and 8 over time.

Figure 9 plots the HTR coefficient for pipes with diameters of 4, 6, and 8 mm over time. HTR between the pipe and PCM was found to be strongly dependent on the diameter, and an increase in the  $D_{\text{Pipe}}$  decreased the HTR coefficient. The HTR coefficient between the pipe and PCM changes incrementally for a longer time and was smaller for larger  $D_{\text{Pipes}}$ . A change in the PCM temperature substantially influenced the amount of HTR; an increase in the PCM temperature increased the temperature difference between the pipe and PCM, increasing the amount of HTR. In addition, the increased diameter enlarged the HTR surface area. As can be seen, the increased surface area reduced the overall HTR coefficient due to the integration of local HTR coefficients, and the HTR coefficient experienced a smaller increase with the increase in diameter due to the larger surface areas. Furthermore, the rapid melting and, therefore, temperature increase in the PCM increased the amount of HTR between the PCM and pipe. For a  $D_{\text{Pipe}}$  of 4 mm, the PCM melted and experienced an increased temperature within a shorter time, leading to a larger HTR coefficient.

Figure 10 illustrates the PCM melting contour of the horizontal cross section of the middle portion of the panel for pipe diameters of 4, 6, and 8 mm. As can be seen,  $D_{\text{Pipe}}$  had a strong effect on PCM melting; an increase in the diameter reduced the melted PCM fraction. For a diameter of 4 mm, the PCM melted entirely in 10 min. Only a very tiny proportion of the PCM remained un-melted for a diameter of 6 mm, particularly in the area of the center pipe and its fins. For a diameter of 8 mm, on the other hand, the PCM remained un-melted, except for some areas under the panel and areas heated by solar radiation. The increased flow rate for a diameter of 8 mm increased the amount of HTR from the solar panel to the flow, leading to lower heat absorption into the PCM and melt fraction. Hence, a larger fraction of the PCM remained un-melted for a  $D_{\text{Pipe}}$  of 8 mm.

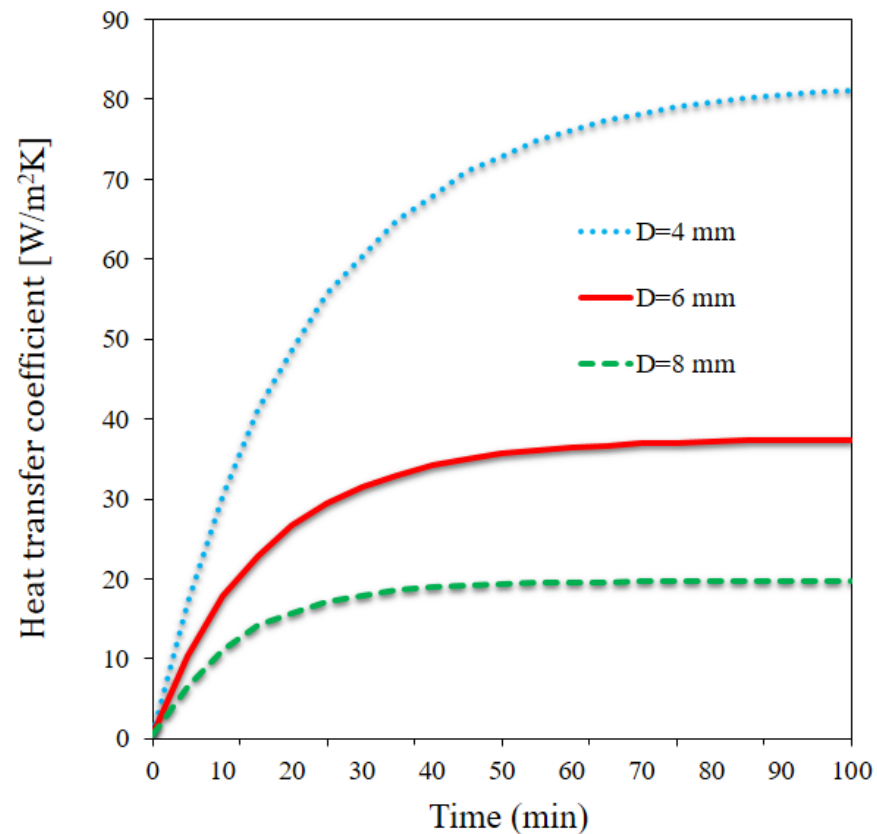


Figure 9. The HTR coefficient on the pipes with diameters of 4, 6, and 8 mm over time.

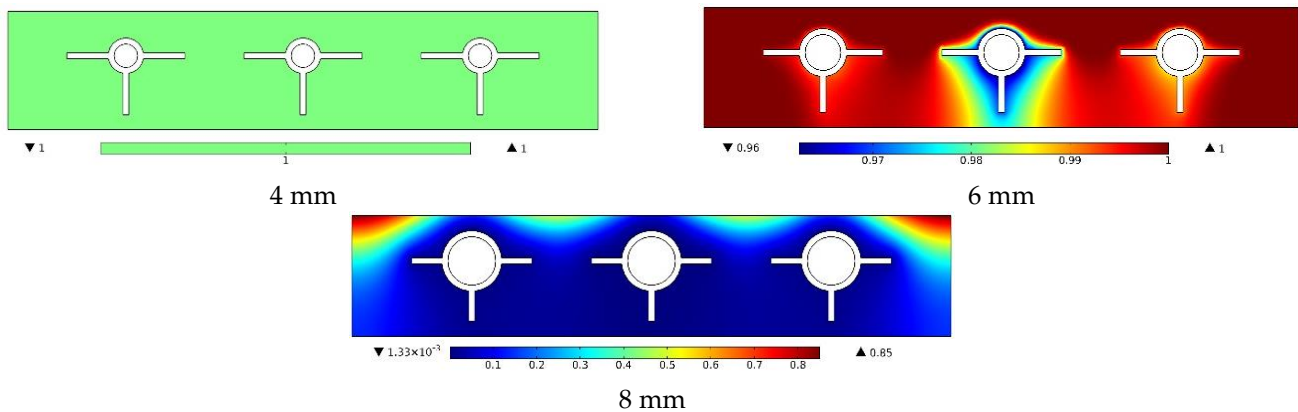
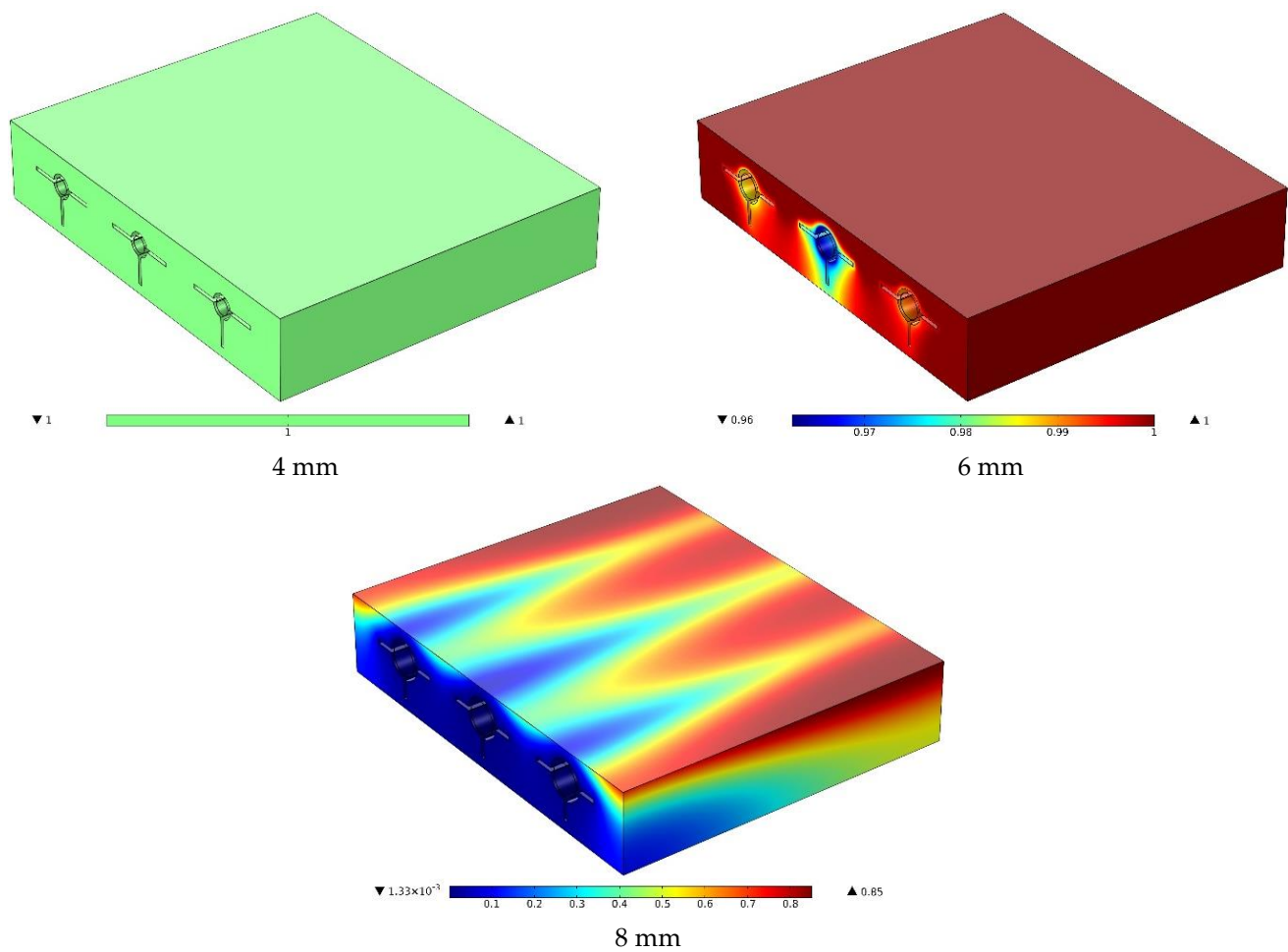


Figure 10. The PCM melting contour of the horizontal cross section of the middle portion of the panel for pipe diameters of 4, 6, and 8 mm.

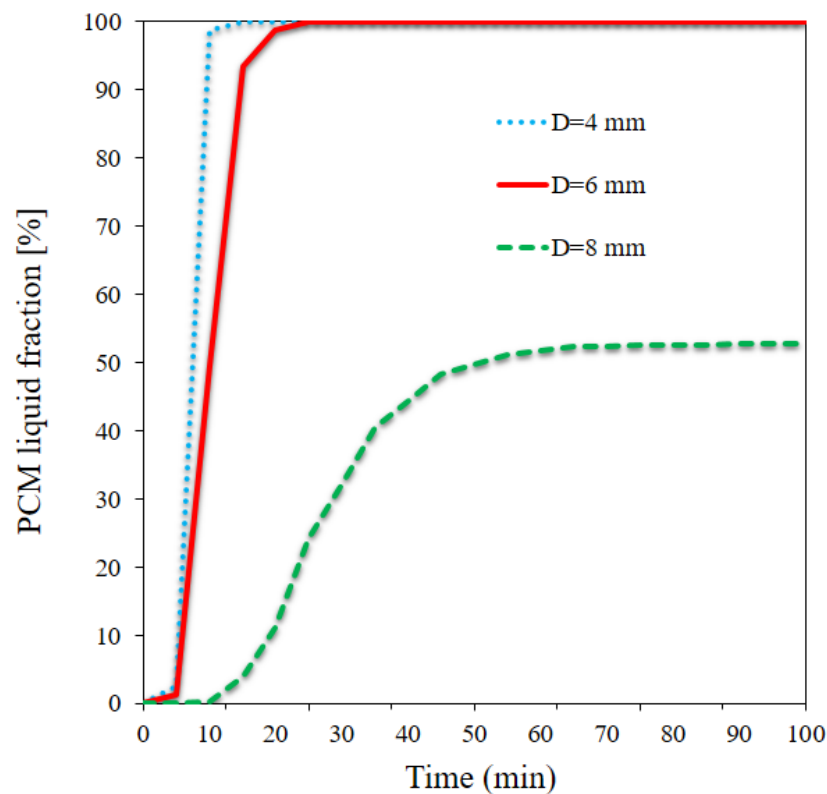
Figure 11 depicts the PCM melting contour for the middle portion of panels with pipes with diameters of 4, 6, and 8 mm.  $D_{\text{Pipe}}$  had a significant effect on the PCM melting time. The PCM melted entirely for a diameter of 4 mm, with the phase change process being completed. A significant portion of the PCM melted for a  $D_{\text{Pipe}}$  of 6 mm, and the PCM only remained solid around the central pipe. For a diameter of 8 mm, however, the PCM remained mostly un-melted; it melted only in areas where the panel was exposed to solar radiation. The dependence of the melted PCM fraction on the diameter is explained by the flow rate; the flow rate was greater for larger  $D_{\text{Pipes}}$ , improving HTR from the panel to the NFD.



**Figure 11.** The PCM melting contour for the middle portion of panels with pipes with diameters of 4, 6, and 8 mm.

The melted PCM volume % for D Pipes of 4, 6, and 8 mm is shown with time in Figure 12. Solar radiation increases the panel temperature, reducing its electrical efficiency. The PCM and NFD flow were exploited under the panel to reduce its temperature and to enhance its electrical efficiency. A significant portion of the PCM melted quickly since there wasn't much of it used. A large NFD flow rate could discharge a significant portion of the heat from the solar panel. However, the heat would remain in the panel at poor flow rates. For a D\_Pipe of 8 mm, the flow rate through the pipe was larger, discharging a greater amount of heat. For diameters of 4 and 6 mm, however, the flow discharged only a small portion of the heat, with a major portion of the heat remaining in the solar panel and increasing the panel temperature. The solid PCM absorbs the heat from the panel, melts into a liquid-like form, and begins to increase in temperature once it has completely melted. For a diameter of 8 mm, however, the melted PCM volume fraction never exceeded 50% due to the strong NFD flow through the pipe. Finally, with the investigations conducted using an artificial intelligence method, it was seen that the best conditions for the solar system to have the lowest panel temperature, the highest NFD output temperature, and the lowest pressure drop in the pipes were a 8 mm pipe diameter and a 350 Reynolds number.





**Figure 12.** The volume percentage of PCM that has melted for D Pipes that are 4, 6, and 8 mm in time.

## 6. Conclusions

This paper evaluated the temperature control of a solar panel using NFD flow and PCM. Eco-friendly NPs fabricated from tea leaf extracts were employed to develop the NFD. A two-phase mixture was adopted to simulate the NFD flow, while the PCM melt front was simulated using the enthalpy method. The PCM made use of a number of pipes with straight fins. Over the course of 100 min, the system was examined for D Pipes of 4, 6, and 8 mm. The application of an eco-friendly NFD and a PCM simultaneously in the solar panel and the evaluation of this system by changing the tube diameter are the novelties of the present work. The results can be summarized as follows:

- (1) The maximum and average panel temperatures dramatically increased from  $t = 0$  to  $t = 10$  min and then increased at a large or small rate, depending on the diameter.
- (2) An increase in the diameter, particularly from 4 to 6 mm, reduced the maximum and average panel temperatures. However, the increased diameter raised the melted PCM volume fraction.
- (3) An increase in D\_Pipe reduced the output flow temperature and the amount of HTR between the pipes and PCM.
- (4) The output temperature and the amount of HTR between the pipe and PCM were found to be dependent on time and increased over time depending on D\_Pipe.
- (5) The panel had significantly lower temperatures in areas in contact with the pipes than in the other areas.

Finally, suggestions for future works are presented based on the present simulations:

1. This study can be performed for a different number of fins and for various fin shapes at different flow rates.
2. The effect of using different PCMs and different NFDs on the outputs should be examined.
3. The influence of using a PV-thermal panel during the night should also be evaluated in the absence of radiation.

- The impact of radiation changes on the outputs should be investigated at different hours of the day.

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