

Thermal analysis of porous fins enclosure with the comparison of analytical and numerical methods

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Abstract

In this study, heat transfer through a porous fin with rectangular cross section is investigated. The Darcy model is utilized to simulate heat transfer in this porous media. It is assumed that the fin is one-dimensional, homogenous, the flow is laminar, and the generated heat is a linear function of temperature. In this research, three different analytical methods are used to obtain the temperature distribution after deriving the heat transfer equation. In order to validate the obtained solution the collocation method (CM) is compared with the results by a numerical method, in order to validate the solutions, homotopy perturbation method (HPM) and homotopy analysis method (HAM) are employed. This problem is solved for the general case, and the output is obtained as a relationship for one iteration. The effects of various parameters including convection (Nc), porosity (Sh), Rayleigh number (Ra) are examined in this research.

Keywords Porous fin · Darcy model · Dimensionless temperature gradient · CM · HAM · HPM

List of symbols

Ra Rayleigh number
Sh Porosity parameter
Nc Convection parameter
 K_r Ratio of conduction heat transfer
Nr Radiation parameter
 G Dimensionless number of generated heat
 ε Parameter of internal heat generation
 θ Parameter of surface temperature
 Q Heat transfer rate
 α Thickness ratio
 Bi Biot number

Θ Dimensionless temperature of convection medium
 θ_s Dimensionless temperature of sink for radiation
 H Homotopy method

Introduction

Porous material [1–3] is a new innovation which provides the ability to gather a specific set of physical, mechanical and biological properties. This has made the aeronautics, car industry, ventilation and electronic industries, industry of medical equipment, constituent parts of the building (concrete, cement, window, solar collector) and especially in nanotechnology, benefit from this novel technology is based on their own requirements [4–27]. Due to the importance of numerical and analytical investigations of heat transfer in fins, various scientists of physics, mathematics and the engineers have focused on this topic. Investigation of extended surface for different cases has been performed based on one- and two-dimensional analyses. Fins are frequently used in various applications of heat transfer. An extensive study has been conducted in this field, and there are numerous references in the field of heat transfer in porous fins.

Chamkha et al. [28–35] proposed a simple method of performance analysis of porous fins in a medium with natural convection. This method was based on energy balance and Darcy's equation for deriving heat transfer

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equation. Thermal performance of fin was considered for three types of fins including long, finite length with adiabatic and non-adiabatic ends subjected to specific convection coefficient. In the subsequent sections, it was inferred that the effects of different parameters such as Rayleigh number, Darcy number, ratio of conduction heat transfer K_r and length ratio on temperature distribution along the fin length are incorporated in one parameter called porosity. In addition, the effects of conduction heat transfer ratio and length on heat transfer rate were investigated and compared to solid fin in special condition. Finally, it was indicated that heat transfer rate from porous fin was higher than conventional solid fin. Sheikholeslami and Ganji [17–45] investigated heat transfer (convective–radiative) porous fins with different section shapes and materials. They show that with the increase in porosity, heat transfer from fin was increased. Besides, the results indicated that there is a restriction for the increase in K_r and L/t that affect heat transfer rate from the porous fin. In other research, they utilized Finite Difference Method in order to investigate the performance of different profiles.

Sheikholeslami et al. [46–74] used analytical perturbation method (HAM) and homotopy perturbation method (HPM) and variational iteration method (VIM) to solve equations. In order to evaluate the accuracy of methods, the obtained results were compared to the exact solutions, and it was observed that both mentioned methods were able to solve the vast majority of nonlinear differential equations at high accuracy. They considered rectangular profile for the problem and utilized Darcy model for simulation in porous medium. They used finite difference and combined methods to solve the governing equations. The obtained results indicated that the aluminum porous fin, temperature distribution and heat transfer. Also, they studied heat transfer in a porous fin of various nanofluids and nanoparticles, such as $\text{CuO-H}_2\text{O}$ and $\text{Al}_2\text{O}_3\text{-H}_2\text{O}$, and investigated the Darcy law for nanofluid flow in a porous cavity under the impact of Lorentz forces and analysis of flow parameter on heat transfer drop for porous fins.

Hoseinzadeh et al. [75–80] studied heat transfer of single/hybrid nanoparticles, hybrid nanofluids, in a differentially heated porous cavity. They analyze the effects of size, shape and type of nanoparticles, type of base fluid and working temperature. Moreover, rectangular, trapezoidal, triangular and parabolic profiles were selected to compare heat transfer rates. Their achievement was a three-dimensional nonlinear equation. For solving the equation, they used Newton–Raphson method. The obtained results revealed that the heat transfer rate (Q) for a profile is a function of length to half of base thickness ratio (α), Biot number (Bi), conduction-radiation number (Nr), dimensionless temperature of convection medium (θ), and dimensionless temperature of sink for radiation (θ_s). In

addition, they indicated that heat transfer rate for rectangular fins was greater than triangular ones. Finally, by comparing the results of parabolic–concave profile, it was inferred that heat transfer from these fins was the lowest in comparison with the other profiles.

Problem and solving methods

In order to simplify the solution, the following assumptions are prescribed. The rectangular profile which is attached to a vertical wall at constant temperature with laminar and steady flow fin is constructed from a porous, homogenous, isotropic material and saturated by single-phase fluid was considered. The fin and surrounding fluid have constant properties unlike the thermal conductivity. Fin temperature is a function of X , and its variations along Y are neglected. Darcy’s law is used to carry out simulation in porous medium, and flow is laminar and steady.

In this study, the fin has adiabatic end with finite length. Linear differential equation defined and it requires two boundary conditions as it is second-order equation [77].

$$\frac{d^2\theta}{dX^2} + 4Rd \frac{d^2\theta}{dX^2} + G(1 + \varepsilon\theta(X)) - Sh\theta^2 + (Nc + Nr)\theta = 0 \quad (1)$$

First boundary condition: $X = 1 \rightarrow \theta(1) = 1$

Second boundary condition: Since fin is adiabatic at the end side, no heat transfer occurs at this side. This is why temperature gradient is zero. Therefore, boundary conditions in dimensionless case will be as follows: $X = 0 \rightarrow \theta'(0) = 1$

Collocation method

In order to provide approximate solutions for nonlinear problems, we can use trial function. For doing this, trial function is usually considered as a function of n specified coefficients including C_1, C_2, \dots . In other words, it is considered as $T.F = f(c_1, c_2, \dots, c_n)$. The condition of selecting trial function is as follows: trial function is written as some base functions such as polynomials and trigonometric functions. Trial function is written in a way that it satisfies boundary conditions. Substituting the trial function as the main function causes a residual which is a function of constants and variables. It is desired that residual approaches zero. The constants C_1 to C_s should be determined by a specific method. For doing this, there are several methods including Galerkin and Rayleigh–Ritz Methods.

The Rayleigh–Ritz method includes (n) unknown coefficients, and it provides different situations based on the residual. This method is approximated based on $0 < t < 1$

which is defined in the problem. In this method, the purpose is to find C_1 to C_n in order to determine the residual and trial function as a result. In fact, calculation of trial function will lead us to the final solution. In order to build an approximation for the solution, we select a base function as a polynomial based on X .

$$\begin{aligned} \theta(X) = & 1 + C_1(1 - X^2) + C_2(1 - X^3) + C_3(1 - X^4) \\ & + C_4(1 - X^5) + c_5(1 - X^6) + c_6(1 - X^7) \\ & + c_7(1 - X^8) + c_8(1 - X^9) \end{aligned} \quad (2)$$

The above approximate solution satisfied the boundary condition. By incorporating Eq. (2) in the differential Eq. (1), the equation of the residual will appear as follows:

$$\begin{aligned} R(X) = & 2Shc_1c_4X^5 + 2Shc_1c_5X^6 - Shc_3^2 - 2Shc_1 \\ & - 2Shc_2 - 2Shc_3 - 2Shc_4 - 2Shc_5 \\ & - 2Shc_6 - 2Shc_7 - 2Shc_8 - Shc_1^2 + Shc_2^2 \\ & - Shc_4^2 + 2Shc_2X^3c_8 - Shc_5^2 - Shc_6^2 - Shc_7^2 \\ & - Ncc_2 - Ncc_3 - Ncc_4 - Ncc_5 - Ncc_6 \\ & - Ncc_7 - Ncc_8 - Nrc_1 - Nrc_2 - Nrc_3 - Nrc_4 \\ & - Nrc_5 - Nrc_6 - Nrc_7 - Nrc_8 - 2Shc_1X^9c_6 \\ & + 2Shc_1X^2c_7 - 2Shc_1X^{10}c_7 + 2Shc_1X^2c_8 \\ & - 2Shc_1X^{11}c_8 + \dots + 2Shc_2c_3X^4 + 2Shc_2c_4X^5 \\ & + 2Shc_2c_5X^6 + 2Shc_2c_6X^7 + 2Shc_2c_7X^8 \\ & + 2Shc_2c_8X^9 + 2Shc_2X^3c_32Shc_2X^3c_6 \\ & - 2Shc_2X^{10}c_6 + 2Shc_2X^3c_7 - 2Shc_2X^{11}c_7 \\ & - 2Shc_2X^{12}c_8 + 2Sh_3c_4X^5 + 2Shc_3c_5X^6 \\ & + 2Shc_3c_6X^7 + 2Shc_3c_7X^8 + 2Shc_3c_8X^9 \\ & + 2Shc_3X^4c_4 - 2Shc_3X^9c_4 - 2Shc_6X^{16}c_8 \\ & + 2Shc_7c_8X^9 + 2Shc_7X^8c_8 - 2Shc_7X^{17}c_8 \\ & - Nc - Nr - 288Rdc_8X^7 - 24Rdc_2X \\ & - 120Rdc_5X^4 - 168Rdc_6X^5 - 48Rdc_3X^2 \\ & - 80Rdc_4X^3 - Shc_8^2 - Ncc_1 - 224Rdc_7X^6 \\ & + 2Shc_2^2X^3 - 2Shc_2c_3 - Sh = 0 \end{aligned} \quad (3)$$

For obtaining the constant coefficients C_1 to C_n in the range of $0 < X < 1$, we have:

$$\begin{aligned} R\left(\frac{1}{9}\right) = 0, \quad R\left(\frac{2}{9}\right) = 0, \quad R\left(\frac{3}{9}\right) = 0, \quad R\left(\frac{4}{9}\right) = 0, \\ R\left(\frac{5}{9}\right) = 0, \quad R\left(\frac{6}{9}\right) = 0, \quad R\left(\frac{7}{9}\right) = 0, \quad R\left(\frac{8}{9}\right) = 0 \end{aligned} \quad (4)$$

By solving the above equations, the coefficients $C_1, C_2, C_3, C_4, C_5, C_6, C_7$ and C_8 can be calculated based on different values of Sh, Nc, Nr, Rd .

Homotopy Method

In this section, homotopy method $H(\tau)$ is used to solve Eq. (1) based on the boundary conditions (6).

$$\begin{aligned} H(\theta, p) = & (1 - P)[\theta''(X) - \theta(X) - g_0(X)] \\ & + p \left[\theta''(X) + 4Rd\theta''(X) - Sh\theta''(X)^2 \right. \\ & \left. + G(1 + \varepsilon\theta(X)) + (Nc + Nr)\theta(X) \right] = 0, \end{aligned} \quad (5)$$

where P is the defined parameter in the range of $P \in [0, 1]$. For $P = 0$ and $P = 1$ we have:

$$\theta(X, 0) = \theta_0(X), \quad \theta(X, 1) = \theta(X) \quad (6)$$

Therefore, when P increases from 0 to 1, $\theta(X; p)$ changes from $\theta_0(X)$ to $\theta(X)$.

$$\begin{aligned} \theta(X) = & \theta_0(X) + p\theta_1(X) + p^2\theta_2(X) + \dots \\ = & \sum_{i=0}^n p^i \theta_i(X), \quad g_0 = 0 \end{aligned} \quad (7)$$

By substituting in Eq. (2) and rearranging the results based on the power of P ($M = 1, \beta = -0.4$ for example)

$$\begin{aligned} P^0 : & (1 + 4Rd)\theta_0''(X) = 0 \\ & \theta_0(1) = 1, \theta_0'(0) = 0 \end{aligned} \quad (8)$$

$$\begin{aligned} P^1 : & \theta_1''(X) - Sh\theta_0(X)^2 - Nr\theta_0(X) - Nc\theta_0(X) \\ & + 4Rd\theta_1''(X) + G + G\varepsilon\theta_0(X) = 0 \\ & \theta_1(1) = 0, \theta_1'(0) = 0 \end{aligned} \quad (9)$$

$$\begin{aligned} P^2 : & 4Rd\theta_2''(X) - Nr\theta_1(X) - Nc\theta_1(X) + \theta_2''(X) \\ & - 2Sh\theta_0(X)\theta_1(X) + G\varepsilon\theta_1(X) = 0 \\ & \theta_2(1) = 0, \theta_2'(0) = 0 \end{aligned} \quad (10)$$

$$\begin{aligned} P^3 : & \theta_3''(X) - Nc\theta_2(X) + 4Rd\theta_3''(X) - Nr\theta_2(X) \\ & - 2Sh\theta_0(X)\theta_2(X) - Sh\theta_1(X)^2 + G\varepsilon\theta_2(X) = 0 \\ & \theta_3(1) = 0, \theta_3'(0) = 0 \end{aligned} \quad (11)$$

⋮

From Eq. (10) with the boundary conditions, we have:

$$\theta_0(X) = 1 \quad (12)$$

$$\begin{aligned} \theta_1(X) = & \frac{1(-G + Nc + Nr + Sh - G\varepsilon)X^2}{2} \\ & + \frac{1G - Nc - Nr - Sh + G\varepsilon}{2} \end{aligned} \quad (13)$$

$$\theta_2(X) = \frac{1(G - Nc - Nr - Sh + G\epsilon)(-Nc - Nr - 2Sh + G\epsilon)}{2(1 + 4Rd)^2}$$

$$\times \frac{1}{2} \left(\frac{1}{12}x^4 - \frac{1}{2}x^2 \right) + \frac{5}{24(1 + 8Rd + 16Rd^2)}$$

$$\times [G^2\epsilon^2 + 3ShNr - 2NcG\epsilon$$

$$- NcG + 2NcNr - 2G\epsilon NrG^2\epsilon + 2Sh^2$$

$$- 3G\epsilon Sh - 2ShG + Nr^2 - NrG + Nc^2 + 3NcSh]$$

$$\vdots \quad (14)$$

Finally, by solving the equation when $p \rightarrow 1$, we will have:

$$\theta(X) = \sum_{i=0}^N \text{Lim}_{p \rightarrow 1} p^i \theta_i(X) \quad (15)$$

Results

Comparison between different solving methods

In the curves provided in Fig. 1, comparison between different methods including collocation method (CM), homotopy perturbation method (HPM) and homotopy analysis method (HAM) with the numerical Runge–Kutta method for different values of Nc , Nr , Rd and Sh with the results of numerical method for boundary value problems. Results indicate that the mentioned methods are so strong in solving the present problem. Also, Table 1 indicates the results obtained by analytical method and numerical method for boundary value problems. Table 2 indicates the results obtained by analytical method and numerical method for boundary value problems.

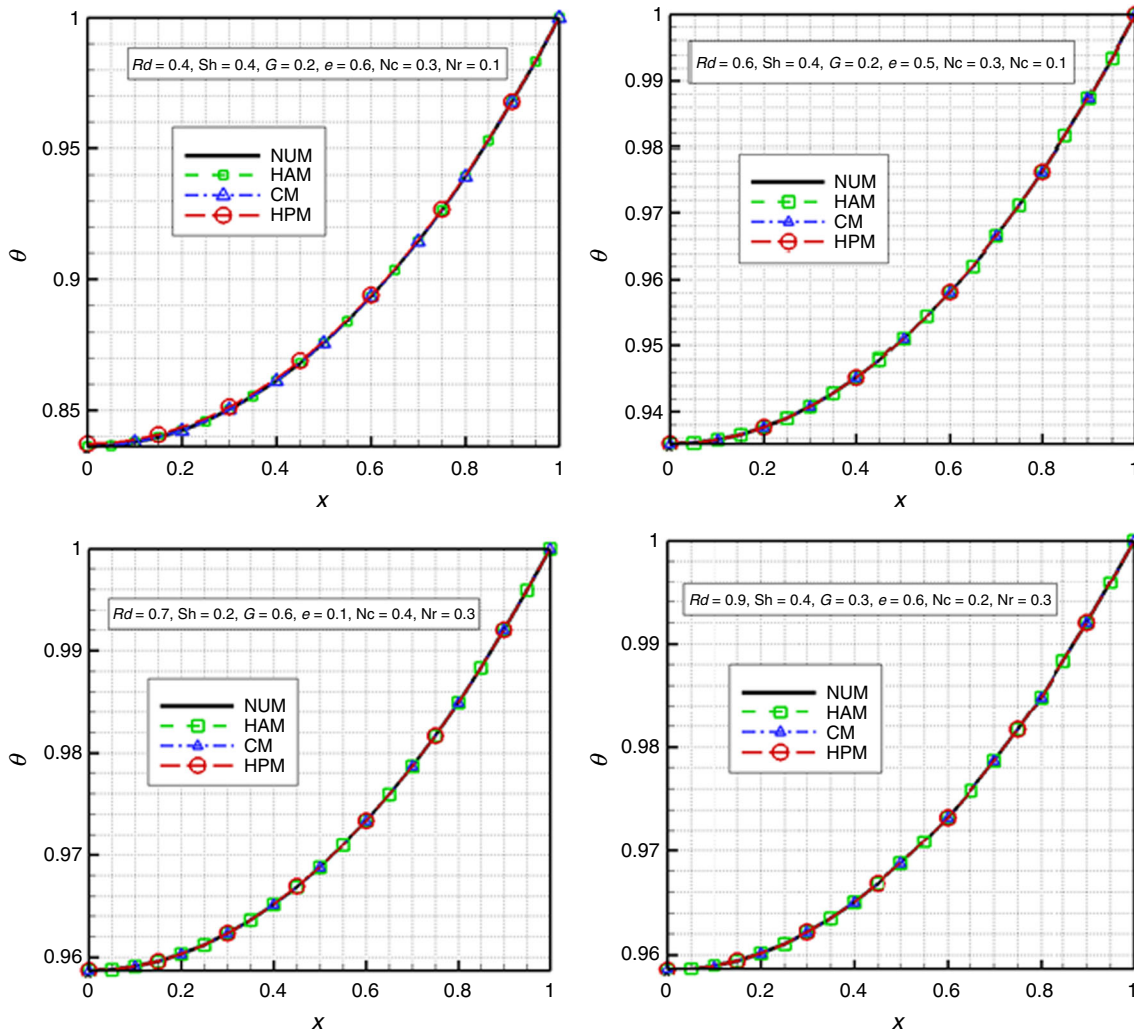


Fig. 1 Comparison between different methods including collocation, homotopy perturbation and homotopy analysis methods with the numerical Runge–Kutta method

Table 1 Comparison of numerical and analytical methods of HAM, CM and HPM for $Rd = 0.6, Sh = 0.4, G = 0, Nc = 0.3, Nr = 0.1$

| X | HAM | CM | HPM | Num. | Error of HAM | Error of CM | Error of HPM |
|------|-------------|-------------|-------------|-------------|--------------|-------------|--------------|
| 0.00 | 0.897079121 | 0.89707909 | 0.897077821 | 0.897079127 | 5.90E-09 | 3.62000E-08 | 1.3053E-06 |
| 0.05 | 0.897329407 | 0.897329377 | 0.897328112 | 0.897329391 | 1.58E-08 | 1.44477E-08 | 1.2794E-06 |
| 0.10 | 0.898080472 | 0.898080441 | 0.898079189 | 0.898080471 | 1.00E-09 | 2.94474E-08 | 1.2819E-06 |
| 0.15 | 0.899332932 | 0.899332901 | 0.89933167 | 0.899332937 | 4.90E-09 | 3.54890E-08 | 1.2674E-06 |
| 0.20 | 0.901087819 | 0.901087788 | 0.901086585 | 0.901087821 | 2.00E-09 | 3.28237E-08 | 1.2361E-06 |
| 0.25 | 0.903346578 | 0.903346547 | 0.90334538 | 0.903346581 | 2.20E-09 | 3.32047E-08 | 1.2002E-06 |
| 0.30 | 0.906111073 | 0.906111042 | 0.906109919 | 0.906111076 | 2.40E-09 | 3.36356E-08 | 1.1569E-06 |
| 0.35 | 0.909383588 | 0.909383557 | 0.909382484 | 0.909383589 | 4.00E-10 | 3.19209E-08 | 1.1044E-06 |
| 0.40 | 0.913166834 | 0.913166802 | 0.913165787 | 0.913166833 | 1.00E-09 | 3.06023E-08 | 1.0456E-06 |
| 0.45 | 0.917463951 | 0.917463919 | 0.917462968 | 0.91746395 | 1.60E-09 | 3.01716E-08 | 9.8163E-07 |
| 0.50 | 0.922278518 | 0.922278486 | 0.922277604 | 0.922278514 | 4.20E-09 | 2.74392E-08 | 9.0967E-07 |
| 0.55 | 0.927614557 | 0.927614525 | 0.927613717 | 0.927614551 | 5.40E-09 | 2.59427E-08 | 8.3383E-07 |
| 0.60 | 0.93347654 | 0.933476509 | 0.93347578 | 0.933476535 | 5.30E-09 | 2.54704E-08 | 7.5445E-07 |
| 0.65 | 0.939869402 | 0.939869372 | 0.939868726 | 0.939869395 | 6.90E-09 | 2.27767E-08 | 6.6885E-07 |
| 0.70 | 0.946798546 | 0.946798518 | 0.946797958 | 0.946798537 | 8.60E-09 | 1.96598E-08 | 5.7939E-07 |
| 0.75 | 0.954269855 | 0.954269829 | 0.954269358 | 0.954269849 | 6.60E-09 | 1.96715E-08 | 4.9021E-07 |
| 0.80 | 0.962289706 | 0.962289683 | 0.962289304 | 0.962289701 | 5.50E-09 | 1.78223E-08 | 3.9685E-07 |
| 0.85 | 0.970864979 | 0.970864959 | 0.970864674 | 0.970864971 | 8.50E-09 | 1.12455E-08 | 2.9697E-07 |
| 0.90 | 0.980003073 | 0.980003058 | 0.980002867 | 0.980003079 | 6.20E-09 | 2.07769E-08 | 2.1193E-07 |
| 0.95 | 0.989711919 | 0.989711911 | 0.989711815 | 0.989711953 | 3.38E-08 | 4.20042E-08 | 1.3776E-07 |
| 1.00 | 1.000000000 | 1.000000000 | 1.000000000 | 1.000000000 | 0.000000 | 0.000000000 | 0.00000000 |

Table 2 Comparison of numerical and analytical methods HAM, CM and HPM for $Rd = 0.7, Sh = 0.2, G = 0, Nc = 0.4, Nr = 0.3$

| X | HAM | CM | HPM | Num. | Error of HAM | Error of CM | Error of HPM |
|------|-------------|-------------|-------------|-------------|--------------|-------------|--------------|
| 0.00 | 0.894162789 | 0.894162788 | 0.894162588 | 0.894162814 | 2.52E-08 | 2.56000E-08 | 2.26400E-07 |
| 0.05 | 0.894421297 | 0.894421297 | 0.894421096 | 0.894421308 | 1.06E-08 | 1.09979E-08 | 2.11144E-07 |
| 0.10 | 0.895197002 | 0.895197001 | 0.895196803 | 0.895197022 | 2.07E-08 | 2.10835E-08 | 2.19276E-07 |
| 0.15 | 0.896490442 | 0.896490442 | 0.896490247 | 0.896490467 | 2.46E-08 | 2.51057E-08 | 2.20063E-07 |
| 0.20 | 0.898302520 | 0.898302520 | 0.898302329 | 0.898302543 | 2.28E-08 | 2.32777E-08 | 2.13745E-07 |
| 0.25 | 0.900634497 | 0.900634497 | 0.900634312 | 0.900634520 | 2.29E-08 | 2.34202E-08 | 2.08180E-07 |
| 0.30 | 0.903488000 | 0.903488000 | 0.903487822 | 0.903488023 | 2.32E-08 | 2.36377E-08 | 2.01520E-07 |
| 0.35 | 0.906865021 | 0.906865020 | 0.906864850 | 0.906865042 | 2.17E-08 | 2.24257E-08 | 1.92318E-07 |
| 0.40 | 0.910767918 | 0.910767917 | 0.910767757 | 0.910767939 | 2.09E-08 | 2.15027E-08 | 1.82354E-07 |
| 0.45 | 0.915199424 | 0.915199423 | 0.915199272 | 0.915199444 | 2.04E-08 | 2.10612E-08 | 1.71894E-07 |
| 0.50 | 0.920162644 | 0.920162643 | 0.920162503 | 0.920162662 | 1.85E-08 | 1.92320E-08 | 1.59144E-07 |
| 0.55 | 0.925661063 | 0.925661062 | 0.925660934 | 0.925661080 | 1.73E-08 | 1.80507E-08 | 1.46224E-07 |
| 0.60 | 0.931698548 | 0.931698547 | 0.931698432 | 0.931698565 | 1.67E-08 | 1.76202E-08 | 1.33320E-07 |
| 0.65 | 0.938279357 | 0.938279356 | 0.938279254 | 0.938279372 | 1.51E-08 | 1.57571E-08 | 1.18338E-07 |
| 0.70 | 0.945408140 | 0.945408139 | 0.945408050 | 0.945408152 | 1.27E-08 | 1.35093E-08 | 1.02414E-07 |
| 0.75 | 0.953089946 | 0.953089945 | 0.953089871 | 0.953089959 | 1.25E-08 | 1.34341E-08 | 8.81937E-08 |
| 0.80 | 0.961330234 | 0.961330233 | 0.961330173 | 0.961330245 | 1.13E-08 | 1.21201E-08 | 7.23534E-08 |
| 0.85 | 0.970134874 | 0.970134873 | 0.970134828 | 0.970134881 | 7.00E-09 | 7.63790E-09 | 5.30487E-08 |
| 0.90 | 0.979510159 | 0.979510159 | 0.979510129 | 0.979510173 | 1.33E-08 | 1.37031E-08 | 4.40762E-08 |
| 0.95 | 0.989462814 | 0.989462814 | 0.989462798 | 0.989462841 | 2.73E-08 | 2.76311E-08 | 4.28286E-08 |
| 1.00 | 1.000000000 | 1.000000000 | 1.000000000 | 1.000000000 | 0.000000 | 0.000000000 | 0.00000000 |

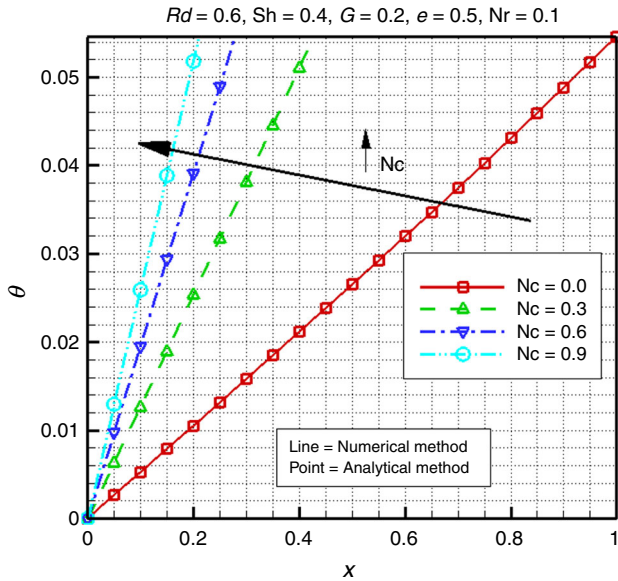


Fig. 2 Dimensionless temperature gradient versus Nc

The effect of different parameters on temperature gradient

In Fig. 2, the effect of changing convection parameter on dimensionless temperature gradient versus fin length is illustrated. According to these variations, it can be inferred that with the increase in different parameters such as convection, temperature gradient along fin is increased. As a result, temperature difference between fin and surroundings will be greater, and great transfer from the surface will take place more easily, which decreases the slope of variations. Besides, in order to investigate the effect of

radiation-surroundings parameter, dimensionless temperature gradient based on dimensionless length for different values of Nr is provided in Fig. 3.

According to these variations, it can be inferred that with the increase in radiation-surroundings parameter, temperature gradient increases along the fin length. As a result, temperature difference between fin and surroundings will be greater, and great heat transfer from the surface will take place more easily. Besides, dimensionless temperature gradient based on dimensionless length for different values of Sh is provided in Fig. 4.

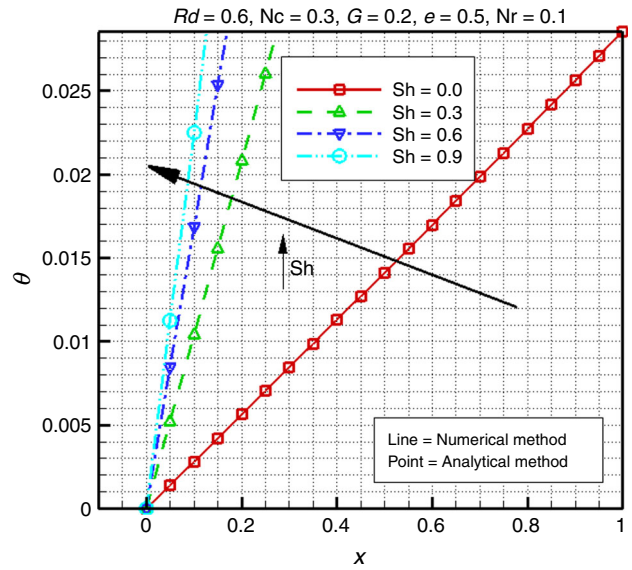


Fig. 4 Dimensionless temperature gradient for different values of Sh

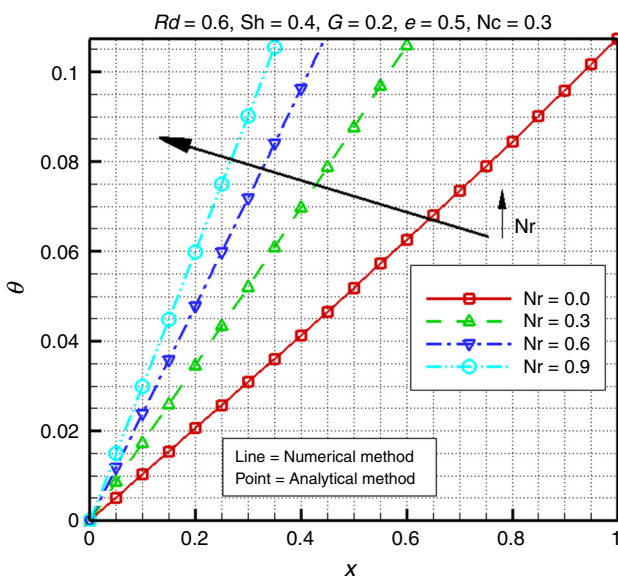


Fig. 3 Dimensionless temperature gradient based on different Nr

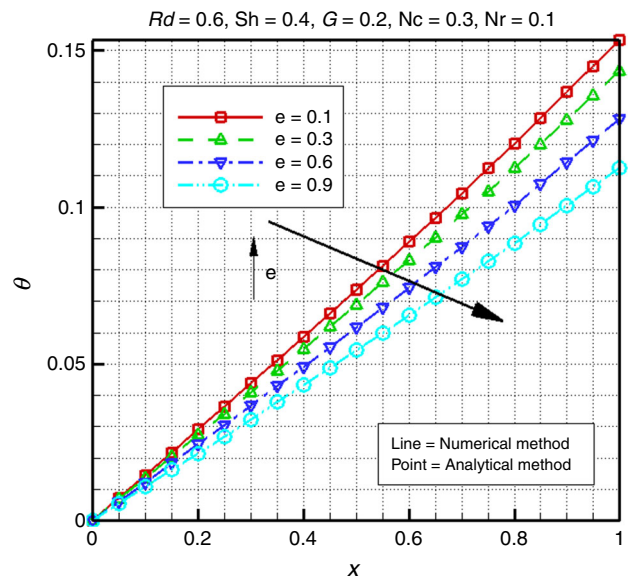


Fig. 5 Dimensionless temperature gradient for different values of e

As illustrated in Figs. 4 and 5, it can be inferred that with the increase in porosity parameter and decrease in internal heat generation parameter, temperature gradient increases along the fin length. As a result, temperature difference between fin and surroundings will be greater, and great heat transfer from the surface will take place more easily. Besides, comparison between the obtained profiles reveals that the radiation-surroundings parameter has more significant impact compared to convection parameter.

Conclusions

In this research, the application of the homotopy analysis method (HAM), homotopy perturbation method (HPM) and collocation method (CM), and validation of their applications in heat transfer problems was studied and compared with themselves. Also, nonlinear equation of temperature along with deriving process of the temperature gradient and the effects of various parameters have been investigated and the following conclusions have been obtained:

- With the increase in some parameters including porosity, convection and radiation-surroundings, the temperature gradient along the fin length rises. Consequently, the temperature difference between the fin and surroundings becomes greater. This simplifies the heat transfer from the surface.
- Comparison between the temperature profiles reveals that the radiation parameters have more considerable impact on the temperature distribution in comparison with the convection parameters.
- With the increase convection, porosity, and radiation-surroundings parameters, the heat flow is increased from ($x = 1$).

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