ON THE MECHANISM OF ACCELERATED SEDIMENTATION OF FINE FRACTIONS IN BIDISPERSE SUSPENSION

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ABSTRACT

An estimation of increasing the average volume of sedimentation velocity of fine particles in bidisperse suspension due to their capturing in the circulation zone formed in the laminar flow of incompressible viscous fluid around the spherical coarse particle is proposed. The estimation is important for an explanation of the non-monotonic shape of the separation curve observed for hydrocyclones. The average volume sedimentation velocity is evaluated on the basis of a cellular model. The characteristic dimensions of the circulation zone are obtained on the basis of a numerical solution of Navier-Stokes equations. Furthermore, these calculations are used for modelling the fast sedimentation of fine particles during their co-sedimentation in bidisperse suspension. It was found that the acceleration of sedimentation of fine particles is determined by the concentration of coarse particles in bidisperse suspension, and the sedimentation velocity of fine fraction is proportional to the square of the coarse and fine particle diameter ratio. The limitations of the proposed model are ascertained.

INTRODUCTION

In a number of industries (mining, chemical, food, etc.) machines based on the principle of settling (sedimentation) of particles in a rotating fluid flow are used for the separation of particulate solids from air or liquid (aircyclones, hydrocyclones, centrifuges, decanters, etc.) [1-3].

Calculation methods for processes in such devices have long been developed that achieve impressive results [4-17]. Even so, a number of effects are in principle incapable of being clearly mathematically described. Such effects include abnormal behavior of the so-called separation efficiency function, i.e. the portion of the separated fraction of initial material depending on the particle size of the fraction.

This phenomenon is often a hindrance for engineers using hydrocyclones because the sharpness of fractionation often deteriorates due to the fine particles (in practice, particles smaller than 10 microns) contrary to expectations falling into the coarse product. Anomalous behavior of the separation function is particularly noticeable for the operation of small hydrocyclones, where the quality of the fine particle separation efficiency deteriorates, leading to an unexpected increase in the separation function with decreasing particle size [1 - 3].

Abnormal growth of the separation function is the subject of lively debate [18-32]. The most likely reason for this anomaly, in our opinion, is connected with the fact that there is an acceleration of sedimentation of fine particles under the influence of neighboring coarse particles in the polydisperse suspension. Due to an entrainment the fine particles have a much higher sedimentation velocity than expected, and are intensively removed together with a coarse fraction from the hydrocyclone [22, 27, 28]. The mechanism of the accelerated sedimentation of fine particles has not been studied well enough.

To explain this effect, a model of the cell for bidisperse suspension has been proposed [22]. That model relies on the determination of the mean residence time of small particles in the cell surrounding the large ones and the subsequent determination of an average sedimentation velocity of small particles. Accelerated sedimentation of small particles occurs due to their retention in the flow boundary layer near the surface of the large particle. Herein the flow around the large particle is postulated identical to the Stokes flow that is valid for $U_c d_c / v_l < 1$. An analysis of the effect of the Reynolds number on the sedimentation velocity of the particles and

consequently on the hydrocyclone separation curve has been carried out [33], but it has not considered the particle-particle interaction phenomena which is so important in the range of the finest particles. Further development of the sedimentation model followed the path of propagation of the entrainment mechanism of small particles by the large ones for the case of polydisperse suspension, using it to evaluate the separation function of the hydrocyclone.

Thus, it was possible to calculate the separation function, including its non-monotonic character [31]. At the same time it becomes clear that some large particles in suspension in a hydrocyclone can move at Re of the order of 10^2. It is known [34, 35] that the boundary layer around the moving particles in a liquid is radically changed already at Re ≈ 25: instead of the smooth streamlines along the direction of particles motion a zone of reverse flows appears. They become more complicated for the increased Reynolds number. This requires further development of the entrainment model.

The logical explanation for the accelerated sedimentation of small particles in the presence of large ones can be considered as a capture of small particles entering the hydrodynamic wake generated by a large particle at the numbers of Re> 25 [20, 23].

The aim of this paper is to study the circulation zone that occurs in the laminar flow of an incompressible viscous fluid around a spherical particle and the determination of the volume average sedimentation velocity of small particles during the sedimentation of bidisperse suspension, based on a cellular model.

NOMENCLATURE

d	[m]	Particle diameter
f	[-]	Relative volume of circulation zone
f_D	[-]	Drag function
g	[m^2/s]	Acceleration
p	[Pa/m^2]	Pressure
t	[s]	Time
r, z	[m]	Spatial coordinates
C_D	[-]	Drag coefficient
L	[-]	Relative length of circulation zone
R	[m]	Radius
U	[m/s]	Particle velocity
V	[m/s]	Fluid flow velocity
Re	[-]	Reynolds number

Special characters

α	[-]	Volume fraction
ν	[m^2/s]	Kinematic viscosity
ρ	[kg/m^3]	Density
υ	[m^3]	Volume

Subscripts

1	Boundary ABC
2	Boundary ED
c	Coarse particle
cell	Cell
f	Fine particle
l	Liquid
m	Maximum
min	Minimum
r	Radial direction
s	Solid
sph	Sphere
z	Axial direction

MATHEMATICAL FORMULATION OF THE PROBLEM

The system of Navier-Stokes equations describing the steady state laminar flow of an axisymmetric incompressible viscous fluid around a sphere in a cylindrical coordinate system is as follows [35]:

$$V_r \frac{\partial V_r}{\partial r} + V_z \frac{\partial V_r}{\partial z} + \frac{1}{\rho}\frac{\partial p}{\partial r} = \nu\left(\nabla^2 V_r - \frac{V_r}{r^2}\right) \tag{1}$$

$$V_r \frac{\partial V_z}{\partial r} + V_z \frac{\partial V_z}{\partial z} + \frac{1}{\rho}\frac{\partial p}{\partial z} = \nu\left(\nabla^2 V_z\right) \tag{2}$$

$$\frac{1}{r}\frac{\partial}{\partial r}\left(rV_r\right) + \frac{\partial V_z}{\partial z} = 0 \tag{3}$$

Here

$$\nabla^2 \equiv \frac{1}{r}\frac{\partial}{\partial r}\left(r\frac{\partial}{\partial r}\right) + \frac{\partial^2}{\partial z^2}.$$

The domain of integration of the system of equations (1) - (3), presented in Figure 1, is limited by the input boundary AB, the output boundary BC, the axis of symmetry DC∪AE, as well as the contour of the sphere ED.
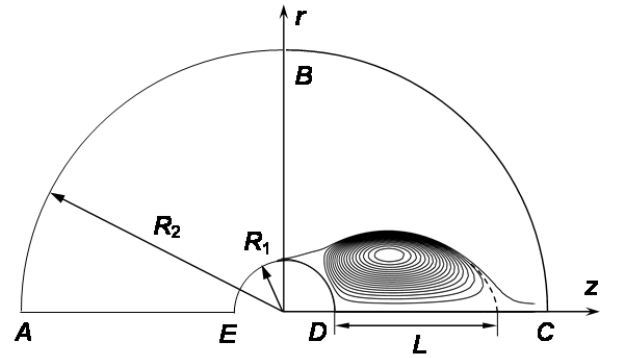

Figure 1 Domain of integration

The boundary conditions are specified as follows.
the solid wall: (ED):

$$-R_1 < z < R_1, \ r = \sqrt{R_1^2 - z^2}, \ V_r = 0, \ V_z = 0.$$

the input boundary (AB):

$$-R_2 < z < 0, \ r = \sqrt{R_2^2 - z^2}, \ V_r = 0, \ V_z = U_0.$$

the output boundary (BC):

$$0 < z < R_2, \ r = \sqrt{R_2^2 - z^2}, \ \frac{\partial V_r}{\partial z} = 0, \ \frac{\partial V_z}{\partial z} = 0.$$

the axis of symmetry AE ∪ DC:

$$-R_2 < z < -R_1, \ R_1 < z < R_2, \ V_r = 0, \ \frac{\partial V_z}{\partial r} = 0, \ \frac{\partial p}{\partial r} = 0.$$

METHOD OF SOLVING THE PROBLEM

A solution of the system (1) - (3) was carried out using the Patankar finite-difference scheme [36] with the SIMPLE procedure to couple the pressure and velocity fields of the fluid and the second order upwind scheme to determine the convective flows.

The implementation of this method was carried out using the software package ANSYS-Fluent. For the construction of the finite-difference grid, the program Gambit was used.

The ratio of the radii of boundaries (ABC) and (ED) are set as a constant, $R_2/R_1 = 14$. Preliminary calculations show that for larger values of R_2/R_1 no change in the calculation results take place.

Special research found that sufficient accuracy of calculations (with an error of 2%) at Re = 100 is achieved by using a computational grid of 40,000 cells.

In particular, the experimental Schiller-Naumann correlation [37] for the drag coefficient of a sphere $C_D = \dfrac{24}{\text{Re}} f_D(\text{Re})$, where $f_D(\text{Re}) = 1 + 0.15 \text{Re}^{0.687}$, is fully reproduced by the numerical solution.

The difference in the results of the numerical solutions and the experimental data does not exceed 5% for Re ≤ 200. At Re = 1000 the calculated value of C_D is lower than the experimental one by 23.7%. The deviation of the calculated drag coefficient from the experimental one can be explained by the fact that at high values of the Re number (about 1000) the turbulization of the flow begins to manifest itself, which is not taken into consideration in the calculations.

DEPENDENCE OF THE CIRCULATION ZONE SIZE ON THE REYNOLDS NUMBER

It is known that when the Reynolds number is greater than 25 [34, 38, 39] a circulation zone is formed at the rear of the sphere which is caused by the detachment of the boundary layer from the surface of the sphere, Figure 1. This fact is confirmed by our calculations.

Below we limit ourselves to describing only those geometric characteristics of the circulation zone, which are needed for the later-described model of the particle mixture sedimentation.

The dependence of the volume of the circulation zone related to the volume of the sphere on the Reynolds number is presented in Figure 2. The relative volume of the circulation zone is approximated by a polynomial of the second degree in the range of Re = 25 – 1000 with a correlation coefficient of $R^2 = 0.9998$:

$$f(\text{Re}) = -0.258 + 1.017 \frac{\text{Re}}{100} - 3.78 \cdot 10^{-2} \left(\frac{\text{Re}}{100} \right)^2 \qquad (4)$$

As follows from Equation (4) and Figure 2 the circulation zone begins to form at $\text{Re}_* = 25.6$.

The size of the circulation zone can be characterized by its length L (related to the diameter of the sphere) defined as the distance from the rear point of the sphere D to the intersection point of the limit streamline of circulation zone and the axis of symmetry (Figure 1).
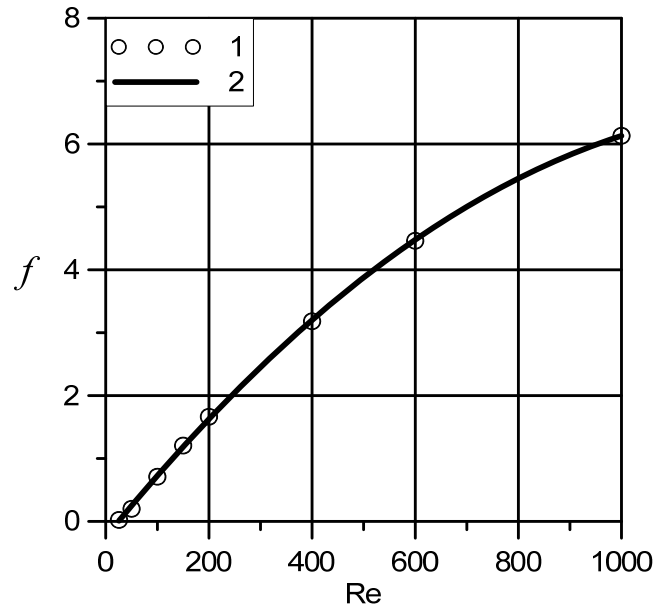

Figure 2 Dependence of the volume circulation zone on the Reynolds number. 1 - numerical experiment, 2 - approximation curve, Eq. (2)

Figure 3 shows the dependence of the length of the circulation zone L on the Reynolds number. The results of the numerical simulation shown as circles are approximated by an exponential with a correlation coefficient of $R^2 = 0.9997$:

$$L(\text{Re}) = 2.858 \cdot \exp\left(-\frac{28.778}{\text{Re}^{0.7}} \right). \qquad (5)$$

The results of experiments obtained by Taneda [39] in the range of Reynolds number from 40 to 100 are depicted in Figure 3 as triangles. A good correlation between the calculated and experimental data is observed. With an increase in the Reynolds number from 10 to 1000, an increase in length of the circulation zone is observed. The rate of growth $L(\text{Re})$ reduces when approaching the values of Re to 1000.

Thus, the relative length and the relative volume as functions of the Reynolds number can characterize the circulation zone at the rear of the sphere.

SEDIMENTATION VELOCITY OF FINE PARTICLES IN BIDISPERSE SUSPENSION

The sedimentation of a bidisperse suspension (a mixture of coarse particles with diameter d_c and fine particles with diameter d_f) is considered. Around each coarse particle of radius R_1, we construct a spherical cell of radius R_2 (Figure 1).

We suppose that during the co-settling of coarse and fine particles, the latter trapped in the circulation zone formed at the rear of the coarse particle have the same sedimentation velocity as the coarse U_c, and other fine particles settle at their own sedimentation velocity U_f.
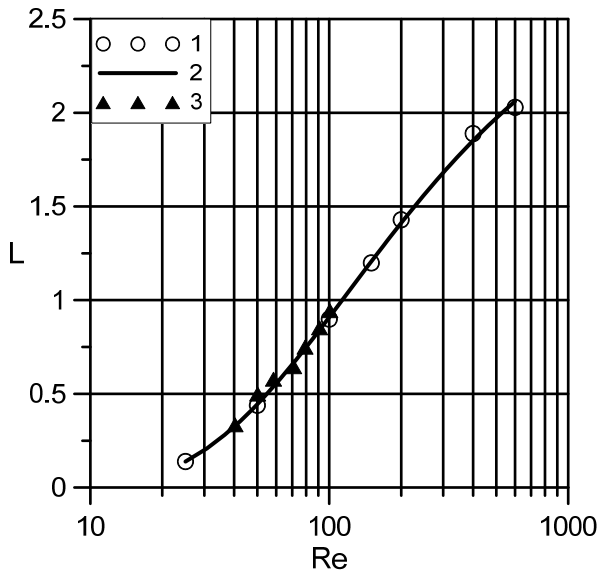
Figure 3 Dependence of the circulation zone length on the Reynolds number. 1 - numerical experiment, 2 - approximation curve, 3 - experimental data [39]

Let us assume that the considered cell has a volume υ_{cell} and the circulation zone has the volume $\upsilon_{cyrc} < \upsilon_{cell}$. Then the volume average sedimentation velocity of fine particles in the cell is determined by the following expression:

$$<U_f> = \frac{\upsilon_{sph} f(\text{Re})}{\upsilon_{cell} - \upsilon_{sph}} U_c + \frac{\upsilon_{cell} - \upsilon_{sph} f(\text{Re})}{\upsilon_{cell} - \upsilon_{sph}} U_f.$$

Here, υ_{sph} – is the volume of the coarse particle and $\text{Re} = \dfrac{d_c U_c}{\nu}$.

The equilibrium equation of forces acting on a particle during the sedimentation allows one to obtain its velocity:

$$U = \frac{\rho_s - \rho_l}{\rho_l} \frac{g \cdot d^2}{18\nu} \frac{1}{f_D(\text{Re})}. \quad (6)$$

For fine particles which can be considered as the Stokes ones $f_D(\text{Re}) = 1$ and $U_f \sim d_f^2$. For coarse particles $U_c \sim d_c^2 / f_D(\text{Re})$.

Therefore,

$$\frac{<U_f>}{U_f} = \frac{\upsilon_{sph}}{\upsilon_{cell} - \upsilon_{sph}} \frac{f(\text{Re})}{f_D(\text{Re})} \left(\frac{d_c}{d_f}\right)^2 + \frac{\upsilon_{cell} - \upsilon_{sph} f(\text{Re})}{\upsilon_{cell} - \upsilon_{sph}}.$$

As a volume fraction of the coarse particles in the suspension is expressed through the volume of the cell and the own volume of coarse particle by the relation $\alpha_c = \upsilon_{sph} / \upsilon_{cell}$, then:

$$\frac{<U_f>}{U_f} = \frac{1}{1-\alpha_c} + \frac{\alpha_c f(\text{Re})}{1-\alpha_c}\left(\frac{1}{f_D(\text{Re})}\left(\frac{d_c}{d_f}\right)^2 - 1\right). \quad (7)$$

As can be seen from the Equation (7), the volume average sedimentation velocity of fine particles increases proportionally to the square of the coarse and fine particle diameter ratio which correlates with the experimental data obtained for the settling of water-sand suspension in a plate centrifuge [40] and for the droplet creaming in a tube [41].

From (5) and (7) it also follows that the volume average sedimentation velocity of fine particles increases monotonically with increasing the volume fraction of the coarse particles. Moreover, the acceleration of sedimentation of fine particles at small α_c is proportional to α_c, in contrast to the flow at a low Re, where the acceleration is proportional to $\alpha_c^{1/3}$ [22].

An analysis of Equation (7) shows that for fixed d_c/d_f the dependence of the volume average sedimentation velocity of fine particles on the Reynolds number is non-monotonic. With the increasing of the Reynolds number the velocity increases, reaching a maximum and then decreases. Note that changing the Reynolds number in real devices is accomplished by setting the level of the tangential velocity through the inlet pressure variation.

The limits of the applicability of formula (5) are determined by the fact that the circulation zone should be completely inside the spherical cell, i.e. $d_c L(\text{Re}) + d_c/2 < R_2$. Whence it follows that a formal limitation on the volume fraction of coarse particles depends on the Reynolds number:

$$\alpha_c \leq \frac{1}{\left[1 + 2L(\text{Re})\right]^3}. \quad (8)$$

As follows from (7) the maximum growth of the volume average sedimentation velocity of fine particles during the settling together with coarse particles is obtained at the maximum possible value of α_c, which is determined by (8)

$$\alpha_m(\text{Re}) = \left[1 + 2L(\text{Re})\right]^{-3}, \text{ Figure 4.}$$

In the region of practical interest, Re is about 10^2 and α_m may be around a few per cent. This is the typical range of the coarse and fine particles concentration ratio in the suspension.

Equations (7) and (8) give a maximum of the average sedimentation velocity of fine particles depending on Re:

$$\frac{<U_f>_m}{U_f} = \frac{1}{1-\alpha_m(\text{Re})} + \\ + \frac{\alpha_m(\text{Re})f(\text{Re})}{1-\alpha_m(\text{Re})}\left(\frac{1}{f_D(\text{Re})}\left(\frac{d_c}{d_f}\right)^2 - 1\right). \quad (9)$$
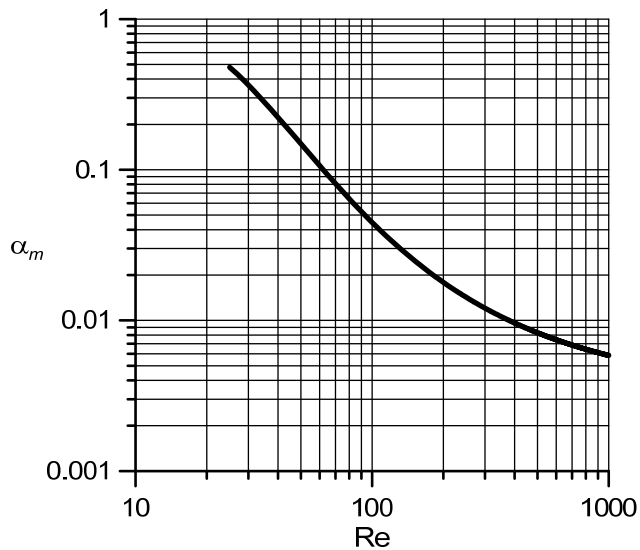
Figure 4 Maximum possible volume fraction of coarse particles

Figure 5 shows the dependence of the maximum value of the average sedimentation velocity of fine particles on the Reynolds number for different values of $\left(d_c/d_f\right)^2$. It is evident that the dependence is non-monotonic due to the different rates of increasing the length and volume of the circulation zone with an increasing Reynolds number.
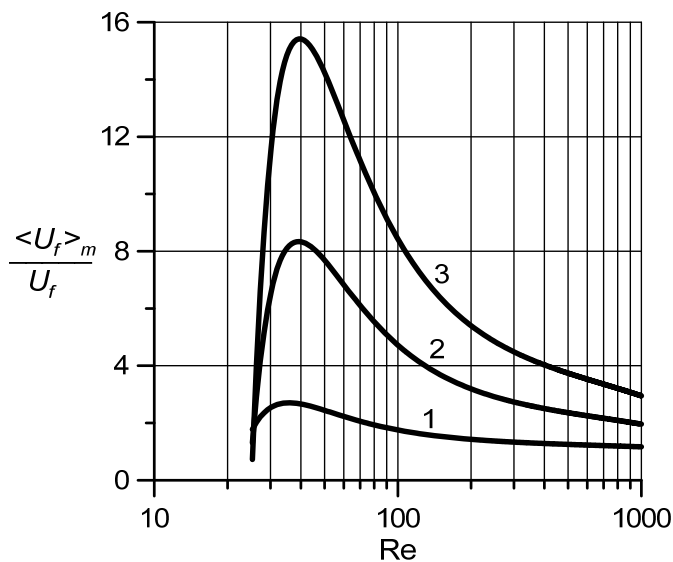

Figure 5 Maximum possible average volume sedimentation velocity of fine particles.
$$1 - \left(d_c/d_f\right)^2 = 100, 2 - 500, 3 - 1000$$

It is noteworthy that the increase in the sedimentation velocity of fine particles by described mechanism is limited and should not be expected to be higher than 10 times.

The Eq. (6) taken at $\mathrm{Re} = \mathrm{Re}_*$ allows one to determine the minimum size $d_{c,\min}$ of coarse particle behind which a circulation zone can be formed:

$$d_{c,\min} = \left(\mathrm{Re}_* \cdot f_D\left(\mathrm{Re}_*\right) \frac{\rho_l}{\left(\rho_s - \rho_l\right)} \frac{18v^2}{g} \right)^{1/3} .$$

The circulation zone in operating conditions of a hydrocyclone (let's take g = 1000 m/s^2)) with a quartz water-sand suspension is formed for particles larger than 88 microns, and in the gravitational settling – for particles larger than 400 microns. Thus, the described mechanism of accelerating the particles sedimentation in a suspension can probably be realized if the suspension includes particularly large particles.

CONCLUSION

Based on a numerical simulation of the laminar flow of incompressible viscous fluid around a spherical particle the geometric characteristics (volume and length) of the circulation zone formed in the rear of the sphere depending on the Reynolds number for 25 <Re <1000 were obtained.

The formula for the volume average sedimentation velocity of fine particles settling in the presence of coarse particles (in the case of bidisperse suspension) under the assumption that the fine particles are trapped in the circulati.on zone settle at a velocity of coarse ones was obtained. An expression for the maximum sedimentation velocity of fine particles shows non-monotonic behavior depending on the Reynolds number.

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