A NUMERICAL STUDY OF NATURAL CONVECTIVE HEAT TRANSFER FROM A HORIZONTAL ISOTHERMAL SQUARE ELEMENT IMBEDDED IN AN ADIABATIC SURFACE WITH A PARALLEL ADIABATIC COVERING SURFACE

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ABSTRACT

Natural convective heat transfer from a square horizontal flat isothermal heated element imbedded in a larger flat square adiabatic surface with a square flat horizontal adiabatic surface mounted parallel to the heated surface at a relatively short distance from it has been numerically studied. The surface of the heated element is in the same plane as the surface of the surrounding adiabatic material. The square heated element considered in this study is at a higher temperature than that of the surrounding fluid. Both the case where the square heated element is facing upwards and the surrounding adiabatic covering surface is above the heated element (upward facing case) and the case where the square heated element is facing downwards and the surrounding adiabatic covering surface is below the heated element (downward facing case) have been considered. The situation considered is a simplified model of some situations that arise in engineering practice examples occurring in some electrical and electronic component cooling problems. In this study, the range of conditions considered is such that laminar, transitional, and turbulent flows occur. The purpose of this study was to numerically determine how the heat transfer rate from the square heated element varies with the distance of the adiabatic covering surface from the heated element. The solution was obtained by numerically solving the governing equations subject to the boundary conditions using the commercial CFD solver ANSYS FLUENT[©] using the kepsilon turbulence model with full account being taken of buoyancy force effects. Because of the applications that motivated this study, results have been obtained for a Prandtl number of 0.74, i.e., effectively the value for air. The effect of the dimensionless distance between the heated element and the cover on the variation of the Nusselt number with Rayleigh number has been studied in detail for both the upward and the downward facing cases.

INTRODUCTION

The natural convective heat transfer rate from a horizontal square isothermal element imbedded in a larger square flat adiabatic surface has been studied numerically. The surface of the heated element is in the same plane as the surface of the surrounding adiabatic surface and there is a square flat horizontal adiabatic surface mounted parallel to the heated surface at a relatively short distance from it, i.e., there is a covering surface over the heated element. This square adiabatic covering surface has the same size as the square adiabatic surface in which the heated element is imbedded. The flow situation considered is therefore as shown schematically in Figure 1.

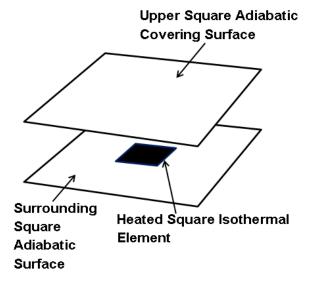
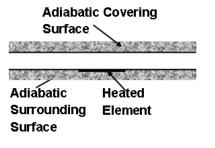
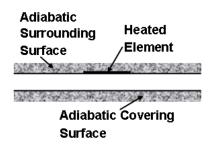


Figure 1 Flow situation considered



Facing Upward



Facing Downward

Figure 2 Upward and downward facing heated element situations

The square heated element considered in this study is at a higher temperature than that of the surrounding fluid. Both the case where the square heated element is facing upwards and the surrounding adiabatic covering surface is above the heated element (upward facing case) and the case where the square heated element is facing downwards and the surrounding adiabatic covering surface is below the heated element (downward facing case) have been considered. These cases are as shown in Figure 2. This study considers a simplified model of some situations that arise in engineering practice. Situations of this general type occur, for example, in some electrical and electronic component cooling problems. Here, the range of conditions considered is such that laminar, transitional, and turbulent flows can occur over the heated element. The aim of the present numerical study was to numerically investigate the variation of the heat transfer rate from the square heated element with the distance of the adiabatic covering surface from the heated element for both the upward and downward facing element cases.

NOMENCLATURE

A	$\lceil m^2 \rceil$	Surface area of heated element
g	$[m/s^2]$	Gravitational acceleration
h	[m]	Vertical distance of covering surface from heated element
H	[-]	Dimensionless vertical distance of covering surface from
		heated element, h/w
k	[W/mK]	Thermal conductivity
Pr	[-]	Prandtl number
Nu	[-]	Nusselt number
$\overline{Q'}$	[W]	Mean heat transfer rate from element
Ra	[-]	Rayleigh number
T	[K]	Temperature

T_f	[K]	Undisturbed fluid temperature		
T_w	[K]	Heated element wall temperature		
w	[m]	Side length of square heated element		
W_{out}	[m]	Side length of surrounding and covering adiabatic surfaces		
W_{out}	[-]	Dimensionless side length of surrounding and covering adiabatic surfaces, w_{out}/w		
Greek symbols				
α	$[m^2/s]$	Thermal diffusivity		
β	[1/K]	Coefficient of thermal expansion		
v	$[m^2/s]$	Kinematic viscosity		
ρ	$[kg/m^3]$	Density		

There have been many studies of natural convective heat transfer from upward facing heated horizontal surfaces without a covering surface, e.g., see [1] to [16]. Most of these, however, have considered situations that involve only laminar flow. There have also been many studies of natural convective heat transfer from downward facing heated horizontal surfaces without a covering surface, e.g., see [17] to [23]. The present study differs from these available studies by considering the effect of the covering surface and by obtaining results for a wide range of Rayleigh numbers that cover conditions in which laminar, transitional, and turbulent flow occur. Some investigations of the effect of a covering surface on natural convective heat transfer from heated horizontal surfaces have been undertaken, e.g., see [24] and [25]. However, these studies cover narrower ranges of the Rayleigh number than considered in the present work.

SOLUTION PROCEDURE

Steady flow has been assumed. Fluid properties have been assumed constant except for the density change with temperature that gives rise to the buoyancy forces. This was treated by means of the Boussinesq type approximation. Effects of radiant heat transfer have been neglected. Allowance has been made for the possibility that turbulent flow can occur in the system. In order to deal with this, the basic k-epsilon turbulence model has been used with standard wall functions and with full account being taken of buoyancy force effects. The numerical approach adopted to allow for the development of turbulence, i.e., solving the Reynolds averaged governing equations together with a turbulence model for all conditions considered and then assessing the solutions obtained with increasing Reynolds number in order to determine when turbulence effects begin to develop has been used quite extensively. For example, this approach was used in the early studies [26-28]. Some work on the use of this approach in natural convective flows has also been undertaken [29, 30]. The commercial CFD solver ANSYS FLUENT® has been used to numerically solve the three-dimensional governing equations subject to the boundary conditions. It has been assumed that the flow is symmetric about the longitudinal centre-lines shown in Figure 3.

Extensive grid independence and convergence-criteria independence testing was undertaken indicating that with the grids used in obtaining the results presented here the heat transfer results are grid- and convergence criteria independent to within about one per cent.

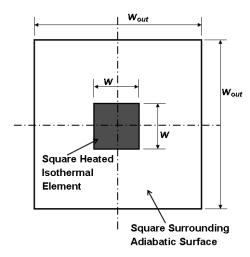


Figure 3 Heated element and surrounding adiabatic surface

RESULTS

The solution has the following parameters:

1. The Rayleigh number, Ra, based on the side length, w, of the square heated element (see Figure 3) and the difference between the temperature of the surface of the heated element, T_w , and the temperature of the undisturbed fluid well away from the system, T_f , i.e.:

$$Ra = \frac{\beta g w^3 (T_w - T_f)}{v \alpha} \tag{1}$$

- 2. The dimensionless size of the square surrounding adiabatic surface and the square adiabatic covering surface, $W_{out} = w_{out} / w$ (see Figure 3).
- 3. The dimensionless vertical distance of the adiabatic covering surface from the heated element, H = h / w (see Figure 3).
- 4. The Prandtl number, Pr.
- 5. The orientation of the heated element, i.e., facing upward or facing downward (see Figure 2).

Results have been obtained only for a Prandtl number of 0.74, i.e., effectively the value for air because of the applications that motivated this study. Results will be presented here only for $W_{out} = 4$. Results obtained for other values of W_{out} showed the same basic characteristics as those presented here. Dimensionless heated element to adiabatic covering surface distances, H, of between 0.125 and 1 and Rayleigh numbers between approximately 10^4 and 10^{12} have been considered. Results have been obtained for both upward and downward facing heated element orientations.

The mean heat transfer rate from the heated surface, \overline{Q} ', has been expressed in terms of a mean Nusselt number based on the side length, w, of the square heated element and on the difference between the temperature of the surface of the heated element, T_w , and the temperature of the undisturbed fluid well away from the system, T_6 i.e.:

$$Nu = \frac{\bar{Q}'w}{kA(T_w - T_f)}$$
 (2)

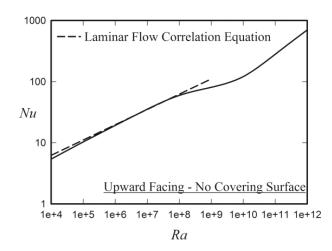


Figure 4 Variation of Nusselt number with Rayleigh number for upward facing heated element with no covering surface

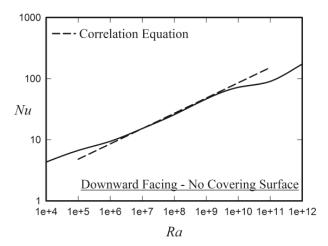


Figure 5 Variation of Nusselt number with Rayleigh number for downward facing heated element with no covering surface

where A is the surface area of the heated surface, i.e., w^2 . Because values of Pr and W_{out} are fixed in this study, Nu is a function of Ra, H, and the element orientation, i.e., upward or downward facing.

Results for the case where there is no covering surface will first be considered. The variations of Nusselt number with Rayleigh number for this case for an upward facing heated element and for a downward facing heated element are shown in Figures 4 and 5 respectively. Also shown in these figures are the results given by the following commonly used empirical equations for laminar flow over a horizontal square isothermal surface, e.g. see for example [31] and [32].

Upward facing surface:

$$Nu = 0.622 Ra^{1/4} (3)$$

Downward facing surface:

$$Nu = 0.27 \, Ra^{1/4} \tag{4}$$

Figures 4 and 5 illustrate that these empirical equations produce results that are in quite good agreement with the numerical results for the upward facing element for Rayleigh numbers between 10⁵ and 10⁸ and for the downward facing element for Rayleigh numbers between 10⁶ and 10⁹.

The case of a covered heated element facing upward will next be considered. The effect of the dimensionless vertical distance of the adiabatic covering surface from the heated element, H, for this case is demonstrated by the variations of Nusselt number with Rayleigh number for various values of H shown in Figures 6 to 11. Also shown in Figures 7 to 11 is the variation of Nusselt number with Rayleigh number for the nocover case. This variation is not shown in Figure 6 because for H = 1 the covered element results for an upward facing element are essentially the same as the no-cover results. From Figures 7 to 11 it will be seen that the covered element variations of Nusselt number with Rayleigh number differ from that for the no-cover case, the difference increasing as H decreases. It will be seen that, generally, the covered element Nusselt number results are lower than the no-cover values at low Reynolds numbers and are higher than the no-cover values in the transition region. The complex form of the variation of Nusselt number with Rayleigh number for the covered element case is the result of changes in the flow pattern with Rayleigh number. The effect of H on the Nusselt number variation for the upward facing covered element case is further illustrated by the results given in Figure 12. This figure shows the variation of Nusselt number with H for various Rayleigh number values. For the lowest Rayleigh number for which results are given it will be seen that the presence of the covering surface affects the Nusselt number value when H is less than approximately 1. For the intermediate Rayleigh numbers considered the value H at which the presence of the covering surface effects the Nusselt number value decreases with increasing Rayleigh number being approximately 0.4 at a Rayleigh number of 10⁸. At the higher Rayleigh number values considered the presence of the covering surface effects the conditions under which transition occurs and the value of H at which the presence of the covering surface affects the Nusselt number value increases.

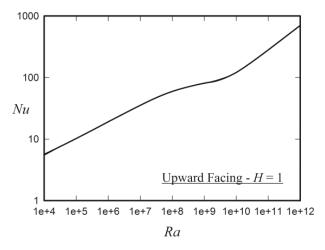


Figure 6 Variation of Nusselt number with Rayleigh number for upward facing heated element with covering surface for a dimensionless element to covering surface distance of 1

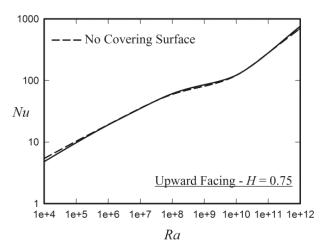


Figure 7 Variation of Nusselt number with Rayleigh number for upward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.75

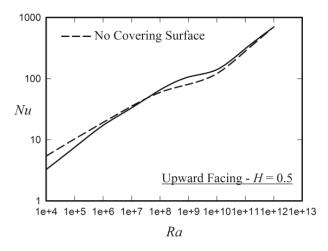


Figure 8 Variation of Nusselt number with Rayleigh number for upward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.5

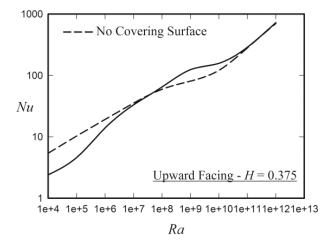


Figure 9 Variation of Nusselt number with Rayleigh number for upward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.375

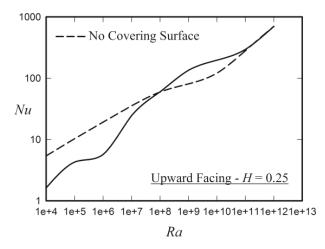


Figure 10 Variation of Nusselt number with Rayleigh number for upward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.25

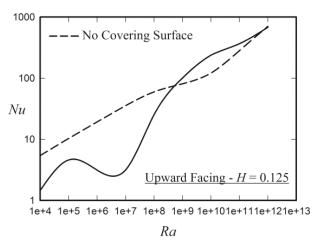


Figure 11 Variation of Nusselt number with Rayleigh number for upward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.125.

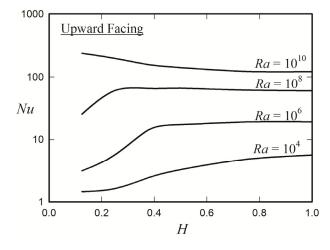


Figure 12 Typical variations of Nusselt number with dimensionless element to covering surface distance for various Rayleigh numbers for upward facing heated element

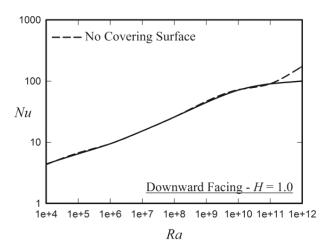


Figure 13 Variation of Nusselt number with Rayleigh number for downward facing heated element with covering surface for a dimensionless element to covering surface distance of 1

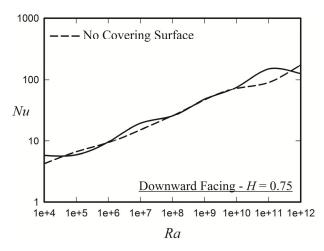


Figure 14 Variation of Nusselt number with Rayleigh number for downward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.75

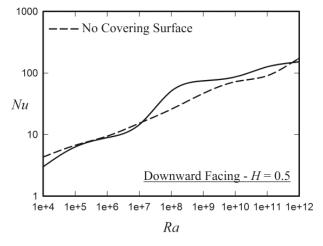


Figure 15 Variation of Nusselt number with Rayleigh number for downward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.5

The results for the case of a covered heated element facing downward will be considered next. The effect of the dimensionless vertical distance of the adiabatic covering surface from the heated element, H, for this case is illustrated by the variations of Nusselt number with Rayleigh number for various values of H shown in Figures 13 to 18. Also shown in these figures is the variation of Nusselt number with Rayleigh number for the no-cover case. It will be seen from Figures 13 to 18 that the difference between the covered element variations of Nusselt number with Rayleigh number and the variations for the no-cover case are generally smaller than the difference that exists in the upward facing element case. The effect of H on the Nusselt number variation for the downward facing covered element case is further illustrated by the results given in Figure 19. This figure shows the variation of Nusselt number with H for various Rayleigh number values. For the lowest Rayleigh number for which results are given it will be seen that the presence of the covering surface affects the Nusselt number value when H is less than approximately 1. At the higher Rayleigh numbers considered the value H at which the presence of the covering surface affects the Nusselt number value is approximately 0.8.

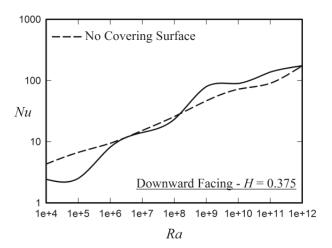


Figure 16 Variation of Nusselt number with Rayleigh number for downward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.375

CONCLUSIONS

The results of the present study indicate that:

- The effect of the dimensionless distance of the covering surface from the heated element on the mean heated element Nusselt number is significantly different for the upward facing element than it is for the downward facing element.
- For the upward facing element case the covered element Nusselt number results are generally lower than the nocover values at low Reynolds numbers and are generally higher than the no-cover values in the transition region.
- 3. For the upward facing element case, the value of the dimensionless distance of the covering surface from the heated element at which the presence of the covering

- surface begins to affect the mean element Nusselt number lies between 0.4 and 1, the value depending on the Rayleigh number.
- 4. For the downward facing element case, the difference between covered element variations of Nusselt number with Rayleigh number and the variations for the nocover case are generally smaller than in the upward facing element case.
- 5. For the downward facing element case, the value of the dimensionless distance of the covering surface from the heated element at which the presence of the covering surface starts to effect the mean element Nusselt number lies between approximately 0.8 and 1, this value depending on the Rayleigh number.

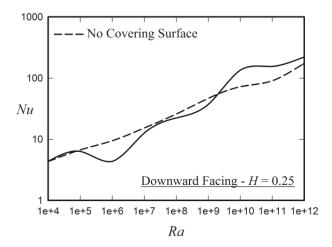


Figure 17 Variation of Nusselt number with Rayleigh number for downward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.25

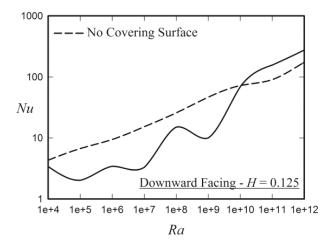


Figure 18 of Nusselt number with Rayleigh number for downward facing heated element with covering surface for a dimensionless element to covering surface distance of 0.125

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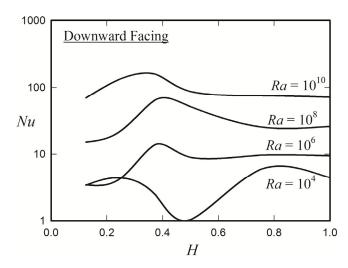


Figure 19 Typical variations of Nusselt number with dimensionless element to covering surface distance for various Rayleigh numbers for downward facing heated element

REFERENCES

- [1] Al-Arabi M., and El-Riedy M.K., Natural convection heat transfer from isothermal horizontal plates of different shapes, *International Journal of Heat and Mass Transfer*, Vol. 19, No. 12 1976, pp. 1399-1404.
- [2] Clifton J.V., and Chapman A.J., Natural-convection on a finitesize horizontal plate, *International Journal of Heat and Mass Transfer*, Vol. 12, No. 12, 1969, pp. 1573-1584.
- [3] Goldstein R.J., Sparrow E.M., and Jones D.C., Natural convection mass transfer adjacent to horizontal plates, *International Journal of Heat and Mass Transfer*, Vol. 16, No. 5, 1973, pp. 1025-1035.
- [4] Hassan K.-E., and Mohamed S.A., Natural convection from isothermal flat surfaces, *International Journal of Heat and Mass Transfer*, Vol. 13, No. 12, 1970, pp. 1873-1886.
- [5] Hossain M.A., and Takhar H.S., Thermal radiation effects on the natural convection flow over an isothermal horizontal plate, *Journal of Heat and Mass Transfer*, Vol. 35, No. 4, 1999, pp. 321-326.
- [6] Kitamura K., and Kimura F., Heat transfer and fluid flow of natural convection adjacent to upward-facing horizontal plates, *International Journal of Heat and Mass Transfer*, Vol. 38, No. 17, 1995, pp. 3149-3159.
- [7] Kozanoglu B., and Lopez J., Thermal boundary layer and the characteristic length on natural convection over a horizontal plate, *Journal of Heat and Mass Transfer*, Vol. 43, No. 4, 2007, pp. 333-339.
- [8] Lewandowski W.M., Radziemska E., Buzuk M., and Bieszk H., Free convection heat transfer and fluid flow above horizontal rectangular plates, *Applied Energy*, Vol. 66, No. 2, 2000, pp. 177-197.
- [9] Lloyd J.R., and Moran W.R., Natural convection adjacent to horizontal surface of various planforms, *Journal of Heat Transfer*, Vol. 96, No. 4, 1974, pp. 443-447.
- [10] Martorell I., Herrero J., and Grau F.X., Natural convection from narrow horizontal plates at moderate Rayleigh numbers, *International Journal of Heat and Mass Transfer*, Vol. 46, No. 13, 2003, pp. 2389-2402.
- [11] Prétot S., Zeghmati B., and Le Palec G., Theoretical and experimental study of natural convection on a horizontal plate,

- Applied Thermal Engineering, Vol. 20, No. 10, 2000, pp. 873-891.
- [12] Prétot S., Zeghmati B., and Caminat Ph., Influence of surface roughness on natural convection above a horizontal plate, *Advances in Engineering Software*, Vol. 31, No. 10, 2000, pp. 793-801.
- [13] Radziemska E., and Lewandowski W.M., The effect of plate size on the natural convective heat transfer intensity of horizontal surfaces, *Heat Transfer Engineering*., Vol. 26, No. 2, 2005, pp 50-53.
- [14] Restrepo F., and Glicksman L.R., The effect of edge conditions on natural convection from a horizontal plate, *International Journal of Heat and Mass Transfer*, Vol. 17, No. 1, 1974, pp. 135-142.
- [15] Rotem Z., and Claassen L. Natural convection above unconfined horizontal surfaces, *J. Fluid Mechanics*, Vol. 38, No. 1, 1969, pp. 173-192.
- [16] Yousef W.W., Tarasuk J.P., and McKeen W.J., Free convection heat transfer from upward-facing isothermal horizontal surfaces, *Journal of Heat Transfer*, Vol. 104, 1982, pp. 493-500.
- [17] Aihara T., Yamada Y., Endö S., Free convection along the downward-facing surface of a heated horizontal plate, *International Journal of Heat and Mass Transfer*, Vol. 15, No. 12, 1972, pp. 2535-2538.
- [18] Chambers B.B., and Lee T.T., A numerical study of local and average natural convection Nusselt numbers for simultaneous convection above and below a uniformly heated horizontal thin plate, *Journal of Heat Transfer*, Vol. 119, No. 1, 1997, pp. 102-108, (1997). doi:10.1115/1.2824074.
- [19] Tetsu F., Hiroshi H., and Itsuki M., A theoretical study of natural convection heat transfer from downward-facing horizontal surfaces with uniform heat flux, *International Journal of Heat* and Mass Transfer, Vol. 16, No. 3, 1973, pp. 611-627.
- [20] Kwak C.E., and Song T.H., Natural convection around horizontal downward-facing plate with rectangular grooves: experiments and numerical simulations, *International Journal of Heat and Mass Transfer*, Vol. 43, No. 5, 2000, pp. 825-838.
- [21] Hatfield D.W., and Edwards D.K., Edge and aspect ratio effects on natural convection from the horizontal heated plate facing downwards, *International Journal of Heat and Mass Transfer*, Vol. 24, No. 6, 1981, pp. 1019-1024.
- [22] Wei J.J., Yu B., Wang H.S., and Tao W.Q., Numerical study of simultaneous natural convection heat transfer from both surfaces of a uniformly heated thin plate with arbitrary inclination, *Journal of Heat and Mass Transfer*, Vol. 38, Nos. 4-5, 2002, pp. 309-317
- [23] Wei J.J., Yu B., and Kawaguchi Y., Simultaneous naturalconvection heat transfer above and below an isothermal horizontal thin plate, Numerical Heat Transfer A-Appl., Vol. 44, No. 1, 2003, pp. 39-51.
- [24] Sparrow E.M., and Carlson C.K., Local and average natural convection Nusselt numbers for a uniformly heated, shrouded or unshrouded horizontal plate, *International Journal of Heat and Mass Transfer*, Vol., 29, No. 3, 1986, pp. 369-379.
- [25] Kitamura K., and Asakawa T., Fluid flow and heat transfer of natural convection over upward-facing, horizontal, heated plate shrouded by a parallel insulated plate, *Heat Transfer Asian Research*, Vol. 29, No. 4, 2000, pp. 333-346.
- [26] Saville, A.M., Evaluating turbulence model predictions of transition. An ERCOFTAC special interest group project, Applied Scientific Research, Vol. 51, 1993, pp. 555-562.
- [27] Schmidt, R.C., and Patankar, S.V., Simulating boundary layer transition with low-Reynolds number k- ε turbulence models:

- Part 1-An evaluation of prediction characteristics, *Journal of Turbomachinery*, Vol. 113, 1991, pp. 10-17.
- [28] Zheng, S., Liu, C., Liu, F., and Yang, C.I., Turbulent transition simulation using the k-ω model, The International Journal for Numerical Methods in Engineering, Vol. 42, 1998, pp. 907-926.
- [29] Plumb, O.A., and Kennedy, L.A., Application of a k-ε turbulence model to natural convection from a vertical isothermal surface, *Journal of Heat Transfer*, Vol. 99, 1977, pp. 79-85.
- [30] Oosthuizen, P.H., and Naylor, D., A numerical study of laminar-to-turbulent transition in the flow over a simple recessed window-plane blind system, *Proceedings of the 4th Canadian Solar Buildings Conference*, Toronto, June 25-27, 2009.
- [31] Burmeister L.C., Convective Heat Transfer, John Wiley & Sons, Inc., 2nd Edition, 1993, pp. 423-424.
- [32] Sucec, J., *Heat Transfer*, Wm. C. Brown Publisher, 1985, pp. 636-637.