# Cr (VI)-CONTAINING ELECTRIC FURNACE DUST AND FILTER CAKE: CHARACTERISTICS, FORMATION, LEACHABILITY AND STABILISATION

by

## Guojun Ma

Submitted in partial fulfilment of the requirements for the degree

### **Philosophiae Doctor**

(Metallurgical Engineering)

in the Faculty of Engineering, Built Environment and Information Technology,
University of Pretoria, Pretoria

12 December 2005

University of Pretoria etd – Ma, G (2006)

To my lovely wife Yinhua, my son, Junteng and my parents

## Acknowledgements

The thesis has been carried out at Department of Materials Science and Metallurgical Engineering, University of Pretoria. I would like to express my sincere gratitude to my supervisor Prof. A.M. Garbers-Craig for her valuable suggestions, discussions and continuous encouragement during the past three years.

I also wish to thank Profs. P.C. Pistoruis and J.M.A. Geldenhuis for their invitation to join in the interesting project and their fruitful discussions. Special thanks are also given to China Scholarship Council (CSC) and Wuhan University of Science and Technology (WUST, P. R. China) as well as Mr. Yanggeng Wei from the education section of Chinese embassy in South Africa for their understanding, help and support during the study period.

The Technology and Human Recourses for Industry Program (THRIP) are greatly acknowledged for the financial support of the project. Thanks are also due to Messrs. Johan Ackeman, Peter Scurr and Nathan Antony from Columbus stainless and Dewald van Niekerk from Middleburg Ferrochrome (MFC) for their discussions and supplying the samples.

I am also greatly indebted to all the personnel and postgraduates at Department of Materials Science and Metallurgical Engineering, especially Mrs Sarah Havenga and Mr Johann Borman (deceased) for their help, and Industrial Metals and Minerals Research Institute (IMMRI) for their friendly support, specifically Prof. Tom von Moltke (XPS), Mr. Carl Coetzee (SEM) and Ms. Junior Mogwaneng (FT-IR) for their help on the relative experimental works and discussions.

Thanks also extend to Dr. Sabine M.C. Verryn (XRD) (Department of Geology), Mrs Maggi Loubser (XRF) (Department of Geology) and Mrs Mila Maksa (TG/DTA) (Department of Chemistry) for their help on the X-ray and thermal analytical experiments,

and Mr. Vusi Mulaudzi (Department of Chemistry) for his discussion on the analysis of Cr (VI).

Finally, I wish to thank my parents (Mr. Anlan Ma and Mrs Anxiang He), my wife (Mrs Yinhua Zhou) for their endless love and unconditional support.

Guojun Ma

12 December 2005

Pretoria, South Africa

Cr (VI)-CONTAINING ELECTRIC FURNACE DUST AND FILTER CAKE: CHARACTERISTICS, FORMATION,
LEACHABILITY AND STABILISATION

Candidate: Guojun Ma

Supervisor: Prof. A.M. Garbers-Craig

**Department:** Department of Materials Science and Metallurgical Engineering

**Degree:** Philosophiae Doctor

#### **Abstract**

In South Africa, the ferrochromium industry produces approximately 100,000 t bag house filter dust and slurry, while the stainless steel industry produces 24,000 t of dust annually [17,39]. The toxic substances in these wastes potentially pose a threat to the environment and human health, especially Cr (VI) due to its toxic, carcinogenic, highly soluble and strongly oxidizing properties. Therefore, the existence and treatment of wastes from stainless steel and ferrochrome production remain a challenge and an issue of concern. The increase of environmental legislation globally and the trend towards sustainable development are drives for alternatives to landfill.

In the present thesis, the characteristics, formation mechanisms, leachability and stabilisation of the Cr (VI)-containing electric furnace dust and filter cake were investigated using various techniques such as XRD, XRF, TG/DTA, XPS, SEM-EDS, FT-IR, Raman spectrometer and UV/Vis spectrometer.

The study on the characteristics of these wastes showed that the electric furnace dust and filter cake are very fine particles. The electric furnace dust has bulk densities that vary between 0.49 and 2.42gcm<sup>-3</sup>, and has low moisture contents. The main phases that are present in the stainless steel plant dust are the (Mg,Fe,Mn,Cr)<sub>3</sub>O<sub>4</sub> spinel phase, quartz, Ca(OH)<sub>2</sub> and nickel. The dominant phases of the coarse fraction of ferrochrome plant dust are chromite, partly altered chromite, quartz and carbon, while the main components

of the fine fractions include chromite, SiO<sub>2</sub>, ZnO, NaCl and Mg<sub>2</sub>SiO<sub>4</sub>. The major phase present in the filter cake is CaF<sub>2</sub>. It is assumed that Cr (VI)-containing species in ferrochrome dust are generated at the top of the SAF or in the off-gas duct, as Cr (VI) is found on the surface of the dust.

Stainless steel dust forms by the entrainment of charge materials, evaporation or volatilisation of elements and ejection of slag and metal by spitting or the bursting of gas bubbles. It was found that ferrochrome dust is formed by the ejection of slag and metals droplets from the electrode hole, the entrainment of charge materials, vaporisation as well as the formation and precipitation of compounds from vaporised species in the off-gas duct. Filter cake contains crystal phases (CaF<sub>2</sub> and CaSO<sub>4</sub>) and metal rich amorphous phases. It is formed due to super saturation and precipitation.

Leaching experiments on the wastes showed that Cr (VI) rapidly leaches out by distilled water. The aging experiment of the stainless steel plant dust and filter cake shows that the Cr (III) species in these wastes can be oxidised into Cr (VI) in the presence of lime at room temperature. Increasing the molar ratio of CaO to  $Cr_2O_3$  and increasing temperature promotes the oxidation of Cr (III) into Cr (VI). Cr (VI) in the wastes can also be reduced into Cr (III) possibly by Fe (II).

Bricks were produced by mixing wastes (stainless steel plant dust, ferrochrome dust and filter cake) and clay. The optimum sinter parameter was found to be 1100°C and 5 hours for a 50wt% SPD-50wt% AS mixture in the brick. Decreasing sinter temperature, increasing waste content in the brick and reducing sinter time increase the Cr (VI) leachability. The leachability of Cr(VI) is strongly influenced mass%CaO/mass%SiO<sub>2</sub> ratio and alkali metal oxides content in the wastes. Ferrochrome dust and filter cake that were sintered with 50% AS clay at 1000°C for 5 hours could not be stabilised as the concentrations of zinc and/or Cr (VI) from the stabilised wastes in the modified TCLP and ASTM D 3987-85-tests exceed the regulation limits. The emission factors from the stabilised wastes (SPD, FCD1, FCD2 and FC) are similar to those reported for the cement industry.

Semi-dynamic leaching tests indicated that the predominant leaching mechanisms of chromium species are initial surface wash-off followed by matrix diffusion. The cumulative release fractions of chromium from the solidified wastes are lower than 2% over a period of approximately 5 months. More than 80% of the leachable chromium from the stabilised products is Cr (VI) species.

**Keywords:** Cr (VI), dust, filter cake, waste management, leachability, stabilisation, sintering, stainless steel, ferrochrome, electric furnace

# Contents

Acknowledgements
Abstract
Contents
List of Figures
List of Tables

Chapter 1 Introduction	1
1.1 Background	1
1.2 Objectives of this project	3
1.3 Structure of the thesis	4
Chapter 2 The characteristics, formation mechanisms and treatment processes of Cr (VI)-containing pyrometallurgical wastes: a review	
2.1 Introduction	5
2.2 The characterisation of electric furnace dust and filter cake	7
2.3 Formation mechanisms of electric furnace dust and filter cake	13
2.3.3 The formation of filter cake in the waste acid treatment plant	
2.4 Treatment processes of electric furnace dust and filter cake	17
2.4.3Solidification/stabilisation	
2.5 Conclusions	24
Chapter 3 The characteristics of the Cr (VI)-containing electric furnace dust an filter cake from a stainless steel waste treatment plant	
3.1 Introduction	26
3.2 Experimental	28
3.2.1 Waste materials and sample preparation	
3.3 Results	
3.3.1 Particle Size Distribution, Bulk Density, Moisture Content and pH	
3.3.2 Chemical Composition and Phase Composition of the EF Dusts and FC 3.3.3 TG/DTA Analysis	

3.4 Discussion	45
3.5 Conclusions	47
Chapter 4 The formation mechanisms of Cr(VI)-containing electric furnace and filter cake from a stainless steel waste treatment plant	
4.1 Experimental	49
4.1.1 Sample Preparation	49
4.1.2 Analytical Methods	49
4.2 Results	49
4.3 Discussion	55
4.3.1 The formation mechanisms of stainless steel plant dust	55
4.3.2 The formation mechanisms of the ferrochrome dust	
4.3.3 The formation mechanisms of filter cake	
4.3.4 Measures to reduce waste generation	61
4.4 Conclusions	63
Chapter 5 The leachability of the Cr (VI)-containing electric furnace dust an cake from a stainless steel waste treatment plant	
5.1 Introduction	64
5.2 Experimental	65
5.2.1 Sample preparation	
5.2.2 Experiment methods	66
5.3 Results and discussion	67
5.3.1 TCLP and ASTM D 3987-85 tests	67
5.3.2 Static distilled water and nitric acid leaching tests	
5.3.3 Effect of stirring speed on the leachability of Cr (VI) from stainless ste	
5.2 1 Effect of temporature on the leach shility of Cv (VI) from stainless stop	
5.3.4 Effect of temperature on the leachability of Cr (VI) from stainless stee 5.3.5 Effect of pH on the leachability of Cr (VI) from stainless steel dust	
5.3.6 The leachability of Cr (VI) from ferrochrome dusts and filter cake	
5.4 Conclusions	
5.4 Conclusions	/ /
Chapter 6 The aging behaviour of Cr (VI)-containing Electric furnace dust filter cake from a stainless steel waste treatment plant	
6.1 Introduction	
6.2 Experimental	
6.2.2 Leaching experiment and analysis methods	
·	
6.3 Results	
6.3.2 Effect of particle size of the wastes on the aging behaviour of Cr (VI)	
6.3.3 Effect of atmosphere on the aging behaviour of Cr (VI)	

6.4 Discussion	87
6.5 Conclusions	91
Chapter 7 Stabilisation of Cr (VI) through sintering using silica-rich clay, Part Synthetic samples	
7.1 Introduction	
7.2 Experimental	
7.2.1 Materials	
7.2.2 Analytical techniques	
7.3 Results and discussion	95
7.3.1 Characteristics of the clays	
7.3.2 Leaching behaviour of Cr(VI) from the sintered brick	
7.3.3 Chromium emissions during sintering process	106
7.4 Conclusions	108
Chapter 8 Stabilisation of Cr (VI) through sintering using silica-rich clay, Part	
Electric furnace dust and filter cake	
8.1 Introduction	
8.2 Experimental	
8.2.1 Sample preparation	
8.2.3 Analytical methods	
8.3 Results and discussion	111
8.3.1 Effect of clay type on the leachability of Cr (VI)	
8.3.2 Effect of leach time on the leachability of Cr (VI) in the modified TCLP to	
8.3.3 Influence of sinter temperature on the leachability of Cr (VI)	
8.3.4 Influence of the SPD content of the brick on the leachability of Cr (VI)	
8.3.5 Influence of sinter time on the leachability of Cr (VI)	
8.3.6 The leachability of other toxic substances from the stabilised wastes	
8.3.7Crystalline phases present in and microstructure of the sintered brick 8.3.8 Cr (VI) stabilisation in the sintered brick	
8.3.9 Stabilisation of Cr (VI) in ferrochrome fine dust and filter cake by sinteri	
8.3.10 Chromium emission during the sinter process	
8.4 Conclusions	
Chapter 9 Stabilisation of Cr (VI) through sintering using silica-rich clay, Part Leaching behaviour of chromium from the stabilised wastes	
9.1 Introduction	137
9.2 Background	138
9.2.1 Leaching model based on initial wash-off or interface reaction kinetics	
9.2.2 Leaching model based on matrix diffusion	
9.2.3 Leaching model based on dissolution or corrosion	141

9.3 Experimental	143
9.3.1 Sample preparation	
9.3.2 Leaching test	
9.4 Results and discussion	144
9.4.1 Leaching mechanisms of chromium from the stabilised product	
9.4.2 Leaching mechanisms of Cr(VI) from the stabilised wastes	
9.5 Conclusions	151
Chapter 10 Summary and Conclusions	153
10.1 Summary	154
10.1.1 Stainless steel plant dust (SPD)	
10.1.2 Ferrochrome plant dust (FCD1, FCD2 and FCD3)	
10.1.3 Filter cake (FC)	
10.2 Conclusions	
10.3 Recommendations for future work	159
10.3.1 Modelling of the formation mechanisms of Cr (VI)	
10.3.2 Simultaneously treatment of stainless steel plant dust and pickling acid	
10.3.3 Properties of the bricks	160
References	161
Appendix I Cr (VI) and total chromium determination using spectrophotomete	r 179
Appendix II Thermal characteristics of clays	182
Appendix III Mass balance of the sintered brick	185
Appendix IV Calculations on the acceptable Cr (VI) concentration in the leach	ate
	188
Appendix V The production process of synthetic calcium chromate	190
Appendix VI Details of experiments on leaching behaviour of chromium from t	
stabilised wester	101

# **List of Figures**

Figure 1.1 Various waste minimisation techniques that can be used to manage the Cr	
(VI)-containing pyrometallurgical wastes [15]	3
Figure 2.1 Micrographs of electric furnace dust from a South African stainless steel plant	
(a) [39] and ferrochrome plant (b) [40]	
Figure 2.2 Formation mechanisms of dust in the EAF [23]	4
Figure 2.3 Formation mechanisms of fine droplets due to bubble bursting [24]	
Figure 2.4 The direct recycling process [70]	
Figure 2.5 The solidification process for treating EF dust with spent acid [115]	
Figure 2.6 Inorganic Recycling Corporation process in which electric furnace dust is	
treated [118]2	3
Figure 3.1 Schematic diagrams of dust treatment systems in the ferrochrome plant (a) and	
the stainless steel plant (b) from which the waste samples were taken	
Figure 3.2 The production process of filter cake in the stainless steel pickling waste	
treatment plant	8
Figure 3.3 The particle size distributions of the original FC, SPD, FCD1, 2 and 3 3	
Figure 3.4 XRD patterns of the EF dusts and filter cake	
Figure 3.5 Typical Raman spectrum obtained for the ferrochrome fine dust (FCD2) 3	
Figure 3.6 Absorbance FT-IR spectra of FCD1 and FCD2 (a), and synthetic basic zinc	Ī
sulphate hydrate (b)	6
Figure 3.7 The TG/DTA curves of the EF dusts and filter cake	
Figure 3.8 Backscatter electron image of the SPD after TG/DTA experiment 4	
(1-spinel; 2-glassy phase)	
Figure 3.9 SEM image of the TG/DTA residue (FCD2)	
Figure 3.10 The DTG curves for the ferrochrome fine dusts	
Figure 3.11 Surface elemental survey of the ferrochrome dust (a) and SPD (b)	
Figure 3.12 Mathematical curve fit of the Cr 2p <sub>3/2</sub> photoelectron peak for sample FCD24	
Figure 4.1 A nickel particle (SPD).	
Figure 4.2 A hollow spherical metal particle (SPD)	
Figure 4.3 A hollow slag particle (SPD)	
Figure 4.4 A spherical slag particle with cubic spinel crystals (SPD)	
Figure 4.5 A spherical particle with dendritically precipitated crystals (SPD)	
Figure 4.6 A spherical particle with precipitated CaCr <sub>2</sub> O <sub>4</sub> needles (SPD)	
Figure 4.7 A stainless steel droplet, coated with slag (SPD)	
Figure 4.8 Slag droplet with a rim of small particles (SPD)	
Figure 4.9 Backscattered electron image and X-ray map of a slag particle coated with a	
Fe-Zn-rich oxide layer (SPD)	2
Figure 4.10 The FCD2 ferrochrome dust sample: (a) Agglomerated fine dusts; (b)	
Backscattered electron image of the typical microstructure	2
Figure 4.11 Microstructure of the FCD3 ferrochromium EF dust. (A): Slag droplet, (B)	
carbon-bearing material; (C) chromite ore	
Figure 4.12 Spinel crystal in a sodium-rich silicate slag matrix (FCD3). [A=spinel crysta	
B=PAC; C=FeCr droplet]5	
Figure 4.13 PAC particle with a Mg <sub>2</sub> SiO <sub>4</sub> -based rim (FCD3). [A=Mg <sub>2</sub> SiO <sub>4</sub> rim;	
B=porous layer; C=FeCr droplets]	4
Figure 4.14 Typical SEM image of FC[A=Ca-S-F-O rich phase; B=Metal rich phase] 5	

Figure 4.15 An un-reacted lime particle in the FC
Figure 4.16 $\Delta G$ vs. temperature calculations for reactions that can contribute to dust
formation during ferrochromium production, using FACT Sage 5.1 56
Figure 4.17 XRD patterns of $Zn_4SO_4(OH)_6 \cdot 5H_2O$ and $NaZn_4(SO_4)Cl(OH)_6 \cdot 6H_2O$ 58
Figure 4.18 Secondary electron image and EDS spectrum of the synthetic crystals (a)
$Zn_4SO_4(OH)_6\cdot 5H_2O$ and (b) $NaZn_4(SO_4)Cl(OH)_6\cdot 6H_2O$
Figure 4.19 Dust formation mechanisms in semi-closed SAF
Figure 5.1 Leaching model of the toxic substances from the waste particles
Figure 5.2 The concentrations of toxic substances in TCLP test(a) and ASTM D3987-85
test(b)
Figure 5.3 XRD patterns of FCD 1,2 and 3 after DW and NA leach for 2 h70
Figure 5.4 XRD patterns of SPD before and after DW and NA leach for 2 h70
Figure 5.5 Effect of stirring speed on the leachability of Cr (VI) from SPD73
Figure 5.6 Effect of temperature on the leachability of Cr (VI) from SPD73
Figure 5.7 Effect of pH on the leachability of Cr (VI) from SPD74
Figure 5.8 The leachability of Cr (VI) from ferrochrome dust, using distilled water 75
Figure 5.9 The leachability of Cr (VI) from FC
Figure 5.10 Zinc concentration and pH in FCD2 leachate versus time (DW, 800rpm, 25°C
and S/L=1/20)77
Figure 6.1 Oxidation mechanism of Cr <sub>2</sub> O <sub>3</sub> by CaO in air [158]80
Figure 6.2 Experimental setup of the modified TCLP test
Figure 6.3 Effects of temperature and aging time on the leaching behaviour of Cr (VI). 83
Figure 6.4 Effect of particle size of the wastes on the Cr (VI) aging behaviour 85
Figure 6.5 Effect of atmosphere on the Cr (VI) aging behaviour
Figure 6.6 The oxidation of Cr <sub>2</sub> O <sub>3</sub> by CaO particles in air at 20°C (synthetic samples) 88
Figure 7.1 The furnace set-up
Figure 7.2 The particle size distribution of the clays
Figure 7.3 The crystalline phases present in the clays (Q-quartz, K-kaolinite, Mi-
Microcline, Mu-Muscovite, R-Rutile)97
Figure 7.4 The effect of temperature on the leachability of Cr (VI)
Figure 7.5 XRD Pattern of the sintered brick (1200°C, 5h, AS+CrO <sub>3</sub> ) (Q-quartz, M-
Mullite, C-Cristobalite, R-Rutile)
Figure 7.6 Typical microstructure and X-ray map of the sintered clay brick (1200°C and
5h) (1-Quartz, 2-Glassy phase (Si-Al-K-Fe), 3-Rutile)
Figure 7.7 Typical microstructure of the sintered clay brick (1200°C and 5h)(1-Quartz, 2-
Mullite+ silica, 3-(Al,Fe,Ti) <sub>3</sub> O <sub>5</sub> , 4-Glassy phase (Si-Al-K-Fe based)) 102
Figure 7.8 The effect of sintering time on the leachability of Cr (VI)
Figure 7.9 The effect of clays on the leachability of Cr (VI)
Figure 7.10 The effect of mass %CaO/ mass %SiO <sub>2</sub> on the leachability of Cr (VI) 105
Figure 7.11 The effect of initial Cr (VI) content on the leachability of the Cr (VI) 105
Figure 7.12 The effect of sinter atmosphere on the leachability of the Cr (VI) 106
Figure 7.13 Chromium emissions during the sintering experiments
Figure 8.1 The influence of different types of clays on the leachability of Cr (VI) 112
Figure 8.2 The influence of mass %CaO/mass %SiO <sub>2</sub> ratio on the leachability of Cr (VI)
from the stabilised wastes (SPD, 1100°C and 5 hours)

Figure 8.23 Chromium emission during the sinter process	. 134
Figure 9.1 Leaching mechanisms of toxic elements from the stabilised product [192]	. 138
Figure 9.2 The theoretical curves of the different leaching mechanisms [192]	. 142
Figure 9.3 Experimental set-up of the leaching test	. 144
Figure 9.4 Cumulative Cr(T) release and modelling results from the stabilised wastes	
(M1-50%SPD+50%AS; M2-50%SPD+50%MR; M3-20%FCD1+80%AS; M4-	
20%FCD2+80%AS and M5-20%FC+80%AS)	. 145
Figure 9.5 Logarithm of cumulative Cr (T) release vs. logarithm of leaching time	. 147
Figure 9.6 Cumulative Cr (VI) release from the solidified wastes (M1-50%SPD+50%	AS;
M2-50%SPD+50%MR; M3-20%FCD1+80%AS; M4-20%FCD2+80%AS and M	<b>1</b> 5-
20%FC+80%AS)	. 147
Figure 9.7 The logarithm of cumulative Cr (VI) release versus logarithm of leaching	time
of the stabilised wastes	. 150
Figure 9.8 The pH profile of the leachant vs. time during the leaching process	. 150
Figure 9.9 The solubility diagrams of chromium species calculated using STABCAL	
W32 at 25°C with a concentration of 10 <sup>-6</sup> M [181].	. 151

Figure 8.3 The Cr (VI) concentration in the modified TCLP leachate as a function of time
(spiked with 2mg/l Cr (VI) in leachate from 40% AS-60% SPD sample @ 1100°C for
5h)
Figure 8.4 The Eh-pH diagram for Cr species calculated using STABCAL with 10 <sup>-6</sup> mol/l
chromium concentration at 25°C [181]
Figure 8.5 The influence of sinter temperature on the leachability of Cr (VI)
Figure 8.6 Bricks (constituted of 50%clay/50%dust) sintered at different temperatures 117
Figure 8.7 The influence of the ratio of SPD in the brick on the leachability of Cr (VI)118
Figure 8.8 The influence of sinter time on the leachability of Cr (VI)
Figure 8.9 The XRD pattern of the sintered brick 50% AS-50% SPD at 1100°C for 5h (Q-
quartz; C-cristobalite; A-anorthite; H-hematite; Au-augite and S-spinel)
Figure 8.10 Microstructure of the 50% AS-50% SPD sintered brick (1-unmelted quartz; 2-
hematite and spinels; 3-anorthite and augite; 4-pores; 5-unreacted metal particles)
Figure 8.11 Microstructure of the 50% AS-50% SPD brick that was sintered at 1100°C for
5 h (1-spinel; 2-pore)
Figure 8.12 Columnar hematite crystals (1), spinels (2) and anorthite (3) in the 50% AS-
50%SPD brick sintered at 1100°C for 5 h
Figure 8.13 The X-ray map of the sintered brick (1100°C, 5h and 50%AS-50% SPD) (1-
Quartz; 2-Augite; 3- Glassy phase; 4- Anorthite; 5- Spinel; 6-Pore)
Figure 8.14 The microstructure of the sintered brick (1100°C, 5h and 50%AS-50% SPD)
(1-Quartz; 2-Augite; 3- Glassy phase; 4- Cr-rich spinel; 5-Anorthite; 5-Hematite; 6-
Fe-rich spinel)
± '
Figure 8.15 The influence of the initial Cr (VI) content on the leachability of Cr (VI). 125
Figure 8.16 XRD patterns of the stabilised SPD that was spiked with Cr(VI) and sintered
at 1100°C for 5h(Q-quartz; C-cristobalite; A-anorthite; H-hematite; Au-augite and
S-spinel)
Figure 8.17 The typical microstructure of the stabilized SPD that was spiked with Cr (VI)
and sintered at 1100°C for 5h [1-Cr <sub>2</sub> O <sub>3</sub> ; 2-spinel (Fe,Mn,Mg,Ni,Zn,Cr,Al) <sub>3</sub> O <sub>4</sub> ; 3-
glassy phase; 4-unreacted quartz; 5-Augite Ca(Mg,Fe)(Si,Al) <sub>2</sub> O <sub>6</sub> ; 6-Anorthite
$Ca(Al,Fe)_2Si_2O_8$ ; 7-Hematite (Fe,Cr,Mn) <sub>2</sub> O <sub>3</sub> ]
Figure 8.18 The typical microstructure of the stabilized SPD that was spiked with
1.55%CaCrO <sub>4</sub> and sintered at 1100°C for 5h [1-spinel (Fe,Mn,Mg,Ni,Zn,Cr,Al) <sub>3</sub> O <sub>4</sub> ;
2-glassy phase; 3-unreacted quartz; 4-Augite Ca(Mg,Fe)(Si,Al) <sub>2</sub> O <sub>6</sub> ; 5-Anorthite
$Ca(Al,Fe)_2Si_2O_8$ ; 6-Hematite $(Fe,Cr,Mn)_2O_3]$
Figure 8.19 The microstructure of the sintered SPD (1100°C, 5h and 100% SPD) (1-
Spinel; 2-Dicalcium silicate (2CaO·SiO <sub>2</sub> ); 3- Hematite; 4- Pore; 5-glassy phase). 130
Figure 8.20 The influence of mass %CaO/mass %SiO <sub>2</sub> ratio on the leachability of Cr(VI)
· ·
[5321mg Cr(VI)/kg mixture - 1 wt% CrO <sub>3</sub> and 1.55%CaCrO <sub>4</sub> , and 245.6mg/kg –
50%AS-50%SPD and CaO spiked 50%AS-50%SPD, 1100°C and 5 hours] 131
Figure 8.21 The influence of mass % $K_2O$ in the mixture on the leachability of $Cr(VI)$
[5321 mg Cr(VI)/kg mixture-1 wt% CrO <sub>3</sub> , 1.46 wt% K <sub>2</sub> CrO <sub>4</sub> and 1.92 wt% K <sub>2</sub> Cr <sub>2</sub> O <sub>7</sub> ,
and 245.6mg/kg–50%AS-50%SPD and 2.07wt%, 4.07wt% K <sub>2</sub> CO <sub>3</sub> spiked, 1100°C
and 5 h]
Figure 8.22 The leachability of Cr (VI) from the stabilised wastes (50%AS-50%FCD1,
FCD2 or FC) that were sintered at 1000°C for 5 hours

# **List of Tables**

Table 1.1 The maximum acceptable concentrations of Cr species, Zn and Pb in leacha	ıte
from the wastes specified by different countries [10-15]	2
Table 2.1 The regulation limits of Cr species for different water sources	6
specified by different countries [13,17,22]	
Table 2.2 Physical properties of electric furnace dust [2,4,6,9,12,14,17,38-51]	9
Table 2.3 Typical elemental compositions and crystalline phases present in the stainle	ess
steel plant dust and ferrochrome dust [2,4,6,9,14,17,38-58]	
Table 2.4 The typical compositions of the stainless steel pickling acid wastes [19]	12
Table 2.5 Electric furnace dust management methods [3,114]	20
Table 3.1 Physical properties of the EF dust and filter cake	
Table 3.2 Chemical analysis of the EF dusts and filter cake	32
Table 3.3 Surface element analysis of the dusts by XPS (atomic%)	44
Table 4.1 Parameters that possibly affect EF dust formation	62
Table 5.1 Experimental conditions of the Cr (VI) leaching tests	67
Table 5.2 XPS analysis of the EF dusts (atomic%)	
Table 6.1 Chemical analysis of different size fractions of SPD and FC	91
Table 6.2 Semi-quantitative XRD analysis of different size fractions of SPD and FC	91
Table 7.1 Experimental conditions	
Table 7.2 The chemical compositions of the clays (wt.%)	96
Table 7.3 Semi-quantitative XRD analysis	
Table 7.4 Typical EDS analysis of different phases (wt%)	
Table 7.5 Emission factors of chromium in various industries [177,178]	108
Table 8.1 The process parameters of the experiments	
Table 8.2 Concentrations of toxic substances in the modified TCLP leachates from the	
stabilised 50%AS-50%SPD mixture that was sintered at 1100°C for 5 hours	
Table 8.3 Typical EDS analyses of the phases present in the brick (50%AS-50%SPD,	
sintered at 1100°C for 5h) (mass%)	
Table 8.4 Calculated Cr (VI) leached ratios in the 50%AS-50%SPD mixture which w	ere
sintered at 1100°C for 5 hours and spiked with Cr (VI) species (%)	
Table 8.5 Typical EDS analyses of the phases present in the brick (100%SPD, sintere	d at
1100°C for 5h) (mass%)	
Table 8.6 Concentrations of selected elements in the leachates of the modified TCLP	tests
from the stabilised FCD1, FCD2 and FC (ppm)	
Table 9.1 Samples and experimental conditions	
Table 9.2 Controlling leaching mechanisms of total chromium from the stabilised was	
Table 9.3 Controlling leaching mechanisms of Cr (VI) from the stabilised wastes	148