

A soft condensed matter approach towards mathematical modelling of mass transport and swelling in food grains

M. Chapwanya^a, N.N. Misra^{b,*}

^a*Department of Mathematics & Applied Mathematics, University of Pretoria, Pretoria 0002, South Africa*

^b*School of Food Science & Environmental Health, Dublin Institute of Technology, Dublin 1, Ireland.*

Abstract

Soft condensed matter (SCM) physics has recently gained importance for a large class of engineering materials. The treatment of food materials from a soft matter perspective, however, is only at the surface and is gaining importance for understanding the complex phenomena and structure of foods. In this work, we present a theoretical treatment of navy beans from a SCM perspective to describe the hydration kinetics. We solve the transport equations within a porous matrix and employ the Flory-Huggin's equation for polymer-solvent mixture to balance the osmotic pressure. The swelling of the legume seed is modelled as a moving boundary with an explicit transient equation. The model exhibits a good agreement with the experimental observations and is capable of explaining the stages of hydration. Sensitivity analysis indicated that the degree of hydration is dependent on the bean size and is also sensitive to the selection of the intrinsic permeability of the bean.

Keywords: Soft Condensed Matter, Hydration, Swelling, Flory-Huggins, Mass Transfer, Navy Bean

1. Introduction

Soaking and hydration of legumes and cereals is an important unit operation in the grain processing industries. For example, legumes such as navy bean and kidney bean are often hydrated prior to canning operations. Hydration of beans decreases the cooking time, minimizes losses and improves the nutritional quality and protein digestibility of the cooked product (Wang et al, 1979; Abd El-Hady and Habiba, 2003). The problem of mass transfer during hydration of food grains has been treated both experimentally and theoretically, and in studies combining both approaches (Zanella-Díaz et al, 2014; Cozzolino et al, 2013; Ghafoor et al, 2014; Nicolin et al, 2012; Bello et al, 2010; Mohoric et al, 2004; Peleg, 1988; Hsu, 1983). Most of the mathematical descriptions reported in literature are either data driven regression models describing hydration kinetics or are based on simple fickian diffusion. Diffusion in many legumes (and cereals) cannot be described adequately by a simple

*Corresponding author

Email address: `misra.nrusimhanath@dit.ie` (N.N. Misra)

concentration dependent form of Fick’s diffusion equation, especially when these undergo swelling (or large deformation in geometry). Such conventional approaches fail to capture the finer details of food structure and their dynamics. Because of the complexity of food systems, interdisciplinary scientific approaches are needed to enable demanding developments (Ubbink and Mezzenga, 2006; Ubbink et al, 2008).

Soft matter physics focusing on description of an increasingly important class of materials that encompasses polymers, liquid crystals, complex fluids, organic-inorganic hybrids, foams, gels and the whole area of colloidal science is a contemporary area of research with several opportunities. Soft matter science plays an important role in a wide variety of processes and applications, examples of which include polymer swelling, phase separation, transport and delivery of drugs etc. The principles of soft matter physics are equally applicable to many food systems. Mezzenga et al (2005) reviewed the nature of foods from a perspective of soft condensed matter physics. The details of structural changes at various scales in food systems often needs experimental and/or theoretical tools of soft matter physics, which are not fully adapted to food systems (Mezzenga, 2007; Mezzenga et al, 2005). An exposition of the potential of soft matter physics for explaining the complex food processes and structuring at various scales is also provided in van der Sman and van der Goot (2009) and van der Sman (2012).

About 60 years ago, Flory and Huggins independently proposed the lattice model to treat the mixing enthalpy and entropy of polymers in a very straightforward way (Huggins, 1942a,b; Flory, 1953). Although many other models have been developed to describe the thermodynamics of polymer systems, the original Flory-Huggins lattice theory always give a very clear and straightforward physical picture (Han and Akcasu, 2011). However, it is worthwhile noting that the Flory-Huggins theory also is based on some assumptions that are often not valid. This includes the assumption that volume changes are not incurred upon mixing the polymer and solvent. It is also supposed that the polymer chain can be modelled on a lattice, which excludes contributions to the entropy from chain flexibility, and specific solvent-polymer interactions are ruled-out (Hamley, 2007). In an early work, van der Sman (2007) deduced an excellent modelling framework based on soft condensed matter perspective to explain the heat and mass transport during cooking of meat. This was based on the Flory-Rehner theory for pressure driven mass-transport in swelling or shrinking gels.

The model that we present in this paper is an attempt at advancing the basis of the theoretical modeling of mass transport during hydration of porous foods with a soft matter perspective. The model described herein shares an integrated approach between the statistical thermodynamics based Flory-Huggins theory and the continuum mechanics of fluid transport in porous media. We take an example case of hydration of navy bean, which is modelled as a saturated porous media undergoing large deformation by swelling. We are including a comparison of the simulation results with experimental data as model validation and an illustration of the model application, while also reporting on the sensitivity of the model to selected parameters. By means of the latter, we attempt to both analyse the influence of the natural variability in food properties on model predictions as well as gauge the sensitivity of the model to potential errors in parameter estimation.

2. Problem description

Figure 1, provides a summary of the geometric domain of the bean under consideration. The geometry of the navy bean can be described as a porous scalene ellipsoid, which is capable of undergoing global deformation. For the present study, we also assume that the pores are ideally filled with water which simplifies the problem to a saturated porous media case. We assume that the complex structural elements of navy bean, mainly proteins and carbohydrates can be approximated as ideal polymers. When applying principles of soft condensed matter physics to foods, it may be noted that polysaccharides and proteins are to foods what polymers are to soft condensed matter (Mezzenga et al, 2005). Notably, navy beans are by large chemically comprised of starch (50 - 60%), protein (20 - 38 %) and fibre ($\sim 18\%$) (Kereliuk and Kozub, 1995; Berg et al, 2012). This gives sufficient reason to justify our soft condensed matter analogy for navy beans. To formulate a feasible model, we also assume that the outer pericarp/skin is very thin and has no influence on the moisture transport.

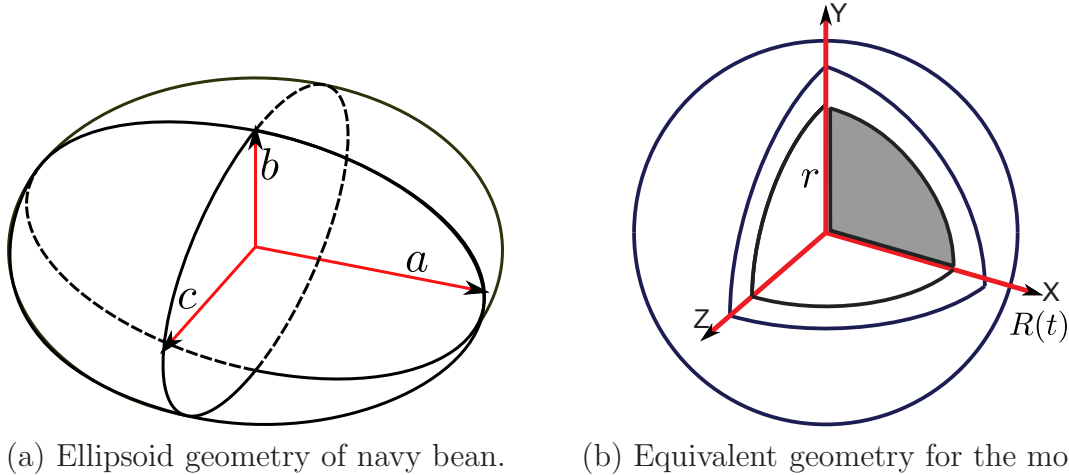


Figure 1: Schematic illustration of (a) the ellipsoid geometry of a navy bean grain and (b) the equivalent sphere concept with model boundaries.

We now simplify the problem geometry, by assuming that bean is spherical in shape and the swelling gives an evolving radius, $R(t)$ which varies with time, t . While assuming a spherical geometry for simplicity, we account for the deviations from the ellipsoid solid by calculating the radius of the sphere whose volume is equal to that of the scalene ellipsoid (Figure 1 (b)). The following equation was employed for calculating the equivalent radius, r [mm] (see Figure 1 (a) for notation)-

$$r = \left(\frac{G_m + S_m + A_m}{6} \right) \quad (1)$$

Herein, $G_m = 2(abc)^{\frac{1}{3}}$, $A_m = \left(\frac{2a + 2b + 2c}{3} \right)$, and $S_m = \left(\frac{4ab + 4bc + 4ca}{3} \right)^{\frac{1}{3}}$ are the geometric mean diameter, arithmetic mean diameter, and square mean diameter, respectively.

tively (Mohsenin, 1986). In accordance with Ghafoor et al (2014), we take the temperature to be constant (16 °C) throughout the duration of soaking and therefore, temperatures capable of causing gelatinisation are not encountered. Finally, we define the volume fraction of the solids in the bean to be ϕ , and to satisfy the criteria of saturation, we have $(1 - \phi)$ as the volume fraction of the liquid water.

3. Mathematical model

In this section a mathematical model based on the Flory-Huggins theory for hydration of Navy bean is presented. Part of the modeling approach has been presented elsewhere in the literature in the context of biofilms (Winstanley et al, 2011). For completeness, we summarize the equations here. Mass conservation of the polymer is given by

$$(\rho_s \phi)_t + \nabla \cdot [\rho_s \phi \mathbf{v}] = 0, \quad (2)$$

where ρ_s [Kg m⁻³] is the averaged phase density and \mathbf{v} [ms⁻¹] is the protein velocity. Similarly, conservation of the liquid is given by

$$(\rho[1 - \phi])_t + \nabla \cdot [\rho(1 - \phi) \mathbf{w}] = 0, \quad (3)$$

where ρ [Kg m⁻³] is the averaged water density and \mathbf{w} [ms⁻¹] is the water velocity.

The bean is assumed to be a porous structure, hence the momentum equations as given by Darcy's law holds. We relate the liquid velocity to the liquid pressure, p [Pa], via

$$-(1 - \phi) \nabla p + \frac{\mu(1 - \phi)^2}{k} (\mathbf{v} - \mathbf{w}) = 0, \quad (4)$$

where μ is the water viscosity, k is the grain permeability. By analogy with (4), the momentum equation for the polymer takes the form

$$-\phi \nabla p_s - \frac{\mu(1 - \phi)^2}{k} (\mathbf{v} - \mathbf{w}) = 0, \quad (5)$$

where p_s [Pa], is the pressure of the polymer. Note that our approach in dropping the viscous stress for equations (8) and (9) is consistent with the the work of Winstanley et al (2011), where the viscous stress was observed to be negligible compared to osmotic stress and pressure. The interaction pressure, which is the pressure difference between the polymer pressure and the water pressure, is given by

$$p_s - p = \psi(\phi).$$

Note that, a polymer in contact with water will swell (or shrink) to equilibrate the total osmotic pressure - and swelling (in the current context) will give rise to changes in ϕ . It has been recognised that the balance equations can be generalized to have a proper coupling to thermodynamics, so that they have the correct driving forces for the transport phenomena (van der Sman, 2012). Keeping this in mind, as will be shown next, here we adopt the

Flory-Huggins theory to relate the osmotic pressure to the polymer volume fraction, i.e., $\psi = \psi(\phi)$. At this point it may be noted that the processes of diffusion and diffusivity are fundamentally different in nature, although they are formally described by the same type of mathematics.

We now manifest the Flory-Huggins free energy per unit volume, as the osmotic pressure term (see c.f. Hill (1987)), which is the additional pressure that is required to equilibrate the solid (polymer) volume fraction with pure water. This is given by-

$$\psi = -\frac{RT}{V} \left[\ln(1 - \phi) + \left(1 - \frac{1}{n}\right) \phi + \chi\phi^2 \right] \quad (6)$$

where n is the ratio of molar volumes of solute (protein) and solvent (water), χ is the interaction parameter between the polymer and the solvent (water), R [$\text{J mol}^{-1} \text{K}^{-1}$] is the gas constant, T [K] is the temperature and V [$\text{m}^3 \text{mol}^{-1}$] is the molar volume of water. The underpinning principles of the theory are backed up by strong thermodynamic basis and the lattice theory, a good discussion of which can be found in Hill (1987). From a thermodynamic viewpoint, the parameter χ is a measure of the interaction enthalpy per solvent (water) molecule. Proceeding further, if n is sufficiently large ($n \rightarrow \infty$), which is a valid assumption for the case of most foods, including navy bean, equation (6) can be simplified to

$$\psi = -\frac{RT}{V} [\ln(1 - \phi) + \phi + \chi\phi^2]. \quad (7)$$

3.1. Model summary

Assuming incompressibility, we summarize the equations as follows

$$-f\phi(1 - \phi)(\mathbf{v} - \mathbf{w}) - \phi\nabla\psi - \phi\nabla p = 0, \quad (8)$$

$$f\phi(1 - \phi)(\mathbf{v} - \mathbf{w}) - (1 - \phi)\nabla p = 0, \quad (9)$$

$$\phi_t + \nabla \cdot [\phi\mathbf{v}] = 0, \quad (10)$$

$$-\phi_t + \nabla \cdot [(1 - \phi)\mathbf{w}] = 0, \quad (11)$$

$$\psi = -\frac{RT}{V} [\ln(1 - \phi) + \phi + \chi\phi^2], \quad (12)$$

where $f = \frac{\mu(1 - \phi)}{k\phi}$ [Pa s m^{-2}] is the interfacial drag term. The model above incorporates the momentum balance (Darcy's law) for each phase (equations (8) and (9)), the osmotic pressure equation (Flory-Huggins equation (12)) relating the chemical potential of the solvent (water) the solute (polymer), and mass conservation for each phase (equations (10) and (11)).

The swelling/shrinking pressure is proportional to $-\nabla\psi = -\psi'(\phi)\nabla\phi$ where

$$\psi'(\phi) = \frac{RT}{V} \frac{2\phi^2}{1 - \phi} \left[\left(\chi - \frac{1}{2} \right) - \chi\phi \right].$$

Here we consider $\psi' > 0$ where a polymer in contact with a solvent will swell. We note that for $\phi \in [0, 1]$, there is a minimum at $\phi^* = (\chi - \frac{1}{2})/\chi$ with $\chi > \frac{1}{2}$, as can be observed in Fig. 2. The above relation can therefore be used for tracking the equilibrium moisture interface over a moving boundary.

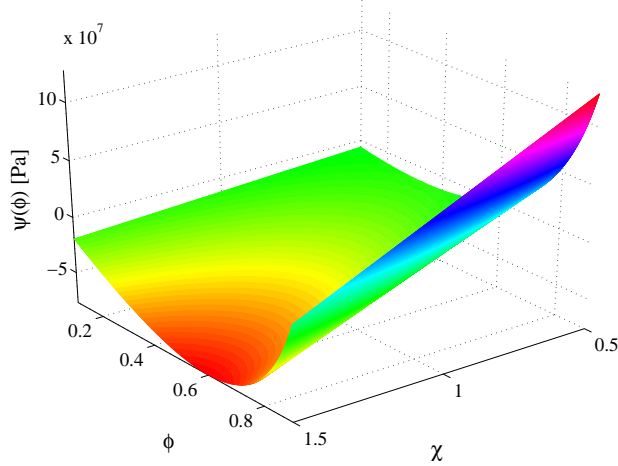


Figure 2: An illustration of the relationship between osmotic pressure and polymer fraction.

After some algebraic simplification, the system of equations (8) – (12) can be reduced to

$$\phi_t = \nabla \cdot [(1 - \phi)\mathbf{w}], \quad (13)$$

$$\mathbf{w} = \frac{\phi}{f(\phi)} \psi'(\phi) \nabla \phi, \quad (14)$$

$$\psi = -\frac{RT}{V} [\ln(1 - \phi) + \phi + \chi\phi^2]. \quad (15)$$

Assuming one dimensional spherical coordinate system, then $\phi(r, t)$ is shown to be governed by the Fick's second Law of diffusion

$$\frac{\partial \phi}{\partial t} = \frac{1}{r^2} \frac{\partial}{\partial r} \left[r^2 D(\phi) \frac{\partial \phi}{\partial r} \right], \quad (16)$$

where the moisture diffusivity term is given by

$$D(\phi) = D_0 \frac{2\phi^3}{1 - \phi} \left[\chi\phi - \left(\chi - \frac{1}{2} \right) \right], \quad (17)$$

and $D_0 = \frac{RTk}{\mu V}$. We now require that $\chi\phi - (\chi - \frac{1}{2}) > 0$ or $\phi^* < \phi < \phi_e$. The Flory's interaction parameter, χ in this range corresponds to approx. [0.5-1.5], which also complies with the values reported in [Jin et al \(2014\)](#). This will be used later to motivate the choice of boundary condition at the interface between free water and the porous structure. This constrain also arises from the peculiar nature of χ as the parameter dictating the phase

separations in polymer-solvent systems, a comment on which is appropriate. The critical value of χ (denoted as χ_c) for miscibility of a polymer in a solvent is approximately 0.5. For values of χ less than 0.5 the polymer will be soluble in the solvent and loss of solids (leaching) will occur. However, the analogous polymer-solvent theory for navy bean assuming no loss of solids (solute) requires that the biopolymer matrix be insoluble in the water, i.e. a poor solvent behaviour. Therefore, our assumption of $\chi > \frac{1}{2}$ is physically valid, for only with this constrain the polymer will not be soluble in the solvent (Flory, 1953; Hill, 1987).

It is worth noting the similarities between the derived model and the literature; see for example Bello et al (2010); Davey et al (2002); Weinstein and Bennethum (2006); Nicolin et al (2012). In particular, Davey et al (2002) derived a nonlinear diffusion equation governing the swelling of a cereal grain. However, the model here deviates from Davey et al (2002) in the choice of the diffusivity function. While their choice is motivated by an empirical exponential function, here the function comes naturally from the Flory-Huggins theory. A model based on thermodynamics arguments and Flory-Huggins theory was also presented by Weinstein and Bennethum (2006). The resulting nonlinear diffusion equation can be reduced to the model derived here with the condition that $\chi = 0$ and an appropriate choice of the permeability function. However, as we have observed earlier, the limit $\chi = 0$ does not make any physical sense.

From a mathematical point of view, the presented model is a moving boundary problem and requires an extra condition for the location of the boundary $r = R(t)$. As the water is absorbed, the grain swells and there is a change of mass inside the grain. From here forthwith, we define $\phi = 1 - \theta$, so that θ defines the volume fraction of water and $1 - \theta$ the volume fraction of the polymer. Using the new variable we have

$$\frac{\partial \theta}{\partial t} = \frac{1}{r^2} \frac{\partial}{\partial r} \left[r^2 D(\theta) \frac{\partial \theta}{\partial r} \right], \quad (18)$$

$$D(\theta) = D_0 \frac{2(1-\theta)^3}{\theta} \left[\chi(1-\theta) - \left(\chi - \frac{1}{2} \right) \right], \quad (19)$$

with $\theta > 0$. Integrating (18) on $r \in [0, R(t)]$ and on application of Leibniz rule, we have

$$R^2 \frac{dR}{dt} = \frac{D(\theta_e) R^2}{1 - \theta_e} \frac{\partial \theta}{\partial r} \Big|_{r=R(t)} + \frac{1}{1 - \theta_e} \frac{d}{dt} \left[\int_0^{R(t)} (1 - \theta) r^2 dr \right], \quad (20)$$

where we have used symmetry and the fact that $\theta_r = 0$ on $r = 0$. The middle term gives the flux of water through the grain and the last term gives the dissolution rate. Here there is no loss of solid during hydration, hence we set

$$\frac{d}{dt} \left[\int_0^{R(t)} (1 - \theta) r^2 dr \right] = 0, \quad (21)$$

so that the moving boundary is described by

$$\frac{dR}{dt} = \frac{D(\theta_e)}{1 - \theta_e} \frac{\partial \theta}{\partial r} \Big|_{r=R(t)}. \quad (22)$$

3.2. Boundary Conditions

As initial condition, we know that $\theta(r, 0) = \theta_0$ under the assumption that the moisture distribution inside the bean is isotropic. We now specify the boundary conditions as follows

$$\frac{\partial \theta}{\partial r} = 0, \quad \text{on } r = 0, \quad (23)$$

$$\theta = \theta_e, \quad \text{on } r = R(t). \quad (24)$$

The volume averaged moisture content at each time step, t [s] is calculated from equation (25), as given by Ruiz et al (2008),

$$M(t) = \frac{3}{R(t)^3} \int_0^{R(t)} R(t)^2 \theta(R, t) dr, \quad (25)$$

where $R(t)$ is the radius at time t [s]. For validation of the model, we employ the experimental results from a previous work Ghafoor et al (2014) and set all parameters as per Table 1, unless otherwise explicitly stated. The moisture content on dry basis given in Ghafoor et al (2014) was transformed into volume fraction of water, $\theta(r, t)$, using the following relation

$$M = \frac{\rho \theta}{\rho_s (1 - \theta)}, \quad (26)$$

where, as defined before, ρ and ρ_s are the density of water and the solid respectively.

Table 1: Typical values of the parameters employed for the simulations and model validation.

Symbol	Definition	Value		Source
θ_0	Initial water fraction	0.12		Ghafoor et al (2014)
θ_e	Equilibrium water fraction	0.60		Ghafoor et al (2014)
T	Temperature	289.15	K	Ghafoor et al (2014)
ℓ	Navy bean initial radius	0.003	m	Ghafoor et al (2014)
ρ_s	Polymer matrix density	1376	kg/m ³	Bellido et al (2003)
ρ	Density of water	999.1	kg/m ³	
μ	Viscosity of water	1.109×10^{-3}	Pa s	
k	Permeability	3.1×10^{-21} (approx.)	m ²	Warning et al (2014)
χ	Interaction parameter	0.51		Jin et al (2014)
R	Gas constant	8.314	J/mol/K	
V	Molar volume of water	18.02×10^{-6}	m ³ /mol	
D_0	$RTk/\mu V$	4.81×10^{-10}	m ² /s	

4. Nondimensionalisation

We introduce the following scales

$$r \sim \ell, \quad s \sim \ell, \quad R \sim \ell, \quad D \sim D_0, \quad t \sim \frac{\ell^2}{D_0}, \quad (27)$$

where ℓ is the initial bean radius. The advantage of this process is that we now have to solve the model on $[0, R(t)]$ with $R(t) \geq 1$. In dimensionless form, we consider

$$\frac{\partial \theta}{\partial t} = \frac{1}{r^2} \frac{\partial}{\partial r} \left[r^2 D(\theta) \frac{\partial \theta}{\partial r} \right], \quad \forall (r, t) \in (0, R(t)) \times (0, \infty), \quad (28)$$

$$\theta(r, 0) = \theta_0, \quad (29)$$

subject to

$$\frac{\partial \theta}{\partial r}(0, t) = 0, \quad (30)$$

$$\theta(R, t) = \theta_e, \quad \text{and} \quad \frac{dR}{dt} = \frac{D(\theta_e)}{1 - \theta_e} \frac{\partial \theta}{\partial r} \Big|_{r=R(t)}, \quad (31)$$

where

$$D(\theta) = \frac{2(1 - \theta)^3}{\theta} \left[\chi(1 - \theta) - \left(\chi - \frac{1}{2} \right) \right]. \quad (32)$$

While some mathematical insight can be obtained from an equivalent two moving boundary problem as in [Davey et al \(2002\)](#), here no analytical approximation is possible. Hence we proceed to solve the problem numerically.

5. Numerical simulations and model validation

The model is discretized in space using finite volume approach on the domain $[0, R(t)]$ with N uniform grid cells of width $\Delta r = R(t)/N$ with cell centers $r_{i \pm \frac{1}{2}} = r_i \pm \frac{\Delta r}{2}$ for $i = 1, 2, \dots, N$. Using the notation consistent with the finite volume literature, we have the scheme

$$\frac{\partial \theta_i}{\partial t} = \frac{1}{r_i^2 \Delta r} \left[r_{i+1/2}^2 D_{i+1/2} \frac{\theta_{i+1} - \theta_i}{\Delta r} - r_{i-1/2}^2 D_{i-1/2} \frac{\theta_i - \theta_{i-1}}{\Delta r} \right]. \quad (33)$$

for equation (28), and

$$\frac{dR}{dt} = \frac{D(\theta_e)}{1 - \theta_e} \frac{\theta_{i+1/2} - \theta_{i-1/2}}{\Delta r} \Big|_{r_i=R(t)} \quad (34)$$

for the moving boundary (31). The same approach is used for the boundary conditions and the resulting scheme is second order in space. The solution code scripted in MATLAB (The MathWorks, MA, USA) was run on a 3.0 GHz Intel Core i7 processor. The system of nonlinear ODEs are integrated with Matlab's standard stiff solver ODE15s, with a relative tolerance values of 1×10^{-12} . The resolution algorithm of ODE15s is based on the numerical

differentiation formula method (improved version of the implicit Backward Differentiation Formula (BDF) method). For all the simulations presented in this paper, we used $N = 201$ and we found no influence on the results upon rerunning the simulations with increased number of nodes.

For evaluating the accuracy of the models, we employ the statistical criterion of the Root Mean Squared Error (RMSE) given by equation (35)

$$RMSE = \sqrt{\frac{\sum_{i=1}^{n_t} (\theta_e - \theta_p)^2}{n_t}} \quad (35)$$

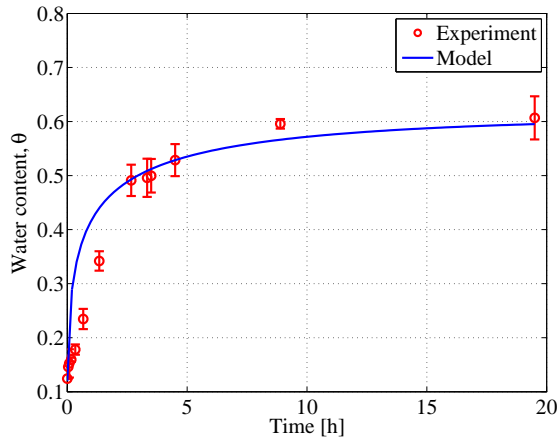
where θ_e denotes the experimental observations, θ_p the predicted values and n_t the total number of data points.

5.1. Base case simulations

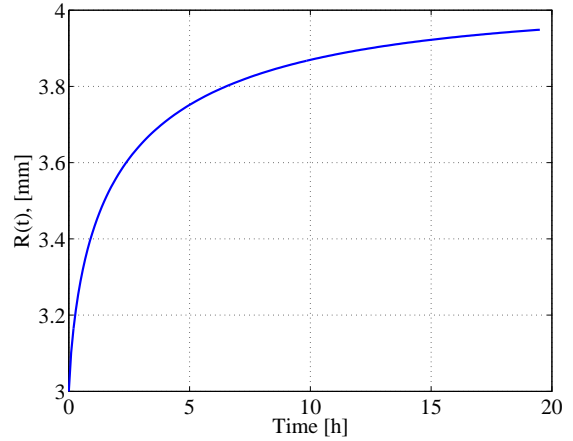
We now compare our results with the experimental data reported by [Ghafoor et al \(2014\)](#), who studied the hydration of navy beans in water at 16 °C. Figure 3 (a) provides a comparison of the model predictions and the experimental data. The model clearly provides a good prediction of the hydration kinetics, within a reasonably small error as observed from the RMSE value of 0.081. At the beginning of the water absorption process, the relative mass of water absorbed by the bean cotyledon strongly increased with the hydration time and then saturated. The exponential behaviour indicates that the water absorption is caused by the gradient of the matrix potential between the dry cotyledon structure and the water environment ([Golonka et al, 2002](#)). The volume fraction of the liquid representing the moisture content tends to approximately a value of 0.6 after 15 h of soaking. In addition, we note that the radius of the representative bean follows a similar trend and swells to a maximum radii of ~ 3.9 mm, which is in excellent agreement with the experimental value of 3.92 mm. We wish to highlight that unlike, the work of [Bakalis et al \(2009\)](#) and [Hsu \(1983\)](#) who employ experimental observations and empirical equations respectively for the bean swelling, our approach accurately predicts the radii as a function of the instantaneous moisture. The deviation from the experimental values during the initial phase of hydration can be ascribed to our ignorance of resistance offered by the seed coat. This fact is experimentally demonstrated elsewhere in the context of soybean hydration ([Meyer et al, 2006](#)).

5.2. Degree of hydration

An earlier work on cooking of grains focused on the degree of gelatinisation of a rice kernel and the significant feature of this model was the presence of two moving boundaries. One describing the change in grain size and the second boundary described the gelatinisation front ([Davey et al, 2002](#)). Mathematically, these represent a class of Stefan's problem where no phase change is involved (see, for example [Barry and Counce \(2008\)](#)). Since cooking temperatures leading to gelatinisation are never encountered for simple hydration, we are left



(a) Water content.



(b) Moving boundary.

Figure 3: Profiles for water content and the radius of the bean with time.

with one moving boundary for the radius and a transient species diffusion. Equivalently, here we implicitly locate the degree of hydration by tracking the front where the moisture content is θ_w . This approach is more physically representative since we are effectively allowing moisture variations beyond the wetting front. We present these relations via a contour plot in Figure 4. The rapid hydration in the initial phase can be ascribed to the creation of free volumes inside the grains, while the slow water uptake in later phases is an outcome of the rearrangement of structural elements. Direct experimental observations using Positron Annihilation Spectroscopy (PAS) and proton Nuclear Magnetic Relaxation (NMR) reported earlier also support our hypothesis and explanation (Golonka et al, 2002). Golonka et al (2002) reported that the hydration of the cotyledon structure evokes reduction of the surface and interior tension, and loosens structure of the bean samples. When the hydration reaches the slower phase, a rearrangement of the cotyledon microstructure occurs and the number and dimensions of the free volume regions does not change significantly.

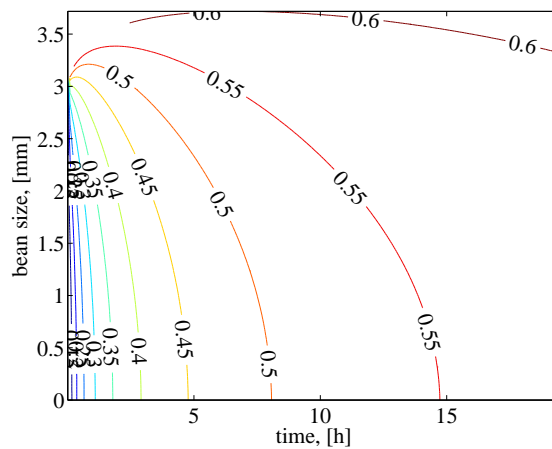


Figure 4: The isolines represent the degree of hydration of the grain at a given time.

5.3. Sensitivity to bean dimensions

Experimental measurement of the initial bean dimensions of several beans and the average values a , b and c were in the range 8.9 ± 0.39 mm, 5.04 ± 0.15 mm and 5.9 ± 0.28 mm respectively, see [Ghafoor et al \(2014\)](#). The bean dimensions after a 19 h soaking duration were found to be in the range 12.94 ± 0.47 mm, 6.32 ± 0.31 mm and 7.54 ± 0.21 mm respectively. These values corresponded to an initial and final radii of the equivalent sphere in the range 3 mm and 4 mm respectively. Differences in bean dimensions affect the degree of hydration, especially for shorter hydration times, which nevertheless, is overcome with standard overnight soaking practice. We performed sensitivity analysis for the degree of hydration to bean dimensions in the range 2.5 to 4.0 mm. The results are summarised in Figure 5. Firstly, we note that beans with higher initial radii swell to higher degree and this was also observed during the experiments ([Ghafoor et al, 2014](#)). Next, the moisture equilibration takes more time for larger beans. However, longer soaking times allow to reach near equilibrium moisture distribution.

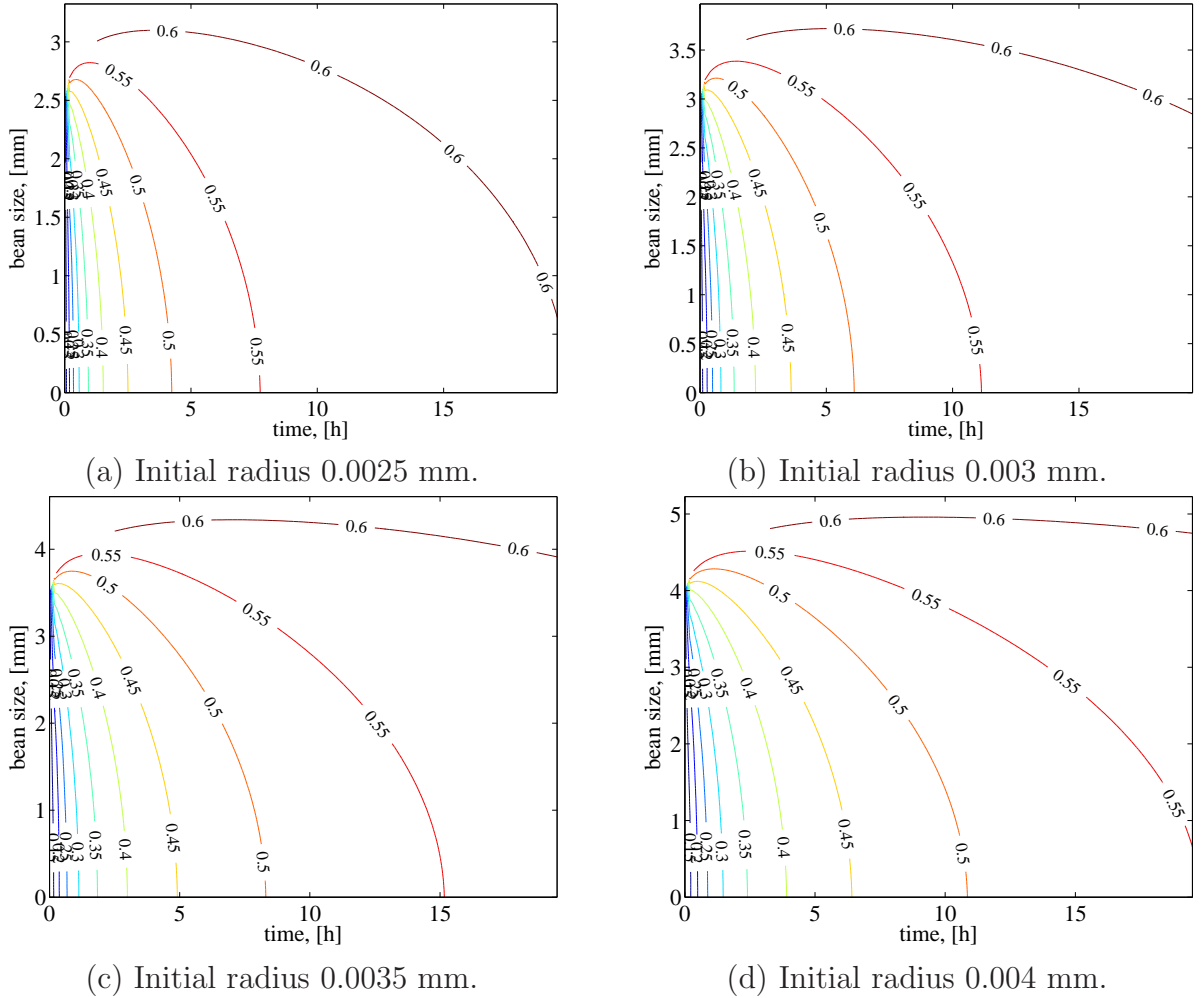


Figure 5: Profiles for the bean radius for different initial bean radii taken in the range [2.5 – 4.0] mm.

5.4. Sensitivity to medium permeability

When considering the moisture diffusion in a single bean, the porosity, pore network size and distribution largely define the rate of hydration. Since we chose porosity as a macroscopic variable in our model, the above factors are ruled by the intrinsic permeability in this framework. Datta (2006) highlighted that when physics based mechanistic models involving pressure driven flow are employed with a clear definition of the individual modes of transport processes, the selection of permeability data becomes important. Considering that we did not find experimentally measured permeability data for navy beans, we approximated the intrinsic permeability from that of parboiled rice grains and those reported for other inert materials (Warning et al, 2014; Datta, 2006). The permeability for heat treated parboiled rice grain was recently reported to be in the order of 10^{-20} m² using Lattice-Boltzmann simulations. As rice grain hydrates to more than double its volume whereas navy bean to approximately 1.2 times the original volume, we take values in the order of 10^{-21} m². To gauge the sensitivity of the model to permeability value we performed sensitivity analysis in the range $[1.1 - 5.1] \times 10^{-21}$ m². The sensitivity of the moisture content of the bean is presented in Figure 6. It can be observed that the evolution of water saturated pore fraction is directly related to the intrinsic permeability. This indicates the strong coupling between the momentum transport and structure evolution in our model. The model was thus found to be highly sensitive to the selection of permeability values, where a higher permeability indicted a faster rate of hydration. It is worth noting that a non-linearly evolving permeability will allow far more accurate predictions than a constant value. This is true considering that the porosity of the bean evolves with time. A direct method for applying the model could be based on the microstructure geometry, similar to that described by Nicolaí and group in their recent work using micro- computed tomography method for fruits (Cantre et al, 2014; Herremans et al, 2014). Conversely, our analysis can also be transformed to an inverse problem scenario to compute the effective water permeability.

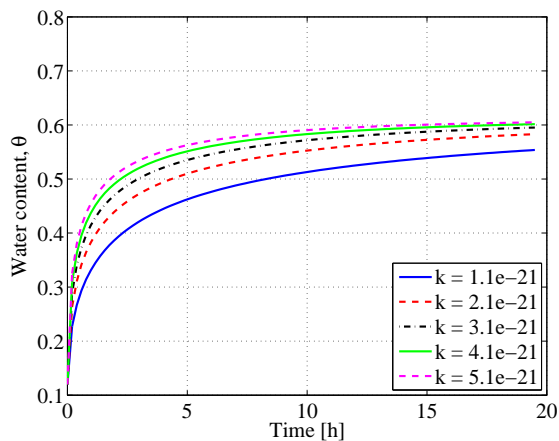


Figure 6: Profiles for the water content for different permeability values taken in the range $[1.1 - 5.1] \times 10^{-21}$ m².

6. Conclusions

The SCM model demonstrated good predictive capabilities for moisture transport and swelling of the navy beans, without losing the elegance of internal porodynamics. The moving boundary equation accurately predicted the final radii of the bean and supported the rapid creation of free volume inside the bean during rapid hydration phase, followed by structural rearrangements observed in experiments. The model was found sensitive to the selection of the permeability value and modelling on accurate physical domain is highly encouraged. The model presented here is a proof of concept of how hydration of foods can be described by using principles of soft condensed matter physics.

To impart an illustrative value, we simplified the model with some assumptions, so that the theory could be easily discussed. Although we demonstrated the applicability of the model with spherical equivalence and radial profile simulations, the extension of this model to foods with complex geometry should be quite straightforward, using finite volume or finite element methods with moving mesh or phase-field and level set approaches using commercial softwares such as COMSOL Multiphysics. This is now practical since significant microstructural details are becoming available with newer imaging techniques such as X-ray micro-computed tomography. The model can be elaborated for cooking of food grains by incorporating the Fourier equation. As a limitation of the current single grain modeling approach, we wish to highlight that diffusion in a single particle is different physically from diffusion through a porous particle layer. Thus, to simulate realistic conditions, the problem turns out to be a two-phase, multiscale, saturated porous media problem. This will be dealt with in our future work.

References

- Abd El-Hady E, Habiba R (2003) Effect of soaking and extrusion conditions on antinutrients and protein digestibility of legume seeds. *LWT - Food Science and Technology* 36:285–293, DOI 10.1016/s0023-6438(02)00217-7
- Bakalis S, Kyritsi A, Karathanos VT, Yanniotis S (2009) Modeling of rice hydration using finite elements. *Journal of Food Engineering* 94:321 – 325, DOI 10.1016/j.jfoodeng.2009.03.023
- Barry SI, Caunce J (2008) Exact and numerical solutions to a stefan problem with two moving boundaries. *Applied Mathematical Modelling* 32:83–98, DOI 10.1016/j.apm.2006.11.004
- Bellido G, Arntfield S, Scanlon M, Cenkowski S (2003) The effect of micronization operational conditions on the physicochemical properties of navy beans (*Phaseolus vulgaris* L.). *Journal of Food Science* 68:1731–1735, DOI 10.1111/j.1365-2621.2003.tb12320.x
- Bello M, Tolaba M, Aguerre R, Suarez C (2010) Modeling water uptake in a cereal grain during soaking. *Journal of Food Engineering* 97:95–100, DOI 10.1016/j.jfoodeng.2009.09.020
- Berg T, Singh J, Hardacre A, Boland MJ (2012) The role of cotyledon cell structure during in vitro digestion of starch in navy beans. *Carbohydrate Polymers* 87:1678 – 1688, DOI 10.1016/j.carbpol.2011.09.075
- Cantre D, East A, Verboven P, Trejo Araya X, Herremans E, Nicolaí BM, Pranamornkith T, Loh M, Mowat A, Heyes J (2014) Microstructural characterisation of commercial kiwifruit cultivars using x-ray micro computed tomography. *Postharvest Biology and Technology* 92:79–86, DOI 10.1016/j.postharvbio.2014.01.012
- Cozzolino D, Roumeliotis S, Eglinton J (2013) Monitoring water uptake in whole barley (*Hordeum vulgare* L.) grain during steeping using near infrared reflectance spectroscopy. *Journal of Food Engineering* 114:545–549, DOI 10.1016/j.jfoodeng.2012.09.010

- Datta A (2006) Hydraulic permeability of food tissues. *International Journal of Food Properties* 9:767–780, DOI 10.1080/10942910600596167
- Davey M, Landman K, McGuinness M, Jin H (2002) Mathematical modeling of rice cooking and dissolution in beer production. *AIChE Journal* 48(8):1811–1826
- Flory PJ (1953) *Principles of Polymer Chemistry*. Cornell University Press
- Ghafoor M, Misra N, Mahadevan K, Tiwari B (2014) Ultrasound assisted hydration of navy beans (*Phaseolus vulgaris*). *Ultrasonics Sonochemistry* 21:409–414, DOI 10.1016/j.ultsonch.2013.05.016
- Golonka P, Dryzek J, Kluza M (2002) Bean cotyledons microporosity under hydration conditions. *Nukleonika* 47:137–140
- Hamley IW (2007) *Polymers*, Wiley, chap 2, pp 39–106
- Han CC, Akcasu ZA (2011) *Dynamics and Kinetics of Phase Separation in Polymer Systems*, John Wiley & Sons, chap 3, pp 103–209. DOI 10.1002/9780470824849.ch3
- Herremans E, Verboven P, Defraeye T, Rogge S, Ho QT, Hertog ML, Verlinden BE, Bongaers E, Wevers M, Nicolai BM (2014) X-ray CT for quantitative food microstructure engineering: The apple case. *Nuclear Instruments and Methods in Physics Research Section B: Beam Interactions with Materials and Atoms* 324:88–94, DOI 10.1016/j.nimb.2013.07.035
- Hill TL (1987) *Polymer and polyelectrolyte solutions and gels*, Dover Publications, chap 21, pp 398–423
- Hsu KH (1983) A diffusion model with a concentration-dependent diffusion coefficient for describing water movement in legumes during soaking. *Journal of Food Science* 48:618–622, DOI 10.1111/j.1365-2621.1983.tb10803.x
- Huggins ML (1942a) Some properties of solutions of long-chain compounds. *The Journal of Physical Chemistry* 46:151–158, DOI 10.1021/j150415a018
- Huggins ML (1942b) Theory of solutions of high polymers. *Journal of the American Chemical Society* 64:1712–1719, DOI 10.1021/ja01259a068
- Jin X, van der Sman RGM, Maanen JFC, Deventer HC, Straten G, Boom RM, Boxtel AJB (2014) Moisture sorption isotherms of broccoli interpreted with the flory-huggins free volume theory. *Food Biophysics* 9:1–9, DOI 10.1007/s11483-013-9311-6
- Kereliuk G, Kozub G (1995) Chemical composition of small white (navy) beans. *LWT - Food Science and Technology* 28:272–278, DOI 10.1016/s0023-6438(95)94176-2
- Meyer CJ, Steudle E, Peterson CA (2006) Patterns and kinetics of water uptake by soybean seeds. *Journal of Experimental Botany* 58:717–732, DOI 10.1093/jxb/er1244
- Mezzenga R (2007) Equilibrium and non-equilibrium structures in complex food systems. *Food Hydrocolloids* 21:674–682, DOI 10.1016/j.foodhyd.2006.08.019
- Mezzenga R, Schurtenberger P, Burbidge A, Michel M (2005) Understanding foods as soft materials. *Nature Materials* 4:729–740, DOI 10.1038/nmat1496
- Mohoric A, Vergeldt F, Gerkema E, de Jager A, van Duynhoven J, van Dalen G, Van As H (2004) Magnetic resonance imaging of single rice kernels during cooking. *Journal of Magnetic Resonance* 171:157–162, DOI 10.1016/j.jmr.2004.08.013
- Mohsenin NN (1986) *Physical Properties of Plant and Animal Materials*. Routledge
- Nicolin D, Coutinho M, Andrade CM, Jorge L (2012) Hsu model analysis considering grain volume variation during soybean hydration. *Journal of Food Engineering* 111:496–504, DOI 10.1016/j.jfoodeng.2012.02.035
- Peleg M (1988) An empirical model for the description of moisture sorption curves. *Journal of Food Science* 53:1216–1217, DOI 10.1111/j.1365-2621.1988.tb13565.x
- Ruiz RS, Vizcarra MG, Martínez C (2008) Hydration of grain kernels and its effect on drying. *LWT - Food Science and Technology* 41:1310–1316, DOI 10.1016/j.lwt.2007.08.007
- van der Sman R (2012) Soft matter approaches to food structuring. *Advances in Colloid and Interface Science* 176-177:18–30, DOI 10.1016/j.cis.2012.04.002
- van der Sman RGM (2007) Soft condensed matter perspective on moisture transport in cooking meat. *AIChE Journal* 53:2986–2995, DOI 10.1002/aic.11323
- van der Sman RGM, van der Goot AJ (2009) The science of food structuring. *Soft Matter* 5:501, DOI 10.1039/b718952b

- Ubbink J, Mezzenga R (2006) Delivery of functionality in complex food systems: introduction. *Trends in Food Science & Technology* 17:194–195, DOI 10.1016/j.tifs.2006.01.004
- Ubbink J, Burbidge A, Mezzenga R (2008) Food structure and functionality: a soft matter perspective. *Soft Matter* 4:1569, DOI 10.1039/b802183j
- Wang H, Swain E, Hesseltine C, Heath H (1979) Hydration of whole soybeans affects solid losses and cooking quality. *Journal of Food Science* 44:1510–1513, DOI 10.1111/j.1365-2621.1979.tb06474.x
- Warning A, Verboven P, Nicolaí B, van Dalen G, Datta AK (2014) Computation of mass transport properties of apple and rice from x-ray microtomography images. *Innovative Food Science & Emerging Technologies* pp in–press, DOI 10.1016/j.ifset.2013.12.017
- Weinstein T, Bennethum L (2006) On the derivation of the transport equation for swelling porous materials with finite deformation. *International Journal of Engineering Science* 44(18):1408–1422
- Winstanley H, Chapwanya M, McGuinness M, Fowler A (2011) A polymer-solvent model of biofilm growth. *Proceedings of the Royal Society A: Mathematical, Physical and Engineering Science* 467(2129):1449–1467
- Zanella-Díaz E, Mújica-Paz H, Soto-Caballero M, Welte-Chanes J, Valdez-Fragoso A (2014) Quick hydration of tepary (*Phaseolus acutifolius* a. gray) and pinto beans (*Phaseolus vulgaris* L.) driven by pressure gradients. *LWT - Food Science and Technology* in–press, DOI 10.1016/j.lwt.2014.05.042