

# Reactivity between carbon cathode materials and electrolyte based on industrial and laboratory data

L Chauke<sup>a\*</sup> and AM Garbers-Craig<sup>b†</sup>

<sup>a</sup> Department of Materials Science and Metallurgical Engineering, University of Pretoria, Pretoria, 0002, South Africa.

<sup>b</sup> Department of Materials Science and Metallurgical Engineering, University of Pretoria, Pretoria, 0002, South Africa

## Abstract

Interaction between electrolyte and carbon cathodes during the electrolytic production of aluminium decreases cell life. This paper describes the interaction between carbon cathode materials and electrolyte, based on industrial and laboratory data. It also reports on the degree of expansion of semi-graphitic and graphitised materials when exposed to a sodium rich environment. Phase relations in the slow cooled bath electrolyte, spent industrial cathodes and laboratory scale cathode samples were similar: all contained  $\text{Na}_3\text{AlF}_6$ ,  $\text{NaF}$ ,  $\text{CaF}_2$  and  $\text{NaAl}_{11}\text{O}_{17}$ .  $\text{Al}_4\text{C}_3$ ,  $\text{AlN}$  and  $\text{NaCN}$  were only detected in the spent industrial cathodes. The inability to locate  $\text{Al}_4\text{C}_3$  in the laboratory scale samples could be due to very low concentrations of  $\text{Al}_4\text{C}_3$  which could not be detected by XRD, or to the limited direct contact between the produced aluminium and carbon material. X-ray diffraction analysis confirmed that sodium intercalation into graphite did not take place. Wear of the examined carbon cathodes proceeded due to penetration of electrolyte and sodium into the cathode,

---

\* Currently with Materials Science and Manufacturing, CSIR, Pretoria, 0001, South Africa.

† Corresponding author. Fax: +27 12 362 5304. E-mail address: [Andrie.Garbers-Craig@up.ac.za](mailto:Andrie.Garbers-Craig@up.ac.za) (A.M. Garbers-Craig)

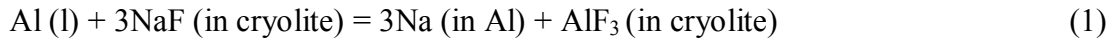
followed by reactions with carbon and  $N_2$  whereby AlN and NaCN formed. Once electrolysis started the carbon cathodes expanded rapidly, but slowed down after approximately an hour. Sodium expansion decreased with degree of graphitisation of the carbon cathode material.

## 1. Introduction

During the electrolytic production of aluminium in the Hall-Heroult cell, electrolyte and sodium penetrate and react with the carbon cathode material [1,2,3]. The cathode subsequently goes through significant changes in its chemical, physical and mechanical properties during operation, which cause degradation of the cathode and contribute to premature cell shutdowns. Penetration of bath constituents and sodium into the carbon cathode are highly dependent on the degree of graphitisation of the cathode as well as porosity, pore size distribution and granulometries, as micro pores provide penetration paths and capillary forces for the bath to penetrate the carbon cathode [4,5].

The interaction between the electrolyte and different types of carbon cathode blocks has been studied extensively. These studies have included the post mortem analyses of carbon cathodes from spent pot linings [6-11], and the evaluation of different types of carbon cathode materials in laboratory scale electrolysis [5,12,13] and Rapoport-Samoilenko or sodium-swelling experiments [6,7,14]. Crystalline phases that have been reported to be present in slow cooled industrial and laboratory cathode samples include  $Na_3AlF_6$ , NaF,  $Na_5Al_3F_{14}$ ,  $Na_2O \cdot 11Al_2O_3$ ,  $NaAlO_2$ ,  $\alpha-Al_2O_3$ ,  $Al_4C_3$ , NaCN, AlN,  $Na_2CO_3$  and  $NaCaAlF_6$  [3,15,16]. Proposed mechanisms explaining observed wear in carbon cathodes include sodium intercalation between graphite layers and chemical reactions between gaseous species, aluminium, electrolyte, sodium and carbon [1,17]. It is reported that reactions

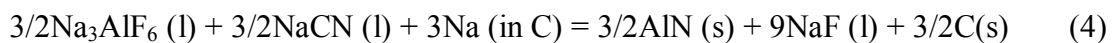
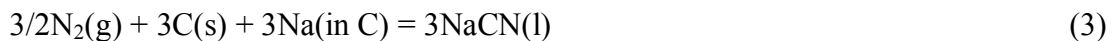
between carbon and gaseous species involve reactions with O<sub>2</sub> and N<sub>2</sub> in the air, anode gases and decomposed carbonates [1]. Zolochovsky *et al.* claimed that sodium can form from reaction between aluminium and electrolyte according to reaction 1, or electrochemically according to reaction 2 [6]:



The mechanisms whereby sodium penetrate and diffuse into the carbon lining are still not fully understood. The following penetration mechanisms have been reported [3,17]:

- i. An interfacial solid state diffusion process via mass transfer, whereby sodium penetrate inside carbon under a chemical potential gradient;
- ii. The direct reduction of sodium ions at the cathode interface and its direct insertion in carbon as shown in equation (2);
- iii. The absorption of sodium from the vapour phase into the porosity of the carbon.

Hop *et al.* studied the thermodynamics of reactions and compounds that can form during the aluminium electrolysis process at 950°C [18]. They found that if only Na, C and N<sub>2</sub> are present NaCN will form, and that NaCN becomes unstable in the presence of Na<sub>3</sub>AlF<sub>6</sub>, and reacts to form AlN (reactions 3 and 4):



They also reported that Na<sub>3</sub>AlF<sub>6</sub> can react with N<sub>2</sub> to form AlN (reaction 5):

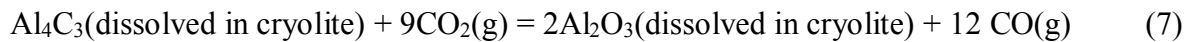


Different mechanisms have been proposed for the formation of Al<sub>4</sub>C<sub>3</sub> and how it affects the wear of carbon cathodes. Thermodynamically the formation of Al<sub>4</sub>C<sub>3</sub> is favoured at all

electrolysis temperatures when carbon and liquid aluminium come in direct contact [19], but according to Hop *et al.* it can also form from Na<sub>3</sub>AlF<sub>6</sub> in an argon atmosphere (reaction 6) [18]:



Various researchers have reported that Al<sub>4</sub>C<sub>3</sub> mainly forms on the cathode surface, and only in pores close to the surface of the cathode [16,19,20,21]. The aluminium carbide layer can dissolve and be transported away from the surface, thereby allowing new surfaces to react [20]. Sørli and Øye reported that Al<sub>4</sub>C<sub>3</sub> is not stable in the presence of anode gas, and converts to Al<sub>2</sub>O<sub>3</sub> according to the following reaction [22]:



Work by Zhang *et al.* on microstructures that form in MgO-C refractories that contain aluminium as antioxidant, indicated that as gaseous diffusion into the refractory increased the Al<sub>4</sub>C<sub>3</sub> (which formed between the aluminium antioxidant and carbon present in the refractory) reacted with N<sub>2</sub> from the atmosphere to form AlN, or was directly oxidised by CO to Al<sub>2</sub>O<sub>3</sub> [23]. A further increase in CO and N<sub>2</sub> contents of the atmosphere lead to the oxidation of AlN to Al<sub>2</sub>O<sub>3</sub>. Al<sub>4</sub>C<sub>3</sub> and AlN were found to co-exist in MgO-C bricks, where AlN whiskers formed on Al<sub>4</sub>C<sub>3</sub> grain surfaces.

The main aim of this study was to compare the crystalline phases that formed in slow cooled electrolyte from a Hall-Heroult cell with crystalline phases found in two spent pot linings and in two types of cathode materials (semi-graphitic and graphitised) that were reacted in laboratory electrolysis experiments. This was done to get a better understanding of how the cathode lining wears during short reaction times (laboratory scale experiments) as contrasted to wear over extended periods of time (as reflected by the spent lot linings). Specific

attention was also given to whether sodium intercalation was a main wear mechanism associated with the examined cathode materials. The study further evaluated different carbon cathode grades (semi-graphitic and graphitised) in terms of their degrees of sodium expansion, porosities and pore size distributions when they were exposed to a sodium rich environment.

## 2. Experimental

### 2.1. *Samples and sample preparation*

Post mortem and virgin carbon cathode samples were received from a South African aluminium smelter. The spent carbon cathode samples (A and B) were each taken from similar positions (bottom block of the cell, 40cm from the sidewall) but from different cells (Figure 1). Virgin samples A and B respectively contained 93% and 97% graphite. Sample A was removed from the cell after 1644 days in operation, while sample B was removed after 1944 days.

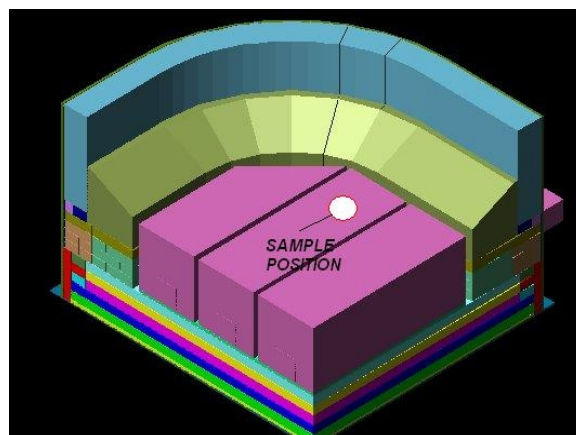


Figure 1. Position from where spent cathode samples were taken

Each spent cathode sample was cut into five slices, up to 26.81mm (sample A) and 33.77mm (sample B) below the electrolyte-carbon cathode interface. All of these slices were phase chemically analysed.

A sample of slow cooled solidified electrolyte was also obtained from the smelter for characterisation. The phase composition of this electrolyte was then compared to the phases that were distinguished in the samples of spent cathode, as well as the laboratory scale cathode samples.

Virgin carbon cathodes samples (50 mm in diameter, 50mm in height) were drilled from commercial semi-graphitic (sample C) and fully graphitised (sample D) carbon blocks. The bulk densities and chemical compositions of these carbon cathodes are given in Table 1.

**Table 1:** Preparation process, bulk density and chemical analysis of the examined carbon cathode materials

Sample name	Preparation process	Bulk Density g/cm <sup>3</sup>	Chemical analysis (mass %)					
			Ash	C	S	N	H	O
C	Semi-graphitic: 30% graphite, baked to 1000 – 1200°C	1.59	6.6	89.1	0.30	0.22	0.02	3.8
D	Graphitised block: Whole block (aggregate and binder) consisting of graphitisable materials, which has been heat treated at 3000°C	1.7	1.6	97.8	0.13	0.47	0.14	0.13

## 2.2. *Experimental procedures*

### 2.2.1 *Laboratory electrolysis experiments*

The virgin samples were electrolysed in a laboratory scale electrolysis cell that was constructed to simulate the behaviour and conditions of the Hall-Heroult cell. The experimental procedure was based on the Brilloit *et al.* experimental approach [21], but with minor modifications [24]. The experiments were performed under N<sub>2</sub> for respectively 1 hour 30 minutes and 3 hours at 980°C, using a current density of 0.75 A/cm<sup>2</sup>. The electrolyte was prepared from 90% Na<sub>3</sub>AlF<sub>6</sub>, 6% Al<sub>2</sub>O<sub>3</sub> and 4% CaF<sub>2</sub> (cryolite ratio of 2.29) giving a total mass of 400g. The carbon samples were furnace cooled under N<sub>2</sub> after each experiment.

### 2.2.2 *Rapoport or sodium expansion test*

Rapoport sodium expansion experiments were performed on the same carbon grades (samples C and D) as the electrolysis experiments. Samples (35mm in diameter, 90 mm height) were drilled parallel to the extrusion direction of the block. The sodium expansion tests were performed according to the Council of Scientific and Industrial Research (CSIR) procedure MMP-WP-315 [24]. A bath consisting of 80% Na<sub>3</sub>AlF<sub>6</sub>, 10% Al<sub>2</sub>O<sub>3</sub> and 10% NaF (with a cryolite ratio of 2.29) was prepared before each experiment. The experiments were performed for respectively 2 and 8 hours at 980°C. Two sets of measurements were performed for each cathode grade.

## 2.3. *Analysis techniques*

### 2.3.1 *X-ray Diffraction Analysis*

X-ray diffraction (XRD) analysis was used to identify and quantify the phases present in the carbon cathode samples. All samples were milled in a WC milling vessel and prepared for XRD analysis using a back loading preparation method. In the semi-quantitative XRD

analysis, 15% Si (Aldrich 99%) was added to the samples as a standard. The samples were micronized in a McCrone micronising mill under ethanol. A PANalytical X'Pert PRO powder diffractometer, with X'Celerator detector and variable divergence - and receiving slits, using Fe filtered Co-K $\alpha$  radiation, was used. The phases were identified using X'Pert Highscore plus software.

Sodium intercalation was assessed by examining the position and possible broadening of the  $2\theta=31.00^\circ$  graphite peak during the interpretation of the XRD patterns. This was done by looking at the full width at half maximum (FWHM) data of the  $2\theta=31.00^\circ$  graphite peak, using the X'Pert Data Viewer software.

### 2.3.2 *Scanning electron microscopy - energy dispersive spectroscopy*

Scanning electron microscopy - energy dispersive spectroscopy (SEM-EDS) analysis and EDS X-ray mapping were done to confirm the phase compositions, as determined by XRD analysis. This was done by using a JSM 6510 Jeol SEM with an EDS facility.

### 2.3.3 *Porosity measurements*

The total porosity, apparent porosity and pore size distribution of both virgin carbon cathode materials were determined. The porosity measurements were repeated five times, and average values are reported. For the determination of the pore size distributions two specimens (5mm thick and 25mm in diameter) were cut from each carbon grade, mounted in resin, ground and polished using 600 $\mu\text{m}$  – 2400 $\mu\text{m}$  grinding paper. Thirty arbitrary micrographs of each specimen were taken at the same magnification, after which the images were analysed using the ImageJ software (Java-based image processing programme developed at the National Institute of Health). The image analyses were conducted at different pore sizes.



### 3. Results and discussion

#### 3.1. *Post mortem analyses of industrial bath and carbon cathode samples*

The solidified electrolyte mostly contained villiaumite (NaF), cryolite ( $\text{Na}_3\text{AlF}_6$ ) and fluorite ( $\text{CaF}_2$ ), while  $\text{Al}_2\text{O}_3$  and diaoyudaiote ( $\text{NaAl}_{11}\text{O}_{17}$  or sodium  $\beta$ -alumina) were present in low concentrations.

The phases that could be distinguished in the electrolyte could be found in cathode samples A and B (Table 2), except for  $\text{Al}_2\text{O}_3$  which could not be found in cathode sample B.

Quantitative XRD analysis indicated that sample A has a higher concentration of  $\text{Na}_3\text{AlF}_6$  than sample B (~21 wt% vs. ~5 wt%), and also contained  $\text{Na}_5\text{Al}_3\text{F}_{14}$ , which could neither be identified in the solidified electrolyte nor in sample B. Both cathode samples A and B contain trace amounts of the reaction product AlN, while low concentrations of  $\text{Al}_4\text{C}_3$  and trace amounts of NaCN could only be found in cathode sample B.

The lower concentration of cryolite in sample B could partly be due to the formation of  $\text{Al}_4\text{C}_3$  according to the reaction 6. This is also supported by a higher concentration of NaF in sample B than in sample A (~8 wt% vs. ~2 wt%). The absence of chiolite in sample B could imply that the bath was depleted of aluminium ions and alumina had to be added, or it can simply indicate that chiolite formed peritectically from cryolite and aluminium fluoride on cooling at  $734^\circ\text{C}$  [7]. The presence of AlN and NaCN point to the formation of reaction products within the industrial cathodes, probably through a combination of reactions 3-5. Stereo microscopic analysis confirmed that the microstructure of cathode B was altered to greater depths than cathode A. However, larger open pores could be distinguished in cathode A than in cathode B.

**Table 2:** Phases identified in spent industrial cathode samples A and B

<b>Cathode sample A</b>	<b>Cathode sample B</b>
Na <sub>3</sub> AlF <sub>6</sub> (Cryolite)	Na <sub>3</sub> AlF <sub>6</sub> (Cryolite)
NaF (Villiaumite)	NaF (Villiaumite)
NaAl <sub>11</sub> O <sub>17</sub> (Diaoyudaoite)	NaAl <sub>11</sub> O <sub>17</sub> (Diaoyudaoite)
CaF <sub>2</sub> (Fluorite)	CaF <sub>2</sub> (Fluorite)
Al <sub>2</sub> O <sub>3</sub> (Corundum)	n.d.
Na <sub>5</sub> Al <sub>3</sub> F <sub>14</sub> (Chiolite)	n.d.
n.d.	Al <sub>4</sub> C <sub>3</sub>
AlN	AlN
n.d.	NaCN

n.d.: not detected

Full width at half maximum (FWHM) data of the  $2\theta=31.00^\circ$  graphite peak confirmed that sodium intercalation did not take place, as no change in peak position, d-spacing or peak broadening could be detected in any of the XRD patterns (Table 3).

Since XRD analysis indicated that intercalation did not take place, it is assumed that sodium diffused along pores in the carbon cathode, reacted with carbon, N<sub>2</sub> and cryolite to form NaCN and AlN according to reactions 3 - 5.

**Table 3:** Peak position and width of the  $2\theta=31.00^\circ$  graphite XRD peak

<b>Sample number</b>					
	1	2	3	4	5
<b>Unused Carbon cathode</b>					
Position ( $2\theta$ )	31.00	31.00	31.00	31.00	31.00
d-spacing ( $\text{\AA}$ )	3.37	3.37	3.37	3.37	3.37
FWHM [ $2\theta$ ]	0.220	0.221	0.220	0.220	0.221
<b>Carbon cathode sample A</b>					
Position ( $2\theta$ )	30.99	30.99	30.99	30.99	30.99
d-spacing ( $\text{\AA}$ )	3.37	3.37	3.37	3.37	3.37
FWHM [ $2\theta$ ]	0.221	0.221	0.220	0.220	0.221
<b>Carbon cathode sample B</b>					
Position ( $2\theta$ )	31.01	31.01	31.01	31.01	31.01
d-spacing ( $\text{\AA}$ )	3.37	3.37	3.37	3.37	3.37
FWHM [ $2\theta$ ]	0.220	0.220	0.220	0.220	0.221

### 3.2. Laboratory scale electrolysis experiments

Cryolite was observed in all the laboratory scale carbon cathode samples (Table 4). More cryolite penetrated the 30% graphite containing cathode than the fully graphitised cathode. The amount of cryolite that penetrated the cathodes increased with increasing time of electrolysis.

NaF was not identified in sample C (30% graphite) that was reacted for 3 hours. NaAl<sub>11</sub>O<sub>17</sub> was identified in all the experiments except when sample D (100% graphitised) was reacted for 1 hour 30 minutes. CaF<sub>2</sub> could only be identified in sample C after 3 hours of reaction, and in sample D after 1 hour 30 minutes. Na<sub>5</sub>Al<sub>3</sub>F<sub>14</sub> was only identified in sample D when it was reacted for 3 hours. NaCN, AlN and Al<sub>4</sub>C<sub>3</sub> could not be detected in any of the laboratory scale samples.

XRD analysis again indicated that intercalation did not take place as the 2θ=31.00° graphite peak did not shift, the d-spacing did not change, and the peak did not broaden or split.

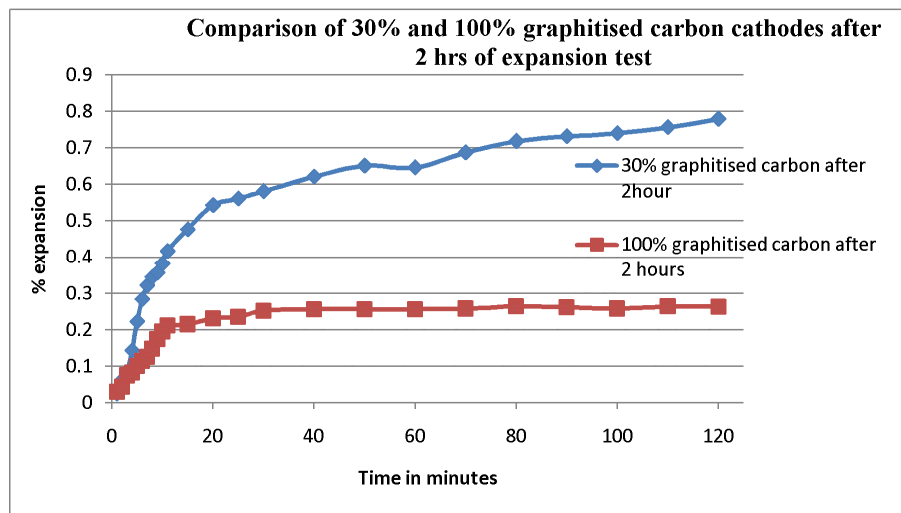
**Table 4:** Phases identified in the laboratory scale electrolysis samples

Sample C		Sample D	
1 hour 30 minutes	3 hours	1 hour 30 minutes	3 hours
Na <sub>3</sub> AlF <sub>6</sub> (Cryolite)	Na <sub>3</sub> AlF <sub>6</sub> (Cryolite)	Na <sub>3</sub> AlF <sub>6</sub> (Cryolite)	Na <sub>3</sub> AlF <sub>6</sub> (Cryolite)
NaF (Villiaumite)	n.d.	NaF (Villiaumite)	NaF (Villiaumite)
NaAl <sub>11</sub> O <sub>17</sub> (Diaoyudaoite)	NaAl <sub>11</sub> O <sub>17</sub> (Diaoyudaoite)	n.d.	NaAl <sub>11</sub> O <sub>17</sub> (Diaoyudaoite)
n.d.	CaF <sub>2</sub> (Fluorite)	CaF <sub>2</sub> (Fluorite)	n.d.
n.d.	n.d.	n.d.	Na <sub>5</sub> Al <sub>3</sub> F <sub>14</sub> (Chiolite)

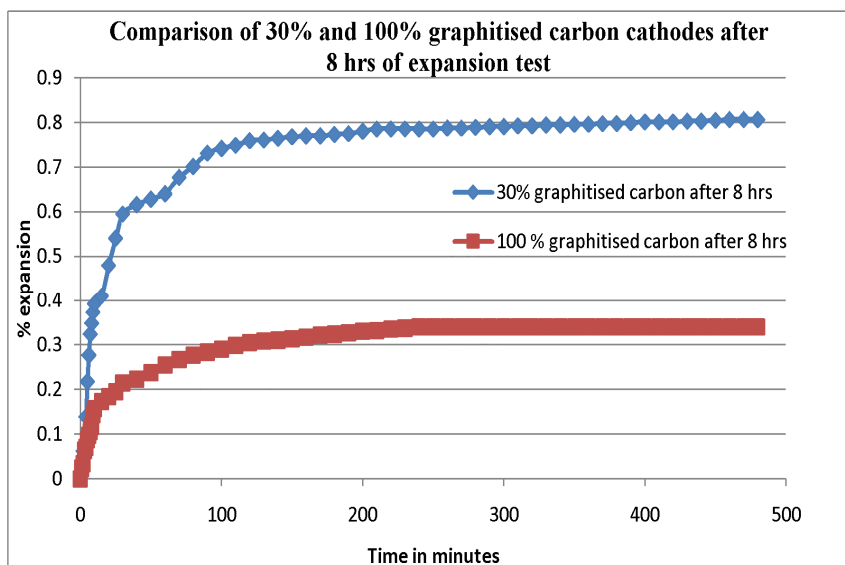
n.d.: not detected

### 3.3 Rapoport or sodium expansion results

Once electrolysis started, the cathode materials expanded rapidly, with the less graphitised carbon cathode (sample C, 30% graphite) being more susceptible to bath penetration than the 100% graphitised cathode material (sample D) (Figures 2 and 3). Expansion slowed down after approximately one hour. Sample C expanded 0.78% after 2 hours and 0.80% after 8 hours of exposure to the sodium rich environment, while the Sample D expanded only 0.27% after 2 hours and 0.34% after 8 hours of exposure.



**Figure 2:** Comparison of degrees of expansion of 30% and 100% graphite - containing carbon cathode materials after 2 hours of reaction



**Figure 3:** Comparison of degrees of expansion of 30% and 100% graphite - containing carbon cathode materials after 8 hours of reaction

### 3.5 Porosities and pore size distributions

The fully graphitised and semi-graphitic cathode materials respectively have total porosities of  $21\pm 3\%$  and  $20\pm 1\%$ , and open porosities of  $19\pm 2\%$  and  $17\pm 1\%$ .

Image analysis of the pore size distributions of the cathode materials indicated that the 100% graphitised material mostly contains small pores ( $1-5\mu\text{m}$ ), while the semi-graphitic carbon material mostly contains pores in the  $200-400\mu\text{m}$  diameter range. This is similar to what is reported in the literature, namely that the more graphitised materials in general have slightly higher porosities, but with smaller pore sizes [4,25]. Since the depth of liquid penetration into a capillary increases with pore diameter, it would be expected that the bath melt will penetrate deeper into the semi-graphitic cathode material, as was the case.

## 4. Conclusions

Phase relations in slow cooled electrolyte, spent industrial cathode and laboratory scale cathode samples were found to be very similar:  $\text{Na}_3\text{AlF}_6$ ,  $\text{NaF}$ ,  $\text{CaF}_2$  and  $\text{NaAl}_{11}\text{O}_{17}$  could be

distinguished in all of these samples. This finding is similar to what has been reported by Lossius and Øye for sixteen industrial carbon cathodes [16] and Tshöpe *et al.* for three spent pot linings [11]. Chiolite ( $\text{Na}_5\text{Al}_3\text{F}_{14}$ ) could only be identified in industrial cathode sample A and laboratory sample D that was reacted for 3 hours. The presence of chiolite could imply that the bath was depleted of aluminium ions and alumina had to be added, or it can simply indicate that chiolite formed on cooling from cryolite and aluminium fluoride through a peritectic reaction at  $734^\circ\text{C}$  [7]. It should invariably be kept in mind however, that during aluminium electrolysis the electrolyte is molten, and does not contain all of these crystalline phases. Cooling rates in the bath electrolyte as well as cathode blocks with penetrated electrolyte will therefore influence the crystalline phases that precipitate, as well as the proportions in which they precipitate.

$\text{Al}_4\text{C}_3$ ,  $\text{AlN}$  and  $\text{NaCN}$  were only found in the spent industrial cathode samples, and not in the electrolytic bath sample or any of the laboratory scale cathode samples. The spent cathode samples that were subjected to long reaction times therefore contain reaction products, i.e. phases that did not directly originate from the electrolyte but formed through interaction between the electrolyte, sodium, carbon and nitrogen. Laboratory scale samples that were subjected to short reaction times only contained phases that originated from the electrolytic bath. The inability to detect  $\text{Al}_4\text{C}_3$  in the laboratory scale cathode samples could be due to concentrations of  $\text{Al}_4\text{C}_3$  below the XRD detection limit, or due to limited direct contact between the produced aluminium and carbon cathode material which prevented  $\text{Al}_4\text{C}_3$  from forming (laboratory scale electrolysis resulted in the formation of an aluminium button in the graphite crucible, which did not evenly cover the cathode material). The absence of or limited presence of  $\text{Al}_4\text{C}_3$  in post mortem analyses were also reported by other authors: Lossius and Øye reported that  $\text{Al}_4\text{C}_3$  could be present at the surface of their examined industrial cathode samples, but not in the porosity [16]. Brisson *et al.* reported the presence

of small amounts of  $\text{Al}_4\text{C}_3$  in laboratory scale samples [12], while Vasshaug *et al.* reported that dissolution of  $\text{Al}_4\text{C}_3$  into the bath was faster than its formation, as no  $\text{Al}_4\text{C}_3$  could be observed on the surface of cathode samples which were used in electrolysis experiments [20]. An important finding from this study was that sodium intercalation into graphite did not take place. It can therefore be concluded that sodium was absorbed into the cathode materials through the porosity of the material. Wear of the examined carbon cathodes thus proceeded through electrolyte and sodium penetration, and the subsequent reaction between these species, the carbon cathode and nitrogen gas. It is however uncertain whether sodium penetrates in liquid form into carbon under a chemical potential gradient, or as sodium vapour into the porosity of the carbon, or in both forms.

During the laboratory scale sodium expansion tests expansion started as soon as the electrolysis process commenced. Expansion was rapid during the early stages of electrolysis, but slowed down after an hour. Sodium expansion decreased with degree of graphitisation of the cathode, similar to what is reported in the literature [2]. Associated with the fully graphitised material are mostly small pores (1-5 $\mu\text{m}$ ), while the semi-graphitic material contains pores predominantly in the 200-400 $\mu\text{m}$  diameter range.

### **Acknowledgements**

The authors would like to thank the Council for Scientific and Industrial Research, and the Technology and Human Resources for Industry Programme (THRIP) of the NRF for research funding. Special thanks are also due to Dr Sabine Verryn and Ms Wiebke Grote for performing the XRD analyses, Messrs Kalenda Mutombo and Siggqibo Camagu for guidance with the SEM-EDS analyses, Drs Sagren Govender, Hein Moller, Dawie van Vuuren and



Isobel McDougall, as well as Proffs Johan Markgraaf and Johan de Villiers for fruitful discussions.

## References

1. Xue, J, Liu, Q, Zhu, J, Ou, W. Sodium penetration into carbon-based cathodes during aluminium electrolysis. *Light Metals* 2006; 651-654.
2. Imris, M, Soucy, G, Fafard, M. Carbon cathode resistance against sodium penetration during aluminium electrolysis - An overview. *Acta Met Slov* 2005; 11(2):231-243.
3. Brisson, P-Y, Darmstadt, H, Fafard, M, Adnot, A, Servant, G, Soucy, G. X-ray photoelectron spectroscopy study of sodium reaction in carbon cathode blocks of aluminium oxide reduction cell. *Carbon* 2006; 44:1438-1447.
4. Gao, Y, Xue, J, Zhu, J, Jiao, K, Jiang, G. Characterisation of sodium and fluoride penetration into carbon cathodes by image analysis and SEM-EDS techniques. *Light Metals* 2011; 1103-1107.
5. Patel, P, Hyland, M, Hiltmann, F. Influence of internal cathode structure on behaviour during electrolysis Part II: Porosity and wear mechanisms in graphitized cathode material. *Light Metals* 2005; 757-762.
6. Zolochovsky, A, Hop, JG, Foosnaes, T, Øye, HA. Rapoport-Samoilenko test for cathode materials-II swelling with external pressure and effect of creep. *Carbon* 2005; 43:1222-1230.
7. Zolochovsky, A, Hop, JG, Servant, G, Foosnaes, T, Øye, HA. Creep and sodium expansion in semigraphitic cathode carbon. *Light metals* 2003; 595-602.
8. Brisson, PY, Soucy, G, Fafard, M, Dionne, M. The effect of sodium on carbon lining of the aluminium electrolysis cell - A review. *Can Met Q* 2002; 44(2):265-279.

9. Brisson, PY, Soucy, G, Fafard, M, Darmstadt, H, Servant, G. Revisiting sodium and bath penetration in the carbon lining of aluminium electrolysis cell, *Light Metals* 2005; 727-732.
10. Tschöpe, K, Schøning, C, Grande, T. Autopsies of spent pot linings – A revised view. *Light Metals* 2009; 1085-1090.
11. Tschöpe, K, Schøning, C, Rutlin, J, Grande, T. Chemical degradation of cathode linings in Hall-Heroult cells – An autopsy study of three spent pot linings. *Met Trans B* 2012; 43B:290-301.
12. Brisson, PY, Fafard, M, Soucy, G. Investigation of electrolyte penetration in three carbon cathode materials for aluminium electrolysis cells. *Can Met Q* 2006; 45(4):417-426.
13. Xue, J, Ou, W, Zhu, J, Liu, Q. Analysis of sodium and cryolite bath penetration in the cathodes used for aluminum electrolysis. *Light Metals* 2009; 1177-1181.
14. Zolochovsky, A, Hop, JG, Foosnaes, T, Øye, HA. Rapoport-Samoilenko test for cathode materials-I, experimental results and constitutive modelling. *Carbon* 2003; 41:497-505.
15. Zoukel, A, Chartrand, P and Soucy, G. Study of aluminium carbide formation in Hall-Heroult cells, *Light Metals* 2009; 1123-1128.
16. Lossius, LP, Øye, HA. Melt penetration and chemical reactions in 16 industrial aluminium carbon cathodes. *Metall Trans B* 2000; 31B:1213-1224.
17. Wang, Zh, Rutlin, J, Grande, T. Sodium diffusion in cathode lining in aluminium electrolysis cells. *Light Metals* 2010; 841-847.
18. Hop, J, Støre, A, Foosnæs, T, Øye, HA. Chemical and physical changes of cathode carbon by aluminium electrolysis. *Trans. Inst. Min. Metall. C*; 114:C181-C187.
19. Sørli, M, Øye, HA. Deterioration of carbon linings in aluminium reduction cells. II. – Chemical and physical characterization of cathode carbons. *Metall* 1984; 38(2):109-115.

20. Vasshaug, K, Foosnæs, T, Haarberg, GM, Ratvik, AP, Skybakmoen, E. Formation and dissolution of aluminium carbide in cathode blocks. *Light Metals* 2009; 1111-1116.
21. Brilloit, P, Lossius, LP, Øye, HA. Penetration and chemical reactions in carbon cathodes during aluminum electrolysis: part i. laboratory experiments. *Metall Trans B* 1993; 24(1):75-89.
22. Sørli, M, Øye, HA. Evaluation of cathode material properties relevant to the life of Hall-Heroult cells. *J Applied Electrochem* 1989; 19:580-588.
23. Zhang, S, Marriott, NJ, Lee, WE. Thermochemistry and microstructures of MgO-C refractories containing various antioxidants. *J Eur Ceram Soc* 2001; 21:1037-1047.
24. Chauke, L. Reactivity of carbon cathode materials and electrolyte based on plant and laboratory data. University of Pretoria, Pretoria, South Africa, MSc thesis, 2012.
25. Patel, P, Hyland, M, Hiltmann, F. Influence of internal cathode structure on behaviour during electrolysis Part III: Wear behaviour in graphitic materials. *Light Metals* 2006; 633-638.